

**APPENDIX B**  
**FIELD DATA**

## **TOLUENE-SOLUBLE ORGANICS**

## FIELD DATA SHEET

Plant: AK Madhetawa  
 Sampling Location: P. Baghouse Stack 2  
 Run Number: P-315-1 Date: 9/12/16  
 Pretest Leak Rate: 0.02 cfm @ 12 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: -

Sample Type: AK Operator: EL  
 Pbar: 30.20 Ps: -1.1  
 CO<sub>2</sub>: CEM O<sub>2</sub>: CEM  
 Probe Length/Type: 3' 6L Pitot#: T3-WP  
 Stack Diameter: 35.5 K: 0.6441

Nozzle ID: 0156 Thermocouple #: T3-4P  
 Assumed Bws: 2.5 Filter #: Q2-3097  
 Meter Box #: 5 Y: 0993 ΔH@: 1926  
 Post-Test Leak Rate: 0.03 cfm @ 5 in.Hg. } End of  
 Post-Test Leak Check: Pitot: ✓ Orsat: - } Day Shift

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)		Temperature EF		Impinger Temp. of	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual			Probe	Filter			Inlet	Outlet	
0	0	1026	196.500												
1	3:14	1026-29	198.616	2.8	1.7	1.7	92	250	265	265	62	N/A	64	63	1
2	6:32	1045-48	200.875	3.7	1.6	1.6	104	248	251	251	61		65	64	1
3	9:42	102-05	203.034	2.5	1.5	1.5	112	250	260	260	60		66	66	1
4	12:55	116-19	205.278	2.8	1.7	1.7	121	257	264	264	60		68	67	1
5	16:19	1136-39	207.614	2.7	1.6	1.6	118	258	265	265	61		69	68	1
6	19:38	1051-54	209.998	3.2	1.9	1.9	122	255	261	261	62		70	69	1
1	22:56	1201-04	212.409	3.3	2.0	2.0	117	261	263	263	61		72	70	1
2	26:14	1221-24	214.976	3.4	2.0	2.0	115	263	265	265	62		73	72	1
3	29:29	1228-41	217.462	3.2	1.9	1.9	122	264	266	266	62		74	73	1
4	32:48	1257-30	220.010	3.3	2.0	2.0	119	267	265	265	64		75	75	1
5	34:13	1316-14	222.756	3.7	2.2	2.2	120	268	264	264	60		76	76	1.5
6	39:26	1356-39	225.374	3.7	2.2	2.2	125	264	265	265	60		77	77	1.5
1	42:42	1350-54	227.984	3.7	2.2	2.2	127	265	262	262	60		77	77	1.5
2	46:05	1409-42	230.581	3.4	2.0	2.0	128	263	260	260	61		77	77	1
3	49:19	1451-54	233.065	3.4	2.0	2.0	124	265	253	253	62		78	77	1
4	52:41	1507-10	235.644	3.4	2.0	2.0	122	265	264	264	63		78	78	1
5	55:54	1524-28	238.197	3.6	2.1	2.1	125	257	265	265	62		78	78	1
6	59:12	1542-45	240.868	3.7	2.2	2.2	121	262	266	266	63		78	78	1.5
1	62:38	1591-03	243.702	3.7	2.2	2.2	123	261	267	267	64		79	78	1.5
2	65:57	1616-19	246.360	3.6	2.1	2.1	123	264	264	264	63		78	78	1.5
3	69:13	1635-37	248.924	3.5	2.1	2.1	130	266	252	252	64		78	78	1
4	72:33	1651-55	251.633	3.5	2.1	2.1	131	265	259	259	62		78	78	1
5	76:20	1708-13	254.660	3.5	2.1	2.1	124	261	266	266	63		78	78	1
6	79:39	1735-28	257.368	3.4	2.0	2.0	118	262	263	263	62		78	78	1
1	82:56	1738-41	260.030	3.5	2.1	2.1	120	268	261	261	63		78	78	1

LEAK: ✓ 260.030 ΔVm = ✓ Δp = ✓ ΔH = ✓ Ts = ✓  
 260.030 260.150

ΔVm Pay Shift = 63.530

Tm =

✓

## FIELD DATA SHEET

Plant: AK Middleton Sample Type: M315 Operator: CJ  
 Sampling Location: Baghouse Stack 2 Pbar: 30.20 Ps: -1.1  
 Run Number: 9-315-1 Date: 9/12/16 CO<sub>2</sub>: CEM O<sub>2</sub>: CEM  
 Pretest Leak Rate: 0.1 cfm @ 10 in.Hg. Probe Length/Type: 3'CL Pitot#: 13-11P  
 Pretest Leak Check: Pitot: ✓ Orsat: — Stack Diameter: 35.5" K: 0.641

[illegible]

$\Delta V_m = 82.488$	$\sqrt{\Delta p} = 182.65$	$\overline{\Delta H} = 2.01$	$\overline{T_S} = 114$
	$\overline{\Delta p} = 3.34$		



### SAMPLE RECOVERY DATA

Plant AK Middleton Run No. P-315-1  
 Date 9/13/16 Sample Box No. SB-12 Job No. 050074.0172  
 Sample Location Pushing Bayhouse Filter No. QZ 3097  
 Train Preparer EZ Sample Head No. 4  
 Sample Recovery Person CJ Barometer No. TLK.COM  
 Comments M315 Balance No. 2

Front Half

Acetone P-315-1 Liquid ✓  
 Container No. FRONT 1/2 ACETONE Level Marked ✓ Sealed ✓  
FRONT 1/2 TOLUENE

Filter  
 Container No. QZ 3097 Sealed ✓

Description of Filter grey loading

Samples Stored and Locked ✓

Back Half/Moisture

Container No. P-315-1 BACK 1/2 H<sub>2</sub>O / ACETONE / TOLUENE

Liquid Level Marked \_\_\_\_\_ Sealed \_\_\_\_\_

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	H <sub>2</sub> O	100	756.0	756.0	0.0
2	H <sub>2</sub> O	100	766.8	773.0	6.2
3	—	—	665.4	666.9	1.5
4	Silica Gel	250	965.9	984.0	18.1
5					
6					
Total					25.8

Description of Impinger Catch: \_\_\_\_\_

BWS = 15%

✓MP

Plant: AK MiddletownSample Type: M315 Operator: EZNozzle ID: 0.56 Thermocouple #: T3-4PSampling Location: Bayhouse Stack 2Pbar: 30.15 Ps: -1.1Assumed Bws: 25 Filter #: R2300Run Number: P-315-2 Date: 9/13/10CO<sub>2</sub>: CEM O<sub>2</sub>: CEMMeter Box #: 5 Y: 0.773 ΔH@: 1.906Pretest Leak Rate: 0.01 cfm @ 16 in.Hg.Probe Length/Type: 3' GL Pitot#: T3-7PPost-Test Leak Rate: 0.003 cfm @ 3 in.Hg. } End of Day ShiftPretest Leak Check: Pitot: ✓ Orsat: -Stack Diameter: 35.5 K: 0.6441Post-Test Leak Check: Pitot: ✓ Orsat: -

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	1359	279.288											
1	3:13	1359-42	281.570	2.7	1.6	1.6	120	261	266	65	N/A	73	73	1
2	6:24	1409-32	283.908	2.5	1.5	1.5	130	260	265	65		75	75	1
3	9:56	1439-43	286.222	2.6	1.5	1.5	131	261	264	64		76	76	1
4	13:15	1456-1500	288.446	2.6	1.5	1.5	129	266	250	64		77	77	1
5	16:32	1521-24	290.905	3.1	1.8	1.8	128	260	261	60		78	77	1
6	19:51	1532-36	293.390	3.1	1.8	1.8	132	263	264	60		78	78	1
1	23:15	1550-53	295.897	3.0	1.8	1.8	130	265	266	60		79	78	1
2	26:36	1605-08	298.431	3.4	2.0	2.0	128	263	264	61		79	78	1.5
3	29:56	1620-24	300.938	3.2	1.9	1.9	135	264	264	61		79	79	1.5
4	33:10	1641-45	303.412	3.4	2.0	2.0	133	264	265	62		79	79	1.5
5	36:28	1651-54	305.872	3.3	1.9	1.9	136	264	265	62		79	78	1.5
6	39:49	1700-03	308.405	3.2	1.9	1.9	139	255	262	63		79	78	1.5
1	43:05	1729-12	310.977	3.6	2.1	2.1	136	270	265	61		79	78	1.5
2	46:26	1721-24	313.507	3.3	1.9	1.9	138	259	264	60		78	77	1.5
3	49:44	1730-33	316.055	3.3	1.7	1.9	129	269	266	59		78	77	1.5
4	53:06	2232-2236	319.121	3.6	2.2	2.2	95	262	266	53		71	70	2
5	56:28	2244-2248	321.954	3.6	2.2	2.2	99	254	264	56		73	72	2
6	59:43	2303-2306	324.644	3.5	2.1	2.1	105	260	266	56		74	73	2
1	62:58	2312-2316	327.240	3.4	2.1	2.1	109	260	264	54		75	75	2
2	66:15	2341-2345	329.716	3.5	2.1	2.1	114	252	264	50		76	76	2
3	69:37	0000-0004	332.601	3.4	2.0	2.0	116	256	265	52		77	76	2
4	72:57	0019-0022	335.344	3.5	2.1	2.1	110	261	262	54		77	77	2
5	76:18	0040-0044	337.929	3.5	2.1	2.1	114	260	267	55		77	77	2
6	79:40	0059-0100	340.615	3.5	2.1	2.1	112	266	266	54		77	77	2
1	83:01	0110-0119	343.315	3.4	2.1	2.1	111	266	264	55		78	77	2

$$\Delta V_m = \sqrt{\Delta p} = \frac{\Delta H}{T_s} = \frac{T_m}{T_s}$$

$$\Delta V_m \text{ Day Shift} = 36.767$$

AM

## FIELD DATA SHEET

Plant: AK Middletown Sample Type: N315 Operator: EZ/cj Nozzle ID: Q156 Thermocouple #: T3-41P  
Sampling Location: Bridge over Stack 2 Pbar: 30.15 Ps: -1.1 Assumed Bws: 2.5 Filter #: Q2 3100  
Run Number: P-315-2 Date: \_\_\_\_\_ CO<sub>2</sub>: CEM O<sub>2</sub>: \_\_\_\_\_ Meter Box #: 5 Y: 0.993 ΔH@: 1.926  
Pretest Leak Rate: \_\_\_\_\_ cfm @ \_\_\_\_\_ in.Hg. Probe Length/Type: 31.6 Pitot#: T3-41P Post-Test Leak Rate: 0.03 cfm @ \_\_\_\_\_ in.Hg.  
Pretest Leak Check: Pitot: \_\_\_\_\_ Orsat: \_\_\_\_\_ Stack Diameter: 33.5" K: 0.6441 Post-Test Leak Check: Pitot: ✓ Orsat: N/A

[illegible]

$$\Delta V_m = 80.346 \sqrt{\Delta p = 1.8092} \quad \Delta H = 1.96 \quad T_s = 120$$

$$\overline{T_m} = 77$$
$$150 = 100.9\%$$


## SAMPLE RECOVERY DATA

Plant AK Middletown Run No. P-315-2  
 Date 9/14/16 Sample Box No. \_\_\_\_\_ Job No. 050074.0172  
 Sample Location Pushing Bay house Filter No. QZ-3100  
 Train Preparer CJ Sample Head No. 4  
 Sample Recovery Person CJ Barometer No. TWE.COM  
 Comments M315 Balance No. 2

Front Half

Acetone P-315-2 Liquid  
 Container No. FRONT 1/2 ACETONE Level Marked ✓ Sealed ✓  
 Filter FRONT 1/2 TOLUENE  
 Container No. QZ-3100 Sealed ✓

Description of Filter light grey loading  
 Samples Stored and Locked ✓

Back Half/Moisture

Container No. P-315-2 BACK 1/2 H<sub>2</sub>O / ACETONE / HEXANE RINSE  
 Liquid Level Marked ✓ Sealed ✓

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	H <sub>2</sub> O	100	755.3	759.1	3.8
2	H <sub>2</sub> O	100	762.6	768.0	5.4
3	—	—	665.3	666.6	1.3
4	SG	250	984.0	1004.4	20.4
5					
6					
Total					30.9

Description of Impinger Catch: clear

BWS = 1.07.

Plant: AK Metallurgy  
 Sampling Location: Baghouse Stack 2  
 Run Number: P-315-3 Date: 9/14/16  
 Pretest Leak Rate: 0.021 cfm @ 15 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: —

Sample Type: 315 Operator: FZ/CJ  
 Pbar: 30.21 Ps: -1.1  
 CO<sub>2</sub>: CEM O<sub>2</sub>: CEM  
 Probe Length/Type: 36L Pitot#: T3-4P  
 Stack Diameter: 35.5" K: 0.6441

Nozzle ID: 156 Thermocouple #: T3-4P  
 Assumed Bws: 2.5 Filter #: R2 3102  
 Meter Box #: 5 Y: 2993 AH@: 1.126  
 Post-Test Leak Rate: 0.021 cfm @ 5 in.Hg.  
 Post-Test Leak Check: Pitot: ✓ Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	1635	360.982											
1	3:17	1635-38	362.285	2.8	1.7	1.7	122	252	264	65	N/A	80	80	2
2	6:40	1648-52	364.697	2.7	1.6	1.6	125	254	264	65		81	80	2
3	9:56	1705-08	367.009	2.9	1.7	1.7	128	257	263	60		81	81	2
4	13:13	1722-26	369.341	2.8	1.7	1.7	127	255	264	61		81	81	2
5	16:28	1735-38	371.650	2.7	1.6	1.6	129	257	266	62		81	81	2
6	20:00	2241-2234	374.665	3.6	2.2	2.2	94	264	266	58		72	73	2
1	23:27	2251-2234	377.168	3.5	2.1	2.1	107	260	265	54		72	72	2
2	26:40	2244-2248	380.000	3.5	2.1	2.1	108	259	265	56		73	73	2
3	29:52	2303-2307	382.609	3.2	1.9	1.9	113	251	268	59		73	73	2
4	33:08	2312-2316	385.247	3.4	2.0	2.0	111	253	264	60		73	73	2
5	36:22	2342-2346	387.869	3.4	2.0	2.0	110	255	266	58		72	73	2
6	39:39	0000-0001	390.500	3.4	2.1	2.1	107	266	262	58		73	73	2
1	42:57	0019-0023	393.145	3.5	2.1	2.1	111	261	262	59		73	73	2
2	46:13	0041-0042	395.775	3.4	2.0	2.0	111	260	268	61		73	73	2
3	49:26	0057-0100	398.386	3.3	2.0	2.0	114	259	268	58		73	73	2
4	52:41	0116-0120	400.801	3.4	2.1	2.1	104	256	263	60		72	73	2
5	55:54	0135-0138	403.629	3.4	2.1	2.1	107	252	264	60		72	72	2
6	59:06	0144-0148	406.100	3.4	2.1	2.1	105	258	265	61		72	72	2
1	62:21	0158-0322	408.767	3.5	2.2	2.2	96	257	264	61		74	71	2
2	65:37	0205-0208	411.433	3.4	2.1	2.1	97	260	265	59		71	71	2
3	68:54	0243-0317	414.111	3.6	2.2	2.2	99	258	266	59		71	71	2
4	72:06	0253-0356	416.662	3.4	2.1	2.1	98	257	264	60		72	71	2
5	75:16	0301-0304	419.239	3.3	2.0	2.0	100	259	262	59		72	71	2
6	78:31	0410-0413	421.873	3.4	2.1	2.1	97	256	262	59		72	71	2

LEAK CHECK  
 0.021 cfm @ 15 in.Hg  
 371.650 - 371.750

End of Day Shift

$$\Delta V_m = \sqrt{\Delta p} = \frac{\Delta H}{T_s} = \frac{T_m}{T_s}$$

Plant: AK Middleton  
 Sampling Location: Baghouse Stack 2  
 Run Number: P-315-3 Date: 7/14-15/16  
 Pretest Leak Rate: 0.001 cfm @ 15" in.Hg.  
 Pretest Leak Check: Pitot: ✓± Orsat: —  
 Sample Type: M315 Operator: EZ/CJ  
 Pbar: 30.21 Ps: -1.1  
 CO<sub>2</sub>: CEM O<sub>2</sub>: CEM  
 Probe Length/Type: 3.6L Pitot#: I3-4P  
 Stack Diameter: 35.5" K: 0.6441

Nozzle ID: 0156 Thermocouple #: T3-4P  
 Assumed Bws: 25 Filter #: Q2-3702  
 Meter Box #: 5 Y: 0993 ΔH@: 1906  
 Post-Test Leak Rate: 0.001 cfm @ 9 in.Hg.  
 Post-Test Leak Check: Pitot: 1 Orsat: -

[illegible]
$$\Delta V_m = 81.234 \quad \sqrt{\Delta p} = 1.8195 \quad \Delta H = 201 \quad T_s = 106$$

WT = 73

$$\Delta_2 = \cancel{2.156} \quad 3.3156$$

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### SAMPLE RECOVERY DATA

Plant AK Middletown Run No. P-315-3  
 Date 9/14/16 Sample Box No. SB-8 Job No. 052074.0072  
 Sample Location Pushing Baghouse Filter No. Q2-3102  
 Train Preparer FZ Sample Head No. SH-7  
 Sample Recovery Person BF Barometer No. PWC.com  
 Comments 315 Balance No. FB-2

Front Half

Acetone Liquid  
 Container No. P-315-3 Level Marked ✓ Sealed ✓

Filter

Container No. Q2-3102 Sealed ✓

Description of Filter no visible loading

Samples Stored and Locked ✓

Back Half/Moisture

Container No. NA

Liquid Level Marked NA Sealed NA

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	H <sub>2</sub> O	100	774.6	767.0	-7.6
2	H <sub>2</sub> O	100	781.3	786.7	5.4
3	—	—	669.9	663.1	2.2
4	Silica Gel	250	942.0	970.9	28.9
5					
6					
Total					28.9

Description of Impinger Catch: clear



## FIELD DATA SHEET

Plant: AK Middleton

Sample Type: 315 MCEM Operator: AK  
 Pbar: 30.70 Ps: -0.00  
 CO<sub>2</sub>: 3 O<sub>2</sub>: 15  
 Probe Length/Type: 6' 6L Pitot#: 15-B  
 Stack Diameter: 16" K: 57.363

Nozzle ID: 500 Thermocouple #: 75-0  
 Assumed Bws: 10 Filter #: Q23098  
 Meter Box #: 3 Y: 1.004 ΔH@: 1.390  
 Post-Test Leak Rate: — cfm @ — in.Hg.  
 Post-Test Leak Check: Pitot: — Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	1005	175.973	0.040	1.50	1.50	351	260	260	65	65	64	63	1
1	5	1010	179.2	0.035	1.3	1.3	361	240	250	57	68	64	63	1
2	10	1015	182.3	0.040	1.5	1.5	365	246	253	53	65	67	64	1
3	15	1020	185.6	0.035	1.3	1.3	370	252	252	53	63	70	65	1
4	20	1025	189.7	0.040	1.5	1.5	370	251	251	53	62	72	65	1
5	25	1030	191.9	0.040	1.5	1.5	374	252	252	55	—	74	66	1
6	30	1035	195.1	0.040	1.5	1.5	376	249	250	57	—	74	67	1
7	35	1040	198.4	0.040	1.5	1.5	380	251	251	59	—	76	68	1
8	40	1045	201.6	0.040	1.5	1.5	355	249	251	60	—	78	69	1
9	45	1050	204.8	0.040	1.5	1.5	352	251	249	63	—	78	70	1
10	50	1055	207.6	0.035	1.3	1.3	355	248	250	64	—	81	72	1
11	55	1100	211.4	0.035	1.3	1.3	358	249	250	61	—	81	73	1
12	60	1105	214.6	0.040	1.5	1.5	364	247	244	62	—	83	75	1
13	65	1110	218.4	0.040	1.5	1.5	366	248	245	62	—	83	75	1
14	70	1115	220.9	0.040	1.5	1.5	370	250	249	61	—	84	76	1
15	75	1120	224.1	0.040	1.5	1.5	374	249	251	61	—	84	77	1
16	80	1125	231.1	0.040	1.5	1.5	379	250	250	62	—	85	77	1
17	85	1130	233.9	0.040	1.5	1.5	381	249	250	62	—	85	78	1
18	90	1135	235.6	0.035	1.3	1.3	349	251	249	62	—	86	78	1
19	95	1140	237.4	0.035	1.3	1.3	350	250	245	62	—	86	79	1
20	100	1145	240.5	0.035	1.3	1.3	351	248	245	63	—	87	79	1
21	105	1150	243.7	0.035	1.3	1.3	354	246	248	64	—	87	80	1
22	110	1155	246.7	0.040	1.5	1.5	358	251	250	62	—	87	81	1
23	115	1200	249.8	0.040	1.5	1.5	360	250	250	61	—	88	81	1
24	120	1205	252.9	0.040	1.5	1.5	360	250	250	61	—	88	81	1

$$\Delta V_m = \sqrt{\Delta p} = \sqrt{\Delta H} = \sqrt{T_s} = \text{---}$$

$$T_m = \text{---}$$





**SAMPLE RECOVERY DATA**

Plant AK Middletown Run No. Comb 315-1  
 Date 9/12/16 Sample Box No. SB-4 Job No. 050074.0172  
 Sample Location COMBUSTION Filter No. 3098  
 Train Preparer EZ Sample Head No. SH-1  
 Sample Recovery Person BF Barometer No. 721.00  
 Comments 315 Balance No. FB-2

Front Half

Acetone C-315-1 Liquid  
 Container No. ✓ Level Marked ✓ Sealed ✓

Filter

Container No. Q2-3098 Sealed ✓

Description of Filter black

Samples Stored and Locked ✓

Back Half/Moisture

Container No. NA

Liquid Level Marked NA Sealed NA

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	H <sub>2</sub> O	100	761.4	862.4	101.0
2	H <sub>2</sub> O	100	752.7	794.5	41.8
3	—	—	675.0	686.7	11.7
4	Silica Gel	250	952.0	973.0	21.0
5					
6					
Total					176.3

Description of Impinger Catch: clar

✓BF

## FIELD DATA SHEET

Plant: AK Steel Middlesex Sample Type: 315 Operator: Wk/D/S Nozzle ID: Q 500 Thermocouple #: TS-2  
 Sampling Location: Combustion Stack Pbar: 30.15 Ps: -0.20" Assumed Bws: 10 Filter #: QZ 3099  
 Run Number: C-315-2 Date: 9/13/10 CO<sub>2</sub>: 3 O<sub>2</sub>: 15 Meter Box #: 3 Y: 1.009 ΔH@: 1.89  
 Pretest Leak Rate: 0.002 cfm @ 11 in. Hg. Probe Length/Type: 5'61 Pitot#: P5-2 Post-Test Leak Rate: 0.002 cfm @ 5 in. Hg.  
 Pretest Leak Check: Pitot: 1/2 Orsat: — Stack Diameter: 16.3" K: 60.573 Post-Test Leak Check: Pitot: 1/2 Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
	0	0955	260.021											
	5	1000	263.500	0.04	1.60	1.60	348	249	252	68		65	64	1
	10	1005	266.7	0.04	1.60	1.60	360	250	253	62		67	65	1
	15	1010	270.3	0.05	1.9	1.9	361	248	252	60		68	66	1
	20	1015	274.2	0.05	1.9	1.9	364	250	250	62		73	67	1
	25	1020	277.6	0.05	1.9	1.9	365	249	250	63		75	67	1
	30	1025	281.3	0.05	1.9	1.9	374	249	249	65		76	68	1
	35	1030	284.8	0.04	1.6	1.6	375	251	249	65		78	69	1
	40	1035	288.0	0.04	1.6	1.6	376	251	250	66		79	70	1
	45	1040	291.2	0.04	1.6	1.6	378	249	250	66		80	70	1
	50	1045	294.8	0.04	1.6	1.6	380	253	250	57		82	72	1
	55	1050	297.8	0.04	1.6	1.6	350	249	251	58		82	73	1
	60	1055	301.2	0.04	1.6	1.6	353	246	250	57		83	74	1
	65	1100	304.6	0.04	1.6	1.6	357	251	250	57		83	76	1
	70	1105	307.7	0.035	1.4	1.4	360	251	242	57		86	76	1
	75	1110	311.2	0.035	1.4	1.4	361	252	241	59		86	77	1
	80	1115	314.2	0.04	1.6	1.6	365	253	250	60		87	78	1
	85	1120	317.6	0.04	1.6	1.6	369	248	249	61		88	79	1
	90	1125	320.9	0.04	1.6	1.6	373	247	249	61		89	80	1
	95	1130	324.3	0.04	1.6	1.6	374	249	250	62		90	80	1
	100	1135	327.8	0.04	1.6	1.6	380	249	250	62		90	81	1
	105	1140	331.0	0.035	1.4	1.4	383	251	249	62		90	82	1
	110	1145	334.4	0.035	1.4	1.4	351	249	250	58		89	82	1
	115	1150	338.1	0.040	1.6	1.6	351	248	249	57		90	82	1
	120	1155	341.622	0.050	1.9	1.9	353	249	249	56		90	83	1

$$\Delta V_m = 81.601 \sqrt{\Delta p} = 0.2028 \Delta H = 1.63 Ts = 365$$

0.0413

$$\overline{T_m} = 78$$

✓68

## SAMPLE RECOVERY DATA

Plant Alt Middletown Run No. Comb 315-2  
 Date 7/13/14 Sample Box No. 587 Z Job No. 052074.0172  
 Sample Location Combustion Stack Filter No. QZ-3099  
 Train Preparer BF Sample Head No. SH-1  
 Sample Recovery Person BF/RK Barometer No. TWC.com  
 Comments 315 Balance No. FB-2

Front Half

Acetone Liquid  
 Container No. C-315-2 Level Marked ☒ Sealed ☒

Filter

Container No. QZ-3099 Sealed ☒

Description of Filter black

Samples Stored and Locked ☒

Back Half/Moisture

Container No. N/A

Liquid Level Marked N/A Sealed N/A

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	H <sub>2</sub> O	100	777.4	899.3	121.9
2	H <sub>2</sub> O	100	757.8	789.6	31.8
3	-	-	668.6	672.3	3.7
4	Silica Gel	250	951.9	981.0	29.1
5					
6					
Total					186.5

Description of Impinger Catch: clear

✓BF

## FIELD DATA SHEET

Plant: AK Middlemore Sample Type: 315 Operator: Re/Ds Nozzle ID: 0.500 Thermocouple #: P5-2  
 Sampling Location: Combustion Stack Pbar: 30.21 Ps: -0.75" Assumed Bws: 9 Filter #: QE 3101  
 Run Number: C-315-3 Date: 9/14/16 CO<sub>2</sub>: 3 O<sub>2</sub>: 15 Meter Box #: 3 Y: 1.009 AH@: 1.89  
 Pretest Leak Rate: 0.001 cfm @ 11 in.Hg. Probe Length/Type: 5'6" Pitot#: P5-2 Post-Test Leak Rate: 0.000 cfm @ 6 in.Hg.  
 Pretest Leak Check: Pitot: 1.5 Orsat: — Stack Diameter: 16.8 K: 60.573 Post-Test Leak Check: Pitot: 1.5 Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp. Tm		Pump Vacuum (in. Hg)
					Desired	Actual	Probe	Filter			Inlet	Outlet	
0 0		0955	342.762										
1 5		1000	346.3	0.04	1.7	1.7	260	244	68		66	65	1
2 10		1005	350.4	0.04	1.7	1.7	268	255	67		67	65	1
3 15		1010	353.1	0.04	1.7	1.7	260	254	62		72	66	1
4 20		1015	356.8	0.04	1.7	1.7	250	242	63		73	67	1
5 25		1020	359.7	0.035	1.4	1.4	245	248	63		75	68	1
6 30		1025	362.870	0.035	1.4	1.4	240	250	64		77	69	1
7 35		1030	366.0	0.035	1.4	1.4	271	253	65		78	70	1
8 40		1035	370.2	0.040	1.7	1.7	270	243	56		78	70	1
9 45		1040	373.0	0.040	1.7	1.7	240	248	51		80	72	1
10 50		1045	376.5	0.04	1.7	1.7	247	244	50		81	72	1
11 55		1050	380.1	0.04	1.7	1.7	250	248	50		82	73	1
12 60		1055	383.6	0.04	1.7	1.7	251	249	51		84	74	1
13 65		1100	387.1	0.04	1.7	1.7	251	251	52		87	76	1
14 70		1105	390.8	0.05	2.0	2.0	248	249	53		87	76	1
15 75		1110	394.4	0.05	2.0	2.0	251	248	55		87	77	1
16 80		1115	398.4	0.04	1.7	1.7	250	249	54		87	78	1
17 85		1120	402.0	0.04	1.7	1.7	249	247	56		89	79	1
18 90		1125	405.6	0.04	1.7	1.7	252	248	57		89	80	1
19 95		1130	409.1	0.04	1.7	1.7	249	246	57		90	80	1
20 100		1135	412.6	0.035	1.4	1.4	253	250	58		90	82	2
21 105		1140	415.9	0.035	1.4	1.4	251	247	58		90	82	2
22 110		1145	419.3	0.040	1.7	1.7	251	254	59		90	82	2
23 115		1150	423.1	0.040	1.7	1.7	251	249	58		91	83	2
24 120		1155	426.554	0.040	1.7	1.7	250	250	58		91	83	2

$$\Delta V_m = 83.787 \sqrt{\Delta p} = 0.1993 \quad \Delta H = 1.66 \quad T_s = 358$$

0.0398

$$T_m = 79$$

✓ 88

## SAMPLE RECOVERY DATA

Plant AK MIDDLETOWN Run No. C-315-3  
 Date 9/14/ Sample Box No. SB-4 Job No. 052074.0172  
 Sample Location COMBUSTION Filter No. QZ-3101  
 Train Preparer BF Sample Head No. SH-1  
 Sample Recovery Person BF/RK Barometer No. FB-2 INCLON  
 Comments 315 Balance No. FB-2

Front Half

Acetone

Liquid

 Container No. C-35-3 Level Marked ☒ Sealed ☒
Filter
 Container No. QZ-3101 Sealed ☒

 Description of Filter black

 Samples Stored and Locked ☒
Back Half/Moisture
 Container No. NA

 Liquid Level Marked NA Sealed NA

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	H <sub>2</sub> O	100	775.0	919.7	144.7
2	H <sub>2</sub> O	100	759.5	793.2	33.7
3	—	—	669.1	671.6	2.5
4	Silica Gel	250	909.9	938.3	28.4
5					
6					
Total					209.3

 Description of Impinger Catch: clear

✓BF

## **FILTERABLE PM AND HAP METALS**

## FIELD DATA SHEET

pg 1 of 3

Plant: AK Middleton  
 Sampling Location: Bayhouse #3  
 Run Number: 8-29-16 Date: 8-29-16  
 Pretest Leak Rate: .00 scfm @ 10 in. Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: —

Sample Type: M29 Operator: GD  
 Pbar: 30.11 Ps: -2.0  
 CO<sub>2</sub>: CEA O<sub>2</sub>: CEA  
 Probe Length/Type: 3.6/Pitot# 73-4  
 Stack Diameter: 35.5" K: 0.6106

Nozzle ID: 0.156 Thermocouple #: T3-4  
 Assumed Bws: 1.7 Filter #: QZ 2960  
 Meter Box #: 13 Y: 0.989 AH@: 1.723  
 Post-Test Leak Rate: .001 cfm @ 5 in. Hg. End of  
 Post-Test Leak Check: Pitot: ✓ Orsat: — Day 1

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	10:24	004.071											
1	3:20	10:27	006.660	3.3	1.9	1.9	100	251	260	63	238	67	66	3.0
2	6:38	10:39	009.238	3.3	1.9	1.9	112	250	258	60	240	69	67	3.0
3	9:47	10:49	011.587	2.8	1.6	1.6	123	259	254	59	241	70	69	2.0
4	13:01	10:53	013.921	2.9	1.6	1.6	120	258	254	57	241	71	70	2.0
5	16:30	11:04	016.466	3.2	1.8	1.8	124	257	260	59	240	72	71	2.0
6	19:36	11:40	018.930	3.2	1.8	1.8	121	259	260	60	243	74	73	2.0
1	22:53	11:59	021.413	3.1	1.7	1.7	122	259	260	57	245	74	74	2.0
2	26:17	12:02	023.945	3.0	1.7	1.7	125	258	259	58	244	76	75	2.0
3	29:35	12:31	026.473	3.2	1.8	1.8	121	257	260	57	248	77	77	2.0
4	33:00	12:59	029.014	3.2	1.8	1.8	120	260	258	58	247	78	78	2.0
5	36:18	13:11	031.405	2.8	1.6	1.6	125	250	260	59	244	80	79	2.0
6	39:33	13:22	033.790	2.8	1.6	1.6	122	254	259	58	249	80	79	2.0
1	42:49	13:45	036.179	2.8	1.6	1.6	126	252	257	57	248	81	80	2.0
2	46:12	14:00	038.745	3.1	1.8	1.8	116	254	258	58	239	82	82	2.0
3	49:31	14:26	041.285	3.1	1.8	1.8	122	253	254	59	237	82	82	2.0
4	52:55	15:06	043.887	3.1	1.8	1.8	123	257	260	60	240	82	82	2.0
5	56:18	15:21	046.428	3.3	1.9	1.9	121	256	259	59	241	82	82	2.0
6	59:43	15:43	049.064	3.3	1.9	1.9	120	258	259	60	238	82	82	2.0
1	62:54	15:57	051.519	3.4	1.9	1.9	124	252	258	57	239	82	82	2.0
2	66:28	16:14	054.208	3.2	1.8	1.8	123	253	260	56	237	82	82	2.0
3	69:56	16:35	056.837	3.2	1.8	1.8	122	260	260	57	240	82	82	2.0
4	73:20	16:59	059.457	3.3	1.9	1.9	121	250	258	59	238	82	82	2.0
5	76:43	17:06	062.036	3.1	1.8	1.8	124	257	259	60	237	82	81	2.0
6	80:01	17:28	064.565	3.2	1.8	1.8	123	255	260	59	240	82	81	2.0
1	83:31	17:40	067.390	3.2	1.8	1.8	120	253	261	57	238	82	81	2.0

$$\Delta V_m = 63.319 \sqrt{\Delta p} = \frac{\Delta H}{T_s} = T_m =$$

(15 DAY VOLUME)



Plant: AK Middletown Sample Type: MZ9 Operator: GA Nozzle ID: 8.156 Thermocouple #: T3-4  
 Sampling Location: Baghouse #3 Pbar: 30.23 Ps: -2.0 Assumed Bws: 1.7 Filter #: QZ 2960  
 Run Number: P-29-1 Date: 8-30-16 CO<sub>2</sub>: CEM O<sub>2</sub>: CEM Meter Box #: 13 Y: 0.289 ΔH@: 1.783  
 Pretest Leak Rate: 0.01 cfm @ 11 in.Hg. Probe Length/Type: 3' G1 Pitot#: T3-4 Post-Test Leak Rate: cfm @ in.Hg. Final  
 Pretest Leak Check: Pitot: ✓ Orsat: — Stack Diameter: 35.5" K: 0.6106 Post-Test Leak Check: Pitot: ✓ Orsat: —

Transpose Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	83:31	1026	067.410		1.7	1.7	105	258	259	63	240	67	67	2.0
2	86:47	1029	069.876	3.0	1.7	1.7	105	255	259	57	239	70	69	2.0
3	90:06	1043	072.383	3.0	1.7	1.7	110	257	259	58	241	72	71	2.0
4	93:29	1102	074.933	3.0	1.7	1.7	108	254	259	59	238	73	72	2.0
5	96:50	1139	077.464	2.9	1.7	1.7	112	260	258	58	240	75	74	2.0
6	100:14	1201	080.040	3.2	1.8	1.8	116	261	261	57	241	76	75	2.0
1	103:36	1211	082.605	3.2	1.8	1.8	119	259	258	59	238	76	75	2.0
2	106:57	1221	085.105	3.1	1.8	1.8	122	263	261	60	240	77	76	2.0
3	110:14	1231	087.548	3.1	1.7	1.7	123	260	258	58	238	78	77	1.5
4	113:35	1245	090.100	3.1	1.7	1.7	121	254	259	54	239	78	78	1.5
5	117:01	1302	092.727	3.1	1.8	1.8	122	256	257	54	238	79	78	1.5
6	120:23	1316	095.263	3.2	1.8	1.8	125	258	258	56	237	80	80	1.5
1	123:52	1338	097.834	3.1	1.7	1.7	126	256	257	57	238	81	80	1.5
2	125:09	1345	098.342	2.9	1.6	1.6	126	255	259	59	238	81	80	1.5
3	128:40	1351	101.407	2.9	1.6	1.6	122	256	258	61	239	82	82	1.5
4	131:53	1445	103.835	3.2	1.8	1.8	121	261	259	60	240	82	82	1.5
5	135:19	1458	106.481	3.2	1.8	1.8	122	260	259	58	238	83	83	1.5
6	138:24	1508	108.798	3.3	1.9	1.9	125	251	260	59	239	83	83	1.5
7	141:42	1535	111.272	3.0	1.7	1.7	124	250	258	59	240	83	83	1.5
8	144:59	1542	113.760	3.0	1.7	1.7	122	252	259	59	239	83	83	1.5
9	148:23	1553	116.288	3.1	1.8	1.8	122	252	259	58	238	83	83	1.5
10	151:48	1619	118.871	3.0	1.7	1.7	122	257	259	60	241	83	83	1.5
11	155:08	1633	121.350	3.0	1.7	1.7	123	258	259	58	239	83	83	1.5
12	158:32	1654	123.865	2.9	1.7	1.7	122	257	260	57	240	83	83	1.5
13	161:57	1708	126.402	3.1	1.8	1.8	119	256	259	58	242	82	83	1.5
14	165:24	1728	129.020	3.1	1.8	1.8	122	255	259	56	239	82	82	1.5

ΔV<sub>m</sub> = $\sqrt{\Delta p}$  =

ΔH =

Ts =

Tm =

Leak  
check  
-0.02ONE  
BackPort  
Change

## FIELD DATA SHEET

Plant: AK Middleton Sample Type: M29 Operator: GD  
 Sampling Location: Baghouse #3 Pbar: 30.23 Ps: -2.0  
 Run Number: 8-24-1 Date: 8-30-16 CO<sub>2</sub>: CEM O<sub>2</sub>: C<sub>EM</sub>  
 Pretest Leak Rate: .001 cfm @ 11 in.Hg. Probe Length/Type: 3' 61 Pitot#: 73-4  
 Pretest Leak Check: Pitot: ✓ Orsat: — Stack Diameter: 35.5" K: 0.6106

[illegible]

Final  $\rightarrow$  Readings

$\Delta V_m = 126.979$	$\sqrt{\Delta p} = 1.7585$	$\Delta H = 1.76$	$T_s = 120$
		$\Delta \bar{P} = 3.0941$	



## SAMPLE RECOVERY DATA

Plant AK Middletown Run No. P-5/29-1  
 Date 8/30/16 Sample Box No. SB-3 Job No. 050074.0172  
 Sample Location Pressure BH Filter No. Q22960  
 Train Preparer EZ Sample Head No. 12  
 Sample Recovery Person BF/CS Barometer No. TUC.com  
 Comments M29-metals Balance No. 2

Front Half

Acetone Liquid  
 Container No. P-29-1 Level Marked ☒ Sealed ☒  
ACE

## Filter

Container No. Q22960 Sealed ☒

Description of Filter light grey loady

Samples Stored and Locked ☒

Back Half/Moisture

Container No. P-29-1 IMPS 1-3 / IMP 4 / KMnO<sub>4</sub> / MRS / 8N HCl

Liquid Level Marked ☒ Sealed ☒

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1			<del>777.1</del>		
2	5% HNO <sub>3</sub> / 10% H <sub>2</sub> O <sub>2</sub>	100	777.1	810.9	+ 33.8
3	5% HNO <sub>3</sub> / 10% H <sub>2</sub> O <sub>2</sub>	100	770.0	777.8	+ 7.8
4			674.9	676.2	+ 1.3
5	4% KMnO <sub>4</sub> / 10% H <sub>2</sub> SO <sub>4</sub>	100	781.4	781.2	- 0.2
6	4% KMnO <sub>4</sub> / 10% H <sub>2</sub> SO <sub>4</sub>	100	782.5	782.8	+ 0.3
7	Total Silica Gel	250g	931.8	955.1	+ 23.3
Total					66.3

Description of Impinger Catch: clear , 024

✓ EZ

EQM

AK Middleton

## FIELD DATA SHEET

pg 1 of 2

T3-4

Nozzle ID: 156 Thermocouple #: 156  
 Assumed Bws: 1.7 Filter #: QE2959  
 Meter Box #: 13 Y: 929 ΔH@: 1.733  
 Post-Test Leak Rate: 100 cfm @ 3 in.Hg.  
 Post-Test Leak Check: Pitot: ✓ Orsat: —

Sample Type: M29 Operator: GD  
 Pbar: 3005 Ps: 2.0  
 CO<sub>2</sub>: CEM O<sub>2</sub>: CEM  
 Probe Length/Type: 3' 61 Pitot#: T3-4  
 Stack Diameter: 35.5"K: .6106

Plant: AK Middleton  
 Sampling Location: P Bayhove 3  
 Run Number: P-29-2 Date: 8-31-16  
 Pretest Leak Rate: 001 cfm @ 10 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	1020	131.400											
1	3:21	1024	133.885	3.0	1.7	1.7	98	244	256	64	238	68	68	1.0
2	6:49	1035	136.513	2.9	1.7	1.7	107	258	257	60	239	69	69	1.0
3	10:03	1042	138.873	2.9	1.6	1.6	118	250	257	58	237	70	70	1.0
4	13:22	1052	141.257	3.0	1.7	1.7	121	256	258	59	238	71	71	1.0
5	16:49	1123	143.780	3.0	1.7	1.7	123	260	257	58	239	72	72	1.0
6	20:21	1155	146.362	3.0	1.7	1.7	122	260	259	59	240	73	73	1.0
1	23:51	1200	148.938	3.2	1.8	1.8	121	262	260	57	238	74	74	1.0
2	27:24	1220	151.628	3.2	1.8	1.8	122	263	260	56	241	75	75	1.0
3	30:53	1239	154.277	3.2	1.8	1.8	122	265	260	57	239	76	76	1.0
4	34:21	1257	156.860	3.0	1.7	1.7	121	256	260	57	238	77	77	1.0
5	37:49	1320	159.413	3.0	1.7	1.7	120	260	261	59	239	78	78	1.0
6	41:21	1335	162.095	3.0	1.7	1.7	116	258	258	60	238	79	79	1.0
1	44:52	1345	164.726	3.0	1.7	1.7	118	261	260	59	239	80	80	1.0
2	48:07	1428	167.174	3.1	1.8	1.8	111	256	261	58	238	79	80	1.0
3	51:26	1459	169.621	3.1	1.8	1.8	115	254	259	57	237	79	79	1.0
4	54:42	1510	172.054	3.2	1.8	1.8	112	250	260	58	237	79	79	1.0
5	58:12	1525	174.767	3.1	1.8	1.8	117	252	260	59	238	79	79	1.0
6	61:32	1543	177.363	3.2	1.8	1.8	110	256	260	58	240	78	78	1.0
1	64:51	1600	179.933	3.2	1.8	1.8	112	254	259	60	240	77	77	1.0
2	68:14	1617	182.525	3.3	1.9	1.9	110	257	260	58	237	77	77	1.0
3	71:32	1637	185.134	3.4	1.9	1.9	112	257	258	59	238	76	76	1.0
4	75:10	1653	188.020	3.4	2.0	2.0	108	251	259	56	236	75	75	1.0
5	78:34	1713	190.768	3.5	2.0	2.0	100	261	260	57	235	75	75	1.0
6	81:52	1730	193.475	3.5	2.0	2.0	98	260	258	58	237	73	73	1.0
1	85:05	1737	196.109	3.5	2.0	2.0	99	261	259	59	236	73	73	1.0
1	85:05	1740												

LEAK ✓

196.109

196.268

ΔV<sub>m</sub> = 196.109 00008" $\sqrt{\Delta p}$  = 196.268ΔH = 196.268Ts = 196.268Tm = 196.268

## FIELD DATA SHEET

pg. 2 of 2

Plant: AK Middletown Sample Type: M29 Operator: GD Nozzle ID: .156 Thermocouple #: T3-4  
 Sampling Location: P Baghouse 3 Pbar: 30.08 Ps: -2.0 Assumed Bws: 1.7 Filter #: QZ2959  
 Run Number: P-29-2 Date: 9-1-16 CO<sub>2</sub>: CEM O<sub>2</sub>: CEM Meter Box #: 13 Y: .989 AH@: 1.783  
 Pretest Leak Rate: 0.001 cfm @ 10 in.Hg. Probe Length/Type: 3'61" Pitot#: T3-4 Post-Test Leak Rate: 0.001 cfm @ 4 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: - Stack Diameter: 35.5" K: .6106 Post-Test Leak Check: Pitot: ✓ Orsat: -

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	85:05	10:20	196.488											
2	88:23	10:23	199.038	3.5	2.0	2.0	99	251	259	59	236	66	67	1.0
3	91:42	10:35	201.637	3.5	2.0	2.0	98	250	260	54	237	67	67	1.0
4	95:05	10:47	204.270	3.4	1.9	1.9	107	250	258	52	239	66	66	1.0
5	98:25	10:50	206.946	3.3	1.9	1.9	108	260	258	53	240	66	66	2.0
6	101:43	11:30	209.475	3.1	1.7	1.7	110	252	259	54	237	66	66	2.0
1	105:05	11:42	211.981	3.0	1.7	1.7	110	254	260	53	238	66	66	2.0
2	108:25	12:04	214.432	3.1	1.8	1.8	107	260	259	54	238	67	66	1.5
3	111:50	12:13	217.033	3.3	1.9	1.9	105	261	259	57	239	67	67	1.5
4	115:14	12:38	219.695	3.2	1.8	1.8	114	259	258	57	237	68	67	1.5
5	118:26	12:57	222.017	3.1	1.7	1.7	115	256	260	58	237	68	68	1.5
6	121:54	13:16	224.789	3.1	1.8	1.8	110	255	259	59	240	69	68	1.5
1	125:24	13:35	227.320	3.1	1.8	1.8	111	260	260	60	237	69	68	1.0
2	128:41	13:45	229.785	3.1	1.8	1.8	112	254	259	58	238	70	69	1.0
3	132:00	14:15	232.274	3.2	1.8	1.8	106	258	260	57	236	70	70	1.0
4	135:14	14:52	234.756	3.3	1.9	1.9	112	258	259	56	239	70	70	1.5
5	138:31	15:10	237.262	3.3	1.9	1.9	110	260	261	58	240	70	70	1.5
6	141:45	15:25	239.642	3.2	1.8	1.8	116	256	261	59	239	71	70	1.5
1	144:58	15:42	242.087	3.2	1.8	1.8	111	256	258	60	238	70	70	1.5
2	148:06	16:05	244.457	3.2	1.8	1.8	110	250	259	60	240	70	70	1.5
3	151:30	16:20	246.941	3.3	1.9	1.9	112	251	259	61	239	70	70	1.5
4														
5														
6														
1														
2														

115.162.62

Final → ΔV<sub>m</sub> = 45.544 √Δp = 1.7845 ΔH = 1.81 Ts = 111 Tm = 72  
~~379 (leak checks)~~ ΔP = 3,1866

✓ E2

## SAMPLE RECOVERY DATA

8/31 -  
9/1

Plant At steel Middletown Run No. P-29-2  
 Date 8/31/16 Sample Box No. SB-3 Job No. SW740172  
 Sample Location Pushing Bay house Filter No. Q2 2959  
 Train Preparer DA Sample Head No. 12  
 Sample Recovery Person DA Barometer No. W.C. van  
 Comments Method 5729 Balance No. 2

Front Half

Acetone P-29-2 Liquid  
 Container No.                      Level Marked                      Sealed                     

Filter

Container No. Q22959 Sealed                      ✓

Description of Filter Log Lt Gray

Samples Stored and Locked                     

Back Half/Moisture

Container No. 9 HNO<sub>3</sub>/H<sub>2</sub>O, 4th empty / HCl

Liquid Level Marked                      Sealed                     

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	5% HNO <sub>3</sub> /10% H <sub>2</sub> O	100	780.2	807.8	27.6
2	5% HNO <sub>3</sub> /10% H <sub>2</sub> O	100	773.5	779.7	6.2
3	empty	—	678.4	679.6	1.2
4	km only	100	785.3	784.2	-1.1
5	km only	100	786.8	786.5	-0.3
6	SL	250	905.8	925.7	19.9
Total					53.5

Description of Impinger Catch:                     

✓ E2

Purple  
8/31 pm  
9/1 AM/PM

EQM

P-5/29-3

## FIELD DATA SHEET

pg 1 of 2

Plant: AK Middlefield Sample Type: MS/202 Operator: GDSampling Location: Bayhouse #3Pbar: 30.20 Ps: -2.0Run Number: P-5/29-3 Date: 9/6/16CO<sub>2</sub>: CEM O<sub>2</sub>: CEMPretest Leak Rate: 0.03 cfm @ 8 in.Hg.Probe Length/Type: 3' 6" / Pitot# 13-4Pretest Leak Check: Pitot: ✓ Orsat: -Stack Diameter: 35.5" K: .6106Nozzle ID: .156 Thermocouple #: T3-4  
Assumed Bws: 1.7 Filter #: QZ 2961  
Meter Box #: 13 Y: 0.489 ΔH@: 1.783  
Post-Test Leak Rate: 0.01 cfm @ 10 in.Hg.  
Post-Test Leak Check: Pitot: ✓ Orsat: -

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg.)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	10:26	247.319											
1	3:14	10:29	249.758	3.3	1.9	1.9	100	258	260	58	236	70	70	1.0
2	6:30	10:38	252.183	3.2	1.8	1.8	108	261	261	57	238	71	71	1.0
3	9:49	10:41	254.675	3.4	1.9	1.9	111	262	259	56	239	72	71	1.0
4	13:51	10:54	257.725	3.4	1.9	1.9	112	258	258	57	240	73	73	1.0
5	17:08	11:01	260.214	3.4	1.9	1.9	114	261	258	56	241	74	74	1.0
6	20:23	11:05	262.818	3.4	1.9	1.9	116	262	260	55	240	76	75	1.0
1	23:42	12:00	265.432	3.3	1.9	1.9	117	260	258	57	239	77	76	1.0
2	27:05	12:04	268.177	3.4	1.9	1.9	117	261	260	58	239	77	77	1.0
3	30:23	12:05	270.775	3.2	1.8	1.8	121	259	260	56	240	79	78	1.0
4	33:44	12:08	273.188	3.3	1.9	1.9	120	262	260	57	238	80	80	1.0
5	36:58	13:16	275.669	3.2	1.8	1.8	120	258	260	58	239	82	81	1.0
6	40:14	13:37	278.144	3.1	1.7	1.7	129	258	261	59	240	82	82	1.0
1	43:40	13:40	280.815	3.2	1.8	1.8	129	262	259	58	240	82	82	1.0
2	47:04	14:41	283.234	2.7	1.5	1.5	122	254	261	59	239	82	82	1.0
3	50:20	14:55	285.515	2.7	1.5	1.5	133	258	259	57	240	82	82	1.0
4	53:38	15:01	287.823	2.8	1.6	1.6	131	263	260	59	239	82	82	1.0
5	56:49	15:25	290.130	3.0	1.7	1.7	128	253	259	55	239	82	82	1.0
6	60:08	15:42	292.502	3.0	1.7	1.7	127	256	258	56	238	82	82	1.0
1	63:27	15:59	295.065	3.0	1.7	1.7	129	252	263	57	240	82	82	1.0
2	66:39	16:19	297.676	3.2	1.8	1.8	130	261	257	57	241	83	82	1.0
3	69:59	16:37	300.215	3.2	1.8	1.8	128	259	257	58	241	83	82	1.0
4	73:14	16:53	302.671	3.2	1.8	1.8	127	261	255	58	238	83	83	1.0
5	76:35	17:08	305.177	3.2	1.8	1.8	129	258	262	59	239	83	83	1.0
6	79:46	17:38	307.587	3.1	1.7	1.7	128	259	260	58	240	83	83	1.0
1	83:06	17:58	310.132	3.2	1.8	1.8	124	262	261	57	239	83	83	1.0

Pitot Change

$$\Delta Vm = 68.813 \sqrt{\Delta p} = \quad \Delta H = \quad Ts = \quad Tm = \quad$$



EQM P-5729-3

FIELD DATA SHEET

pg 2 of 2

Plant: AK Middle town Sample Type: M5/202 Operator: GD Nozzle ID: .156 Thermocouple #: T3-4  
Sampling Location: Baghouse #3 Pbar: 30.16 Ps: -2.0 Assumed Bws: 1.7 Filter #: QE29601  
Run Number: P-5729-3 Date: 9/7/16 CO<sub>2</sub>: CEM O<sub>2</sub>: CEM Meter Box #: 13 Y: 0.989AH@: 1.783  
Pretest Leak Rate: .001 cfm @ 5 in.Hg. Probe Length/Type: 3' 61 Pitot#: T3-4 Post-Test Leak Rate: .001 cfm @ 3 in.Hg.  
Pretest Leak Check: Pitot: ✓ Orsat: — Stack Diameter: 35.5" K: .6106 Post-Test Leak Check: Pitot: ✓ Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. of	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	83:06	1051	310.382											
2	86:22	1054	312.867	3.1	1.8	1.8	106	254	260	60	240	72	72	1.0
3	89:41	1057	315.335	3.0	1.7	1.7	118	262	258	56	239	75	74	1.0
4	92:52	1120	317.778	2.8	1.6	1.6	127	261	260	55	241	76	75	1.0
5	96:06	1123	320.209	3.1	1.7	1.7	133	260	259	54	240	77	76	1.0
6	99:25	1141	322.672	3.1	1.7	1.7	134	260	259	55	238	78	77	1.0
1	102:38	1154	325.126	3.2	1.8	1.8	130	259	259	56	239	78	77	1.0
2	105:52	1506	327.563	3.2	1.8	1.8	123	262	259	55	240	82	82	1.0
3	109:11	1520	330.106	3.2	1.8	1.8	124	260	260	56	237	84	84	1.0
4	112:21	1534	332.488	3.0	1.7	1.7	124	264	258	55	239	86	85	1.0
5	115:42	1550	335.038	3.1	1.8	1.8	127	262	258	57	238	86	86	1.0
6	119:05	1604	337.643	3.1	1.8	1.8	128	260	258	58	237	87	86	1.0
1	122:25	1616	340.217	3.1	1.8	1.8	129	263	260	59	237	87	86	1.0
2	125:42	1629	342.761	3.2	1.8	1.8	129	263	260	58	238	87	87	1.0
3	128:56	1643	345.261	3.2	1.8	1.8	127	258	261	57	237	87	87	1.0
4	132:17	1659	347.807	3.0	1.7	1.7	129	262	259	58	239	86	86	1.0
5	135:34	1715	350.336	3.1	1.8	1.8	125	260	260	59	240	85	85	1.0
6	138:56	1725	352.999	3.1	1.8	1.8	124	259	259	57	238	85	85	1.0
1	142:29	1739	355.653	3.1	1.8	1.8	126	258	257	58	239	84	84	1.0
2	145:41	1753	358.138	3.1	1.8	1.8	127	259	260	57	240	84	84	1.0
3														
4														
5														
6														
1														
2														

ΔV<sub>m</sub> =  $\frac{110.569}{\sqrt{1.77}}$  ΔH =  $\frac{1.77}{4.77-T_s}$  = 124  
ΔP =  $\frac{6.3-13573.1341}{60}$  T<sub>m</sub> =  $\frac{60}{80}$  81  
- .25 from leak checks



## SAMPLE RECOVERY DATA

Plant KK Steel Middletown Run No. P-5729-3  
 Date 9/7/16 Sample Box No. SB-3 Job No. 50074.0172  
 Sample Location Pushing Bay, Lorse Filter No. QZ 2961  
 Train Preparer CS Sample Head No. 12  
 Sample Recovery Person DA Barometer No. TWC  
 Comments M 5/29 Balance No. 2

Front Half

Acetone/ $HNO_3$  Liquid  
 Container No. P-5729-3 Level Marked — Sealed ✓

Filter

Container No. QZ 2961 Sealed ✓

Description of Filter Light Gray

Samples Stored and Locked ✓

Back Half/Moisture

Container No.  $HNO_3/H_2O_2$ ; 4th Sep;  $KMnO_4$ ; HCL

Liquid Level Marked — Sealed —

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	5% $HNO_3$ /10% $H_2O_2$	100	779.1	808.5	29.4
2	5% $HNO_3$ /10% $H_2O_2$	100	772.4	780.9	8.5
3	—	—	676.7	677.7	1.0
4	$KMnO_4$	100	794.4	792.8	-1.6
5	$KMnO_4$	100	769.0	769.0	0
6	SC	250	928.9	950.6	21.7
Total					59.0

Description of Impinger Catch: Clear - Runway Purple @ end

✓ 122

Plant: AK Steel Mid-Durham Sample Type: 5/29 Operator: NP  
 Sampling Location: Conveyer 57th St Pbar: 30.20 Ps: -0.80  
 Run Number: 6-5/29-1 Date: 9/16/16 CO<sub>2</sub>: 0.48 O<sub>2</sub>: 15  
 Pretest Leak Rate: 0.002 cfm @ 10 in.Hg. Probe Length/Type: 6' 6" Pitot#: 76-157  
 Pretest Leak Check: Pitot: ✓ Orsat: — Stack Diameter: 16 1/2" K: 53.113

Nozzle ID: 02500 Thermocouple #: 76-157  
 Assumed Bws: 10 Filter #: QZ 2956  
 Meter Box #: 2 Y: 1.005 ΔH@: 16.87  
 Post-Test Leak Rate: — cfm @ — in.Hg.  
 Post-Test Leak Check: Pitot: — Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp. Tm		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	1002	770.192											
1	5	1007	773.03	.03	1.1	1.1	351	250	250	65	104	76	76	1
2	10	1012	775.8	.03	1.1	1.1	340	250	251	65		76	77	1
3	15	1017	778.2	.02	.7	.7	350	234	236	62		77	77	1
4	20	1022	780.9	.03	1.1	1.1	350	237	232	58		78	77	1
5	25	1027	784.2	.04	1.4	1.4	340	234	234	58		80	77	1
6	30	1032	787.5	.04	1.4	1.4	341	234	234	58		83	78	1
7	35	1037	790.8	.04	1.4	1.4	349	234	233	59		85	79	1
8	40	1042	794.3	.04	1.5	1.5	330	234	235	61		86	79	2
9	45	1047	798.0	.04	1.5	1.5	297	234	235	61		88	80	3
10	50	1052	801.7	.04	1.5	1.5	293	235	235	62		90	81	3
11	55	1057	805.3	.04	1.5	1.5	293	233	234	64		91	81	3
12	60	1102	809.1	.04	1.5	1.5	290	234	234	65		92	82	3
1	65	1107	812.8	.04	1.5	1.5	294	233	234	65		93	83	3
2	70	1112	816.7	.04	1.6	1.6	292	234	234	60		94	84	3
3	75	1117	820.5	.04	1.5	1.5	301	232	233	56		95	85	3
4	80	1122	824.2	.04	1.5	1.5	313	234	234	56		97	86	3
5	85	1127	827.9	.04	1.5	1.5	320	234	234	56		97	87	3
6	90	1132	831.7	.04	1.5	1.5	320	235	234	57		98	88	3
7	95	1137	835.3	.04	1.5	1.5	313	234	235	56		98	88	3
8	100	1142	838.8	.04	1.5	1.5	314	234	233	57		99	89	3
9	105	1147	842.3	.04	1.5	1.5	291	234	233	59		99	90	3
10	110	1152	845.8	.04	1.5	1.5	276	233	233	59		99	90	3
11	115	1157	849.3	.04	1.5	1.5	278	234	235	61		100	91	3
12	120	1202	852.9	.04	1.5	1.5	281	234	234	62	✓	100	92	3

$$\Delta V_m = \sqrt{\Delta p} = \frac{\Delta H}{T_s} = \frac{T_m}{T_s}$$

## FIELD DATA SHEET

Plant: AK Middleton Sample Type: 5/29 Operator: NP  
 Sampling Location: Combobox 01 Stack Pbar: 30.20 Ps: -.80  
 Run Number: 65/29/1 Date: 9-6-16 CO<sub>2</sub>: 3 O<sub>2</sub>: 13  
 Pretest Leak Rate: .001 cfm @ 10 in.Hg. Probe Length/Type: 6' GL Pitot#: 76-15P  
 Pretest Leak Check: Pitot: ✓ Orsat: - Stack Diameter: 168" K: 53.113

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
1	1207	125	856.6	.04	1.5	1.5	288	234	232	63	NA	101	92	3
2	1212	130	860.1	.04	1.5	1.5	283	234	234	63		101	92	3
3	1217	135	863.7	.05	1.9	1.9	305	234	236	58		102	93	3
4	1222	140	867.6	.05	1.9	1.9	325	234	236	57		103	94	3
5	1227	145	871.5	.05	1.9	1.9	327	233	233	57		104	95	3
6	1232	150	875.4	.05	1.9	1.9	318	235	235	57		105	95	3
1	1255	1237	879.3	.05	1.9	1.9	330	234	234	57		105	95	3
2	1300	1242	883.2	.05	1.9	1.9	335	233	234	57		105	96	3
3	1305	1247	887.1	.04	1.6	1.6	277	236	234	59		106	96	3
4	1310	1252	890.7	.04	1.6	1.6	288	235	234	60		106	97	3
5	1315	1257	894.2	.04	1.6	1.6	289	234	234	59		100	95	3
6	1320	1302	897.840	.04	1.6	1.6	297	234	234	59		100	95	3

$$\Delta V_m = \frac{127.6 \text{ eV}}{\sqrt{\Delta p}} \quad \sqrt{\Delta p} = .2001 \quad \Delta H = \frac{1.5167 T_s}{311}$$

Age D<sub>9</sub> = 0.403

## SAMPLE RECOVERY DATA

Plant AK MIDDLETOWN Run No. C-5/29-1  
 Date 9/6/16 Sample Box No. \_\_\_\_\_ Job No. 050074.0172  
 Sample Location COMBUSTION STAGE Filter No. QZ 2956  
 Train Preparer CS Sample Head No. SP-9  
 Sample Recovery Person CS Barometer No. TWC.COM  
 Comments 5/29 Balance No. 2

Front Half

Acetone C-5/29-1 Liquid  
 Container No. FRONT 112 Level Marked ACE / 0.1 w HNO<sub>3</sub> RINGE Sealed /

Filter

Container No. QZ-2956 Sealed /

Description of Filter black coating

Samples Stored and Locked /

Back Half/Moisture

Container No. C-5/29-1 IMP 1-3 / IMP 4 / KMnO<sub>4</sub> / H<sub>2</sub>O + 8N HCl

Liquid Level Marked / Sealed /

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	—	—	664.5	844.0	179.5
2	5% HNO <sub>3</sub> / 10% H <sub>2</sub> O <sub>2</sub>	100	779.0	853.6	74.6
3	5% HNO <sub>3</sub> / 10% H <sub>2</sub> O <sub>2</sub>	100	763.2	784.8	21.6
4	—	—	651.2	653.6	2.4
5	KMnO <sub>4</sub>	100	765.4	762.5	-2.9
6	KMnO <sub>4</sub>	100	805.3	807.6	2.3
7	Total SG	250	922.7	956.1	23.4

Description of Impinger Catch: clear / purple TOTAL 300.9

✓ E2

BWS = 10.2%

## FIELD DATA SHEET

Page 1 of 2

Plant:

AK Middleton

Sample Type:

5/29

Operator:

NP

Sampling Location: Combustion Stack

Pbar:

30.16

Ps:

-0.75"

Run Number: C-5/29-2

CO<sub>2</sub>:

3

O<sub>2</sub>:

15

Pretest Leak Rate: 1.02 cfm @ 11 in.Hg.

Probe Length/Type:

6' 64 Pitot#: T6-15P

Stack Diameter:

16.6" K: 53.113

Pretest Leak Check: Pitot:  $\sqrt{1}$  Orsat: —

Nozzle ID: 0.500

Thermocouple #:

T6-15P

Assumed Bws: 10

Filter #: Q2

2962

Meter Box #: 2

Y: 1.005

ΔH@: 1.687

Post-Test Leak Rate: — cfm @ — in.Hg.

Post-Test Leak Check: Pitot: —

Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	840	939.326											
1	5	845	942.6	.04	1.5	1.5	262	263	265	65	140	69	69	2
2	10	850	946.0	.04	1.5	1.5	269	265	267	64	151	70	69	2
3	15	855	949.5	.04	1.5	1.5	275	265	265	53	227	71	70	2
4	20	860	952.7	.03	1.2	1.2	261	265	265	52	244	73	70	2.5
5	25	865	956.0	.04	1.4	1.4	334	264	265	53	259	75	71	3
6	30	870	959.5	.04	1.4	1.4	324	264	264	54	267	77	72	3
7	35	875	963.0	.04	1.4	1.4	327	264	265	55	271	78	72	3
8	40	880	966.5	.04	1.4	1.4	328	264	264	56	275	80	73	3
9	45	885	970.0	.04	1.4	1.4	320	264	264	56	274	82	74	3
10	50	890	973.5	.04	1.5	1.5	328	265	265	57	277	84	75	3
11	55	895	977.0	.04	1.5	1.5	327	267	264	58	277	84	76	3
12	60	900	980.9	.04	1.5	1.5	329	264	263	58	276	85	77	3
1	65	905	984.0	.04	1.5	1.5	294	263	264	60	274	85	78	3
2	70	910	987.5	.04	1.5	1.5	302	264	264	60	274	85	78	3
3	75	915	991.1	.04	1.5	1.5	290	264	264	60	274	86	78	3
4	80	920	994.0	.04	1.5	1.5	303	265	265	63	273	86	79	3
5	85	925	998.2	.04	1.5	1.5	306	264	265	63	273	86	79	3
6	90	930	1001.7	.04	1.5	1.5	291	263	264	63	273	86	79	3
7	95	935	1005.2	.04	1.5	1.5	314	264	263	64	273	87	79	3
8	100	940	1008.8	.04	1.5	1.5	305	264	264	65	274	87	80	3
9	105	945	1012.4	.04	1.5	1.5	314	265	264	61	275	87	80	3
10	110	950	1015.9	.04	1.5	1.5	311	263	264	59	275	87	80	3
11	115	955	1019.5	.04	1.5	1.5	317	264	264	59	274	88	80	3
12	120	960	1023.0	.04	1.5	1.5	318	265	264	59	275	88	80	3

ΔV<sub>m</sub> = $\sqrt{\Delta p}$  =

ΔH =

Ts =

Tm =



## SAMPLE RECOVERY DATA

Plant AK Steel - Middletown Run No. C-29-2  
 Date 6/7/16 Sample Box No. H50-4 Job No. 52074.0172  
 Sample Location Combustion Stack Filter No. QZ 2962  
 Train Preparer DA Sample Head No. 9  
 Sample Recovery Person DA Barometer No. TWC.com  
 Comments Moq Metals Balance No. 2

Front Half

Acetone/HN<sub>3</sub> Liquid  
 Container No. C-29-2 Level Marked        Sealed       

Filter

Container No. QZ 2962 Sealed ✓

Description of Filter Black Loading

Samples Stored and Locked ✓

Back Half/Moisture

Container No. 4 HN<sub>3</sub>/H<sub>2</sub>O<sub>2</sub>; 4th Impinger, KMnO<sub>4</sub>, HCL

Liquid Level Marked        Sealed       

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	empty	—	669.3	850.9	181.6
2	5% / 10%	1W	780.5	855.6	75.1
3	5% i/HN <sub>3</sub> / 10% KMnO <sub>4</sub>	1W	767.1	783.9	16.8
4	empty	—	653.2	655.9	2.7
5	KMnO <sub>4</sub>	1W	774.7	775.1	0.4
6	KMnO <sub>4</sub>	1W	803.9	804.3	0.4
Total					303.0

Description of Impinger Catch: Clear - purple KMnO<sub>4</sub>

7	SG	250	935.7	961.7	26.0
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BWS = 10.2%  
 ISO = 100.2%

✓  
 EZ

Plant: AK Middleton

Sample Type: 5/29 Operator: NP

Sampling Location: COMBUSTION STACK

Pbar: 30.16 Psi: 75

Run Number: C-5/29-3 Date: 9-7-16

CO<sub>2</sub>: 3 O<sub>2</sub>: 15

Pretest Leak Rate: 2.1 cfm @ 10 in.Hg.

Probe Length/Type: 6' 6L Pitot#: 76-5P

Pretest Leak Check: Pitot: 1.5 Orsat: -

Stack Diameter: 168" K: 53.113

Nozzle ID: 500 Thermocouple #: 76-5P

Assumed Bws: 10 Filter #: Q72453

Meter Box #: 2 Y: 1005 ΔH@: 1.637

Post-Test Leak Rate: 2 cfm @ 10 in.Hg.

Post-Test Leak Check: Pitot: 1.5 Orsat: -

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	1230	65.820											
1	5	1235	69.7	.04	1.6	1.6	268	259	266	65	153	83	83	3
2	10	1240	73.1	.04	1.6	1.6	273	264	268	58	229	84	84	3
3	15	1245	76.8	.04	1.6	1.6	285	267	266	58	233	85	84	3
4	20	1250	80.5	.04	1.6	1.6	293	263	266	59	243	87	84	3
5	25	1255	84.0	.04	1.6	1.6	286	265	265	58	250	90	84	3
6	30	1300	87.7	.04	1.6	1.6	277	264	263	61	252	92	85	3
7	35	1305	91.3	.04	1.6	1.6	278	263	263	64	254	94	86	3
8	40	1310	94.8	.04	1.6	1.6	282	263	263	64	255	95	86	3
9	45	1315	98.4	.04	1.6	1.6	289	263	263	64	255	95	87	3
10	50	1320	102.4	.04	1.6	1.6	263	266	265	65	256	95	87	3
11	55	1325	105.7	.04	1.6	1.6	267	264	264	65	255	96	88	3
12	60	1330	109.4	.04	1.6	1.6	272	263	263	65	259	97	88	3
1	65	1335	113.1	.04	1.6	1.6	278	262	263	64	259	97	89	3
2	70	1340	116.8	.04	1.6	1.6	275	263	263	60	261	98	89	3
3	75	1345	120.4	.04	1.6	1.6	276	265	264	60	261	98	89	3
4	80	1350	124.1	.04	1.6	1.6	287	268	264	61	259	98	90	3
5	85	1355	127.6	.04	1.6	1.6	281	263	266	61	258	99	90	3
6	90	1400	131.4	.04	1.6	1.6	285	264	264	62	258	99	90	3
7	95	1405	135.2	.04	1.6	1.6	291	264	263	64	258	100	90	3
8	100	1410	138.8	.04	1.6	1.6	281	264	264	67	260	99	91	3
9	105	1415	142.5	.04	1.6	1.6	281	265	264	65	261	99	91	3
10	110	1420	146.5	.04	1.6	1.6	263	263	266	61	260	99	91	3
11	115	1425	149.8	.04	1.6	1.6	271	265	264	60	260	99	92	3
12	120	1430	153.6	.04	1.6	1.6	280	265	264	59	261	99	92	3

$$\Delta V_m = \sqrt{\Delta p} = \frac{\Delta H}{T_s} = \frac{T_m}{T_s}$$





**SAMPLE RECOVERY DATA**

Plant AK Middletown Run No. C-29-3  
 Date 9/7/10 Sample Box No. HSB-4 Job No. 50074.0172  
 Sample Location Combustion Filter No. QZ 2958  
 Train Preparer EZ/DA Sample Head No. 9  
 Sample Recovery Person DA Barometer No. RWC  
 Comments M29-Metals Balance No. 2

Front Half

Acetone/ $HNO_3$  Liquid  
 Container No. C-2983 Level Marked Sealed

Filter  
 Container No. QZ 2958 Sealed ✓

Description of Filter Black

Samples Stored and Locked ✓

Back Half/Moisture

Container No. 4  $HNO_3/H_2O_2$ , Empty,  $KMnO_4$ , HCL

Liquid Level Marked ✓ Sealed Sealed

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	—	—	651.9	889.6	237.7
2	5% $HNO_3$ / 10% $H_2O_2$	100	792.6	862.8	70.2
3	5% $HNO_3$ / 10% $H_2O_2$	100	780.6	795.6	15.0
4	—	—	662.3	664.5	2.2
5	4% $K_2NO_3$ / 10% $H_2SO_4$	100	780.1	778.7	-1.4
6	4% $K_2NO_3$ / 10% $H_2SO_4$	100	767.5	771.1	3.6
7	Total	250g	948.9	972.6	23.7
	Total				351.0

Description of Impinger Catch: clear

$KMnO_4$  - Purple

✓ EZ

**PM<sub>2.5</sub> FILTERABLE AND CONDENSABLE**

Plant: AK Middlebrook  
 Sampling Location: Bohose Stack 2  
 Run Number: FB-2022-1 Date: 8/29/16  
 Pretest Leak Rate: 0.022 cfm @ 10 in.Hg.  
 Pretest Leak Check: Pitot:  $\sqrt{1}$  Orsat: -

Sample Type: MS-202 Operator: EL  
 Pbar: 30.11 Ps: -0.85  
 CO<sub>2</sub>: LEA O<sub>2</sub>: CEM  
 Probe Length/Type: 3' 6" Pitot#1: T3-2  
 Stack Diameter: 35.5" K: 0.5221

Nozzle ID: Q148 Thermocouple #: T3-2  
 Assumed Bws: 2.5 Filter #: 832610  
 Meter Box #: 5 Y: 0.993 AH@: 1.906  
 Post-Test Leak Rate: 0.021 cfm @ 5 in.Hg. End of  
 Post-Test Leak Check: Pitot:  $\sqrt{1}$  Orsat: - Day 1

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	10:24	835.117											
1	3:29	12:41:27	837.275	2.5	1.2	1.2	93	263	268	65	80	68	68	4
2	6:46	10:36:37	839.248	2.5	1.1	1.1	104	260	265	65	81	70	70	3.5
3	9:49	10:49:52	841.189	2.4	1.2	1.2	124	262	265	64	82	71	71	3.5
4	12:56	11:03:06	843.117	2.5	1.3	1.3	118	264	265	63	82	72	72	3.5
5	16:19	11:21:24	845.116	2.6	1.2	1.2	124	257	264	62	84	73	73	3.5
6	19:48	11:40:43	847.335	2.7	1.3	1.3	120	257	265	63	84	75	74	3.5
1	23:13	11:59:22	849.359	2.8	1.3	1.3	120	266	266	62	84	75	75	3.5
2	26:38	12:17:21	851.407	2.6	1.2	1.2	131	257	264	61	83	77	76	3.5
3	30:00	12:41:45	853.404	2.4	1.1	1.1	130	259	264	62	82	78	77	3.5
4	33:22	12:55:59	855.420	2.6	1.3	1.3	125	261	266	63	82	78	77	3.5
5	36:40	13:01:14	857.427	2.4	1.2	1.2	127	258	264	64	82	81	71	3.5
6	40:02	13:22:25	859.450	2.5	1.2	1.2	128	263	264	61	80	81	80	3.5
1	43:26	13:45:49	861.448	2.2	1.1	1.1	122	256	265	62	81	82	81	3.5
2	46:56	14:00:44	863.623	3.0	1.5	1.5	113	264	266	61	81	83	83	4
3	50:17	14:02:56	865.835	3.0	1.5	1.5	120	268	265	60	82	83	82	4
4	53:47	15:06:10	868.100	3.1	1.5	1.5	125	265	267	61	81	83	83	4
5	57:07	15:22:25	870.215	2.8	1.3	1.3	129	262	264	62	80	83	83	3.5
6	60:33	15:40:43	872.418	2.9	1.4	1.4	123	264	265	63	79	84	83	4
1	63:51	15:57:40	874.591	3.2	1.5	1.5	127	254	262	64	79	83	83	4
2	67:22	16:14:18	876.992	3.4	1.6	1.6	125	261	265	65	78	83	83	4.5
3	70:38	16:31:35	879.288	3.1	1.5	1.5	124	259	267	64	79	83	83	4
4	73:44	16:50:53	881.444	3.1	1.5	1.5	126	261	265	65	82	83	83	4
5	76:58	17:06:09	883.541	2.6	1.3	1.3	126	259	264	62	82	83	83	3.5
6	80:15	17:23:26	885.747	3.0	1.4	1.4	127	261	265	61	82	83	83	3.5
1	83:32	17:39:40	888.279	2.8	1.4	1.4	125	260	265	60	80	83	83	3.5

$$\Delta V_m = \sqrt{\Delta p} = \frac{\Delta H}{T_s} = \frac{T_m}{T_s}$$

Δh Day 1 = 53.162

## FIELD DATA SHEET

Plant: AKMolletown Sample Type: M5-202 Operator: FZ  
 Sampling Location: Beachouse Stack 2 Pbar: 30.23 Ps: -0.85  
 Run Number: PB-202-1 Date: 8/30/16 CO<sub>2</sub>: LEM O<sub>2</sub>: LEM  
 Pretest Leak Rate: 0.01 cfm @ 10 in.Hg. at 100% Pitot#: 73-2  
 Pretest Leak Check: Pitot: 1.4 Orsat: ~ Stack Diameter: 35.5" K: 0.5221

[illegible]
$$\Delta V_m = 82.138 \sqrt{\Delta p} = 1.6794 \quad \Delta H = 1.36 \quad T_s = \frac{120 \text{ of.}}{123}$$

$\overline{T_m} = 79$  ✓



## SAMPLE RECOVERY DATA

Plant AK Middletown Run No. P-202-1  
 Date 8/30/14 Sample Box No. SB-17 Job No. 050074.0172  
 Sample Location Pushing Bighouse Filter No. 832610  
 Train Preparer EZ/60 Sample Head No. SH-1  
 Sample Recovery Person BF Barometer No. TWC.com  
 Comments MS-202 Balance No. FB-2

Front Half

Acetone Liquid  
 Container No. 202-1 Level Marked ☒ Sealed ☒

Filter

Container No. 832610 Sealed ☒

Description of Filter Light gray dots

Samples Stored and Locked ☒

Back Half/Moisture

Container No. ☒

Liquid Level Marked ☒ Sealed ☒

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	—	—	488.5	595.0	106.5
2	—	—	675.3	674.8	-0.5
3	H <sub>2</sub> O	100	615.2	621.2	6
4	Silica Gel	250g	935.7	964.3	28.6
5					
6					-100.0
Total					40.6

+100ml  
TypetH<sub>2</sub>O

Description of Impinger Catch: clear

23% BWS

Plant: AK Middlefield  
 Sampling Location: Baghouse Stack 2  
 Run Number: PB-202-2 Date: 8/31/16  
 Pretest Leak Rate: .001 cfm @ 9 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: -

Sample Type: MS-202 Operator: EZ  
 Pbar: 30.05 Ps: -0.86  
 CO<sub>2</sub>: CEM O<sub>2</sub>: CEM  
 Probe Length/Type: 36L Pitot#: T3-2  
 Stack Diameter: 35.5" K: 0.5221

Nozzle ID: 0.148 Thermocouple #: T3-2  
 Assumed Bws: 2.5 Filter #: 832594  
 Meter Box #: 5 Y: 0993 ΔH@: 1906  
 Post-Test Leak Rate: .001 cfm @ 7 in.Hg. } End of  
 Post-Test Leak Check: Pitot: ✓ Orsat: - } Day 1

Transpose Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	1020	917.744											
1	3:20	1020-24	919.843	2.8	1.4	1.4	102	258	264	62	82	75	75	5
2	6:42	1035-39	921.910	2.6	1.3	1.3	117	262	263	61	81	76	76	5
3	9:58	1049-52	923.872	2.5	1.2	1.2	127	262	265	62	81	77	76	5
4	13:19	1104-07	925.884	2.5	1.2	1.2	134	255	263	61	81	78	77	5
5	16:40	1123-26	927.905	2.6	1.2	1.2	138	255	266	61	82	80	79	5
6	20:00	1141-45	929.907	2.6	1.2	1.2	134	261	264	62	81	81	80	5
7	23:18	1200-04	932.204	3.5	1.7	1.7	133	262	267	60	80	82	81	6.5
2	26:41	1220-24	934.463	3.1	1.5	1.5	130	263	266	61	81	82	82	6
3	30:02	1238-42	936.770	3.1	1.5	1.5	130	265	264	62	82	84	83	6
4	33:23	1257-10	939.044	3.3	1.6	1.6	134	256	265	63	84	84	84	6
5	36:44	1316-20	941.302	3.3	1.6	1.6	135	264	265	63	82	85	85	6
6	40:04	1335-39	943.524	3.0	1.4	1.4	138	257	264	64	83	85	85	5.5
1	43:26	1345-49	945.791	3.2	1.5	1.5	129	259	267	64	85	86	86	6
2	46:49	1408-52	948.002	2.5	1.2	1.2	123	256	259	59	80	85	85	5
3	50:09	1434-02	950.201	2.7	1.3	1.3	124	263	258	59	76	85	85	5
4	53:22	1510-13	952.240	2.7	1.3	1.3	116	261	259	58	74	84	84	5
5	56:50	1525-29	954.465	2.6	1.3	1.3	119	260	273	59	75	84	84	5
6	60:10	1543-46	956.634	2.6	1.3	1.3	120	260	270	60	80	83	83	5
1	63:29	1600-03	958.739	2.5	1.2	1.2	122	262	266	61	82	83	82	5
2	66:52	1617-21	960.309	2.5	1.2	1.2	125	260	266	63	84	82	82	5
3	70:07	1634-37	962.990	3.1	1.5	1.5	124	260	264	61	78	82	82	5.5
4	73:49	1652-55	965.497	3.2	1.6	1.6	108	250	259	57	76	81	81	6
5	77:10	1708-12	967.703	3.0	1.5	1.5	106	270	262	58	74	80	80	6
6	80:31	1727-30	969.987	3.1	1.5	1.5	107	263	264	60	75	79	79	6
1	83:44	1737-40	972.076	2.8	1.4	1.4	107	267	267	61	74	79	79	5.5

LEAK ✓ 972.076 30.1 @ 10" ΔV<sub>m</sub> =             $\sqrt{\Delta p}$  =             $\frac{\Delta H}{\Delta H}$  =             $\frac{T_m}{T_s}$  =             
 972.200 ΔV<sub>m</sub> Day 1 = 54.322

# FIELD DATA SHEET

Plant: AK M. delletano Sample Type: 15-202 Operator: EZ  
 Sampling Location: Highrise Stack 2 Pbar: 30.08 Ps: -0.86  
 Run Number: PB-202-2 Date: 8/9/16 CO<sub>2</sub>: CEM O<sub>2</sub>: CEM  
 Pretest Leak Rate: 0.03 cfm @ 10 in.Hg. <sup>3000000</sup> Probe Length/Type: 3' 6" Pitot#: T3-2  
 Pretest Leak Check: Pitot: ✓ Orsat: - Stack Diameter: 35.5" K: 0.5221

[illegible]

$$\Delta V_m = 82.245 \sqrt{\Delta p} = 1.7058 \quad \Delta H = 1.41 \quad T_s = 121$$

$$\Delta q = 2.9184$$

$$T_m = 78$$





## SAMPLE RECOVERY DATA

Plant AK Middletown Run No. P-202-2  
 Date 7/1/16 Sample Box No. HSB-1 Job No. 052074.0172  
 Sample Location Pushing Baghouse Filter No. 832594  
 Train Preparer EZ/GD Sample Head No. SH-4  
 Sample Recovery Person BF Barometer No. two con  
 Comments M5-202 Balance No. FB-2

Front Half

Acetone Liquid  
 Container No. P-202-2 Level Marked / Sealed /

Filter

Container No. 832594 Sealed /

Description of Filter 1.5hr dry loading

Samples Stored and Locked /

Back Half/Moisture

Container No. not 2 Acetone/Hexane ; H<sub>2</sub>O

Liquid Level Marked NA Sealed NA

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	MT	-	506.9	610.2	103.3 - 100 = 3.3
2	MT	-	663.7	663.0	-0.3
3	H <sub>2</sub> O	100	781.4	788.8	4.4
4	Silica Gel	250	917.2	953.0	35.8
5					
6					
Total					43.2

100 ml  
Type 1 H<sub>2</sub>O

Description of Impinger Catch: clear  
 GWS - 2.4%

350 99.7%

Plant: AK Middleton Sample Type: M5-202 Operator: FEZ Nozzle ID: 0.148 Thermocouple #: T3-2  
 Sampling Location: Boghouse Stack 2 Pbar: 30.20 Ps: -1.1 Assumed Bws: 2.5 Filter #: 832587  
 Run Number: B3-202-3 Date: 9/6/16 CO<sub>2</sub>: CEN O<sub>2</sub>: CEN Meter Box #: 5 Y: 0.993 ΔH@: 1.906  
 Pretest Leak Rate: 0.01 cfm @ 10 in.Hg. Probe Length/Type: 3' GL Pitot#: T3-2 Post-Test Leak Rate: 0.01 cfm @ 10 in.Hg. End of  
 Pretest Leak Check: Pitot: ✓ Orsat: ✓ Post-Test Leak Check: Pitot: ✓ Orsat: ✓

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	1026	1.510		1.4	1.4	100	260	263	65	80	72	73	3.5
1	3:15	1026-29	3.620	2.9	1.3	1.3	115	264	259	64	81	73	73	3.5
2	6:31	1038-41	5.699	2.7	1.4	1.4	121	262	257	63	80	74	74	3.5
3	9:47	1051-54	7.783	2.9	1.4	1.4	124	258	264	62	84	76	75	3.5
4	13:51	120-24	10.449	3.4	1.6	1.6	128	260	265	61	83	77	76	4
5	17:04	1151-35	12.640	3.3	1.6	1.6	131	264	265	62	82	78	77	4
6	20:20	1146-48	14.822	3.5	1.7	1.7	130	262	265	63	81	78	78	4.5
1	23:38	1200-04	17.179	3.5	1.7	1.7	128	260	265	65	85	79	79	4.5
2	27:10	1219-23	19.628	3.3	1.8	1.8	133	258	262	61	84	81	80	4
3	30:30	1241-45	21.887	3.7	1.5	1.5	130	264	267	63	84	82	82	5
4	33:52	1258-13	24.345	3.2	1.4	1.4	132	257	264	63	83	83	82	4.5
5	37:10	1316-30	26.622	3.0	1.5	1.5	139	262	265	63	81	83	83	3.5
6	40:24	1337-41	28.749	3.1	1.5	1.5	145	260	264	65	82	84	83	4
1	43:45	1352-55	31.008	2.5	1.2	1.2	139	257	264	60	83	84	84	3
2	47:12	1414-44	33.185	2.5	1.2	1.2	148	260	266	61	81	84	84	3
3	50:22	1455-58	35.165	3.1	1.5	1.5	140	263	265	62	79	84	84	4
4	53:38	1509-12	37.378	2.8	1.3	1.3	141	259	266	60	72	84	84	3.5
5	57:00	1525-28	39.580	2.7	1.3	1.3	142	262	265	62	79	84	84	3.5
6	60:24	1542-46	41.844	2.7	1.3	1.3	139	263	265	63	80	84	84	3.5
1	63:40	1559-10	43.912	2.7	1.3	1.3	137	260	264	61	80	84	84	3.5
2	66:57	1616-19	46.152	3.0	1.4	1.4	138	260	266	62	79	84	84	4
3	70:15	1633-37	48.364	2.9	1.4	1.4	137	262	265	60	79	84	84	4
4	73:29	1652-55	50.521	3.0	1.4	1.4	132	263	265	62	78	85	84	4
5	76:44	1708-11	52.694	3.0	1.4	1.4	129	263	265	62	78	85	84	4
6	79:53	1724-28	54.767	3.0	1.4	1.4								
1	83:11	1735-39	56.964	3.0	1.4	1.4								

$$\Delta V_m = \sqrt{\Delta p} \quad \Delta H = \quad T_s =$$

$$T_m =$$

$$\Delta V_m \text{ Day 1} = 55.454$$



## SAMPLE RECOVERY DATA

Plant AK Middletown Run No. P-202-3  
 Date 8/30/16 <sup>DA</sup> 9/7/16 Sample Box No. 17 Job No. 0520740172  
 Sample Location Pushing Bay house Filter No. 832587  
 Train Preparer BF Sample Head No. 1  
 Sample Recovery Person DA Barometer No. TWC 60  
 Comments M5/202 Balance No. FB-2

Front Half

Acetone

Liquid

 Container No. P-202-3 Level Marked — Sealed —
Filter
 Container No. 832587 Sealed ✓

 Description of Filter Gray - Very Light

 Samples Stored and Locked ✓
Back Half/Moisture
 Container No. H<sub>2</sub>O; Acetone / Hexane

 Liquid Level Marked ✓ Sealed ✓

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	Empty	—	489.2	504.6	15.4
2	Empty	—	676.5	674.7	-1.8
3	DI H <sub>2</sub> O	100	722.8	729.3	6.5
4	Silica Gel	250	968.2	990.6	22.4
5	Purge H <sub>2</sub> O	100	100	100	-100.0
6					
Total					42.5

 Description of Impinger Catch: clear

Plant: Alk Steel - Mill Refinery Sample Type: 2014/20 2 Operator: dm  
 Sampling Location: Combustion Stack Pbar: 30.20 Ps: 30.82  
 Run Number: C-PM-0-1 Date: 9/6/16 CO<sub>2</sub>: 3.24 O<sub>2</sub>: 15  
 Pretest Leak Rate: 0.02 cfm @ 10 in.Hg. Probe Length/Type: 6.6 Pitot#: P5-2  
 Pretest Leak Check: Pitot: ✓ Orsat: — Stack Diameter: 16.8 K: —

Nozzle ID: 0.342 Thermocouple #: 75-2  
 Assumed Bws: 10 Filter #: 420923  
 Meter Box #: 3 Y: 1.009 AH@: 1.890  
 Post-Test Leak Rate: — cfm @ — in.Hg.  
 Post-Test Leak Check: Pitot: — Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	1002	822.400											
1	5.25	1007	824.30	0.05	0.452	0.45	350	249	250	68		78	77	1
2	10.50	1012	826.30	0.05	0.45	0.45	350	249	250	68		77	77	1
3	15.75	1017	828.15	0.05	0.45	0.45	325	247	250	61		76	77	1
4	20.50	1022	829.90	0.04	0.45	0.45	349	251	250	63		77	76	1
5	25.75	1027	831.80	0.05	0.45	0.45	337	250	250	62		77	76	1
6	31.0	1033	833.7	0.05	0.45	0.45	305	247	249	63		77	76	1
7	36.25	1036	835.7	0.05	0.45	0.45	319	252	250	60		78	77	1
8	41.00	1043	837.5	0.04	0.50	0.50	307	247	249	56		79	77	1
9	45.75	1048	839.35	0.04	0.50	0.50	323	251	250	57		80	77	2
10	50.50	1053	841.15	0.04	0.50	0.50	339	248	250	50		80	78	2
11	55.25	1058	843.05	0.04	0.50	0.50	341	250	251	50		80	79	2
12	60.00	1102	844.7	0.04	0.50	0.48	348	251	250	58		82	79	2
1	65.25	1107	846.7	0.05	0.50	0.48	361	251	250	59		82	79	2
2	70.00	1112	848.5	0.04	0.50	0.48	364	249	250	59		83	80	2
3	75.25	1117	850.35	0.05	0.50	0.48	357	249	250	60		84	80	2
4	80.50	1123	852.4	0.05	0.50	0.48	369	250	251	61		85	81	2
5	86.25	1128	854.3	0.04	0.50	0.48	371	249	250	61		86	81	2
6	90.50	1132	856.1	0.05	0.50	0.48	371	248	250	62		87	82	2
7	95.75	1137	858.1	0.05	0.50	0.45	365	250	249	62		88	83	2
8	101.00	1143	860.07	0.05	0.50	0.48	357	250	250	62		87	84	2
9	106.25	1148	862.1	0.05	0.50	0.48	342	251	250	62		88	84	2
10	111.50	1153	864.07	0.05	0.50	0.48	353	250	250	63		88	85	2
11	116.75	1158	866.05	0.05	0.50	0.48	331	252	252	60		89	85	2
12	122.00	12	868.034	0.05	0.50	0.50	332	250	254	61		89	85	2

$$\Delta V_m = \sqrt{\Delta p} \quad \Delta H = \quad T_s = \quad T_m =$$

Plant: AK Steel  
 Sampling Location: Conductivity Stack  
 Run Number: C-Puro-1 Date: 9/6/16  
 Pretest Leak Rate: 0.002 cfm @ 10 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: —

Sample Type: 201A/202 Operator: PLC  
 Pbar: 30.20 Ps: -0.80  
 CO<sub>2</sub>: 3.0 O<sub>2</sub>: 15.0  
 Probe Length/Type: 6' Pitot#: 85.2  
 Stack Diameter: 16.8" K: —

Nozzle ID: 0.342 Thermocouple #: 75.2  
 Assumed Bws: 10 Filter #: 470 923  
 Meter Box #: 3 Y: 6009 ΔH@: 1.980  
 Post-Test Leak Rate: 0.01 cfm @ 10 in.Hg.  
 Post-Test Leak Check: Pitot: ✓ Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)		Temperature EF		Impinging Temp. °F	Aux. Temp.	Dry Gas Meter Temp. Tm		Pump Vacuum (in. Hg)
					Desired	Actual			Probe	Filter			Inlet	Outlet	
0	0	1205	969.034												
1	5.25	1210	870.1	0.05	0.50	0.50	318	253	252	252	65	83	89	87	2
2	10.50	1215	872.0	0.05	0.50	0.50	315	252	251	251	60	83	90	87	2
3	15.75	1220	874.3	0.05	0.50	0.50	300	251	251	251	57	82	91	87	3
4	20.50	1225	876.0	0.04	0.54	0.53	300	250	251	251	57	82	91	88	3
5	25.25	1230	877.9	0.04	0.55	0.54	297	251	249	249	58	81	92	88	3
6	30.50	1235	880.0	0.05	0.55	0.54	305	250	251	251	60	81	92	88	3
7	35.75	1240	882.1	0.05	0.54	0.54	301	248	251	251	61	82	94	89	3
8	40.50	1245	883.9	0.04	0.54	0.54	304	248	249	249	60	81	94	90	3
9	45.25	1250	885.8	0.04	0.54	0.52	307	251	251	251	61	80	94	90	3
10	50.50	1255	887.3	0.05	0.54	0.50	316	254	249	249	61	80	94	90	3
11	56.25	1300	889.0	0.06	0.54	0.50	327	254	253	253	62	81	95	91	3
12	61.75	1306	892.15	0.055	0.54	0.50	318	247	248	248	62	82	95	91	3
1	67.00	1311	894.25	0.050	0.54	0.52	312	246	249	249	63	81	95	92	3
2	72.25	1316	896.3	0.050	0.53	0.50	304	252	250	250	63	81	95	92	4
3	77.50	1321	898.3	0.050	0.54	0.50	295	247	249	249	64	81	95	92	4
4	82.75	1326	900.3	0.050	0.54	0.50	285	247	251	251	65	82	95	92	4
5	88.00	1331	902.4	0.050	0.53	0.50	297	248	250	250	66	83	95	92	4
6	93.25	1336	904.5	0.050	0.55	0.52	301	252	252	252	60	82	96	92	4
7	98.25	1344	906.3	0.045	0.55	0.52	302	248	252	252	61	81	96	93	4
8	103.00	1350	908.3	0.040	0.50	0.52	305	251	250	250	61	80	96	93	5
9	108.25	1354	910.1	0.05	0.5	0.48	331	250	249	249	61	80	97	93	5
10	113.50	1359	912.0	0.05	0.5	0.48	319	250	249	249	62	80	97	93	6
11	118.75	1404	914.1	0.05	0.5	0.48	323	249	251	251	62	81	97	94	6
12	124.00	1409	916.101	0.05	0.5	0.48	325	251	250	250	63	81	97	94	6

$\Delta V_m = 93.701$   $\sqrt{\Delta p} = 0.2168$   $\Delta H = 0.490$   $T_s = 326$   
 $T_m = 86.8$   $150 = 104.9$   
 $246.0$   $0.2170$   $327.02$   
 $0.0475$   $87.02$   
 $0.2170$

## SAMPLE RECOVERY DATA

Plant AK Middletown Run No. C-PM<sub>10</sub>-1  
 Date 9/6/16 Sample Box No. \_\_\_\_\_ Job No. 0580740172  
 Sample Location Combustion stack Filter No. 470923  
 Train Preparer BF Sample Head No. SH-2  
 Sample Recovery Person CJ Barometer No. twc.com  
 Comments 202 Balance No. F0-2

Front Half 257 PM<sub>10</sub>  
 Acetone PM<sub>2.5</sub> Liquid \_\_\_\_\_  
 Container No. PM<sub>10</sub> Level Marked ☒ Sealed ☒

Filter  
 Container No. 470923 Sealed ☒

Description of Filter grey/green loading

Samples Stored and Locked ☒

Back Half/Moisture C-PM<sub>10</sub>-1  
 Container No. BACK 1/2 H<sub>2</sub>O / C-PM<sub>10</sub>-1  
ACE/HEX

Liquid Level Marked ☒ Sealed ☒

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	Empty	<del>10</del> -	507.2	1060.4	153.2
2	Empty	-	665.0	663.4	-1.6
3	DI H <sub>2</sub> O	100	788.8	790.0	1.2
4	Silica Gel	250	947.4	970.9	23.5
5					
6					
Total					176.3

Description of Impinger Catch: clear

Bus 8.37  
 ✓ E2

Plant: Alk Steel Sample Type: 2014/202 Operator: 12/1/15 Nozzle ID: 0342 Thermocouple #: 75-2  
 Sampling Location: Combustion Stack Pbar: 30.16 Ps: -0.75 Assumed Bws: 10 Filter #: 470 920  
 Run Number: C-202-2 Date: 9/7/16 CO<sub>2</sub>: 3 O<sub>2</sub>: 15 Meter Box #: 3 Y: 1.09 ΔH@: 1.89  
 Pretest Leak Rate: 0.002 cfm @ 10 in.Hg. Probe Length/Type: 5'6" Pitot#: 15-2 Post-Test Leak Rate: — cfm @ — in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: — Post-Test Leak Check: Pitot: — Orsat: —

202

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp. Tm		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	6835	950.750		0.34	0.35	257	251	252	68	84	70	70	1
1	4.75	0839	952.4	0.04	0.34	0.35	257	250	251	64	84	71	70	1
2	9.50	0844	954.9	0.04	0.34	0.36	356	249	251	61	84	71	70	1
3	14.00	0849	955.7	0.035	0.34	0.40	356	251	251	57	84	71	70	1
4	18.50	0854	957.3	0.035	0.34	0.45	362	252	250	55	84	73	71	1
5	23.25	0859	958.95	0.040	0.34	0.45	363	251	250	54	83	73	71	1
6	28.0	0904	960.7	0.040	0.34	0.45	365	260	250	55	83	74	71	1
7	32.75	0908	962.5	0.040	0.34	0.48	366	247	244	55	81	75	72	1
8	37.50	0913	964.3	0.040		0.48	345	249	246	54	79	76	72	1
9	42.00	0918	966.1	0.035		0.48	350	250	248	54	78	76	73	1
10	46.75	0922	967.9	0.040		0.48	335	253	251	54	77	77	74	1
11	51.50	0927	969.7	0.040		0.48	330	250	249	54	76	78	74	1
12	56.25	0932	971.5	0.040		0.48	317	249	250	54	76	79	25	1
1	60.50	0937	973.4	0.050		0.48	297	249	250	55	76	80	76	1
2	66.25	0942	975.2	0.040		0.48	297	250	250	55	77	81	77	1
3	71.00	0947	977.0	0.040		0.48	350	250	251	56	78	82	77	1
4	75.75	0952	978.8	0.040		0.48	352	249	251	57	78	82	78	1
5	80.25	0956	980.45	0.035		0.48	353	250	251	57	79	82	78	1
6	84.75	1000	982.1	0.035		0.48	358	251	252	57	79	82	78	1
7	89.50	1005	983.9	0.040		0.48	358	251	250	57	79	82	78	1
8	94.25	1010	985.8	0.040		0.48	353	241	251	58	79	82	79	1
9	99.00	1015	987.70	0.040		0.48	336	253	249	58	80	83	79	2
10	104.25	1020	989.6	0.050		0.48	241	252	245	58	80	83	79	2
11	109.0	1025	991.50	0.040		0.48	288	251	248	59	81	83	80	2
12	113.75	1030	993.248	0.040		0.48								

$$\Delta V_m =$$

$$\sqrt{\Delta p} =$$

$$\Delta H =$$

$$T_s =$$

$$T_m =$$



Plant: AK Steel Middletown Sample Type: 2014/202 Operator: RL/BL Nozzle ID: 0342 Thermocouple #: 75.2  
 Sampling Location: Combustion Stack Pbar: 30.16 Ps: -0.25" Assumed Bws: 10 Filter #: 470920  
 Run Number: C-202-2 Date: 9/7/16 CO<sub>2</sub>: 3 O<sub>2</sub>: 15 Meter Box #: 3 Y: 1.009 ΔH@: 1.000  
 Pretest Leak Rate: — cfm @ — in.Hg. Probe Length/Type: 5'6" Pitot#: P5.2 Post-Test Leak Rate: 0.003 cfm @ 2.0 in.Hg.  
 Pretest Leak Check: Pitot: — Orsat: — Stack Diameter: 160 K: — Post-Test Leak Check: Pitot: 1.2 Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp. Tm		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0		1030	993.248											
1	4.75	1034	995.1	0.040	.	0.48	307	250	251	60	81	84	80	2
2	9.50	1039	996.9	0.040		0.48	266	249	249	62	82	83	80	2
3	14.25	1044	998.6	0.040		0.48	261	250	248	63	83	84	81	2
4	19.50	1049	1000.5	0.050		0.46	304	250	249	58	83	84	81	2
5	24.25	1054	1002.4	0.040		0.46	307	248	251	56	81	85	81	2
6	29.00	1059	1004.2	0.040		0.46	298	240	248	56	81	85	82	2
7	33.75	1104	1006.0	0.040		0.45	292	250	250	57	80	85	82	2
8	38.50	1109	1007.7	0.040		0.45	315	254	251	58	80	86	83	2
9	43.25	1114	1009.45	0.040		0.45	294	247	250	58	79	87	83	2
10	48.00	1119	1011.3	0.040		0.45	293	254	250	59	79	87	83	2
11	53.25	1124	1013.2	0.040		0.45	288	250	249	59	80	87	83	2
12	58.00	1129	1014.7	0.050		0.45	258	240	251	59	80	87	84	2
1	62.00	1134	1016.4	0.040		0.45	288	253	250	59	80	88	84	2
2	67.00	1139	1018.100	0.035		0.45	289	252	251	61	81	87	84	2
*3	72.00	1144	1020.000	0.040		0.45	245	250	251	62	81	87	84	10
*4	76.75	1149	1021.810	0.040		0.45	217	253	250	60	81	87	85	11
5	81.50	1154	—	0.040		0.45	214	251	252	62	81	87	85	20
6		*	Vacuum went to 20" - could not pull ΔH. Stopped test run											
7	195.25													
8	Total Time													
9														
10														
11														
12														

$$\Delta V_{tm} = 71.06 \sqrt{\Delta p} = 0.2004 \text{ ft/s}$$

$$\Delta H = 0.4507 \text{ ft}$$

$$T_m = 80$$

0.457 ft 314 ft  
0.0402 ft

✓ E2

## SAMPLE RECOVERY DATA

Plant AK Steel Middletown Run No. C-202-2  
 Date 9/7/16 Sample Box No. HSB-1 Job No. 52074-0172  
 Sample Location Combustion Stack Filter No. 470920  
 Train Preparer CJ Sample Head No. 2  
 Sample Recovery Person DA Barometer No. PUL-con  
 Comments Methods 2014/202 Balance No. 2

Front Half - 3  $\rightarrow$  1 m.o. 7 m.o. 2 m.o. 2 m.o.  
 Acetone Liquid  
 Container No. C-2022 Level Marked        Sealed       

Filter  
 Container No. 470920 Sealed       

Description of Filter Black

Samples Stored and Locked        ✓

Back Half/Moisture  
 Container No. 2 H<sub>2</sub>O ; Acetone / Hexane

Liquid Level Marked        Sealed       

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	—	—	508.0	632.1	124.1
2	—	—	665.3	663.5	-1.8
3	H <sub>2</sub> O	100	790.0	793.6	3.6
4	SG	250	986.9	955.8	18.9
5					
6					
Total			2900.2	3045.0	144.8

Description of Impinger Catch: Clear

## FIELD DATA SHEET

Plant: AK Steel Middle town Sample Type: 2014/202 Operator: PK/BLF  
 Sampling Location: Combustion Stack Pbar: 30.16 Ps: 25  
 Run Number: C-202-3 Date: 9/1/16 CO<sub>2</sub>: 3 O<sub>2</sub>: 15  
 Pretest Leak Rate: 0.005 cfm @ 10 in.Hg. Pitot#: 15.2  
 Prefest Leak Check: Pitot: ± Orsat: — Stack Diameter: 16.8" K: —

Nozzle ID: 0.342 Thermocouple #: 75-2  
 Assumed Bws: 10 Filter #: 420922  
 Meter Box #: 3 Y: 1009 AH@: 1.89  
 Post-Test Leak Rate: — cfm @ — in.Hg.  
 Post-Test Leak Check: Pitot: — Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	1225	1027.9											
1	4.50	1230	1023.8	0.035	0.50	0.50	331	233	249	68	84	86	85	1
2	9.25	1235	1025.6	0.040	0.5	0.50	304	252	250	68	84	85	86	1
3	14.00	1239	1027.5	0.040	0.5	0.53	322	249	248	59	84	86	85	1
4	18.75	1244	1029.3	0.040	0.5	0.53	308	250	250	57	84	86	86	1
5	23.25	1249	1031.1	0.035	0.5	0.53	325	250	250	56	85	87	86	1
6	28.00	1254	1033.0	0.040	0.5	0.53	333	246	248	56	85	88	86	1
7	32.75	1258	1034.8	0.040	0.5	0.53	332	252	250	56	85	89	86	1
8	37.50	1303	1036.6	0.040	0.5	0.52	326	248	249	57	85	89	86	1
9	42.25	1308	1038.5	0.040	0.5	0.52	339	251	249	58	84	90	87	1
10	46.75	1313	1040.3	0.035	0.5	0.50	333	251	249	58	84	90	87	1
11	51.50	1317	1042.0	0.040	0.5	0.50	319	244	251	59	84	91	87	1
12	56.25	1322	1043.8	0.040	0.5	0.50	322	254	251	59	85	92	88	1
1	60.75	1326	1045.5	0.035	0.5	0.49	320	250	250	59	85	92	88	2
2	65.25	1330	1047.3	0.035	0.5	0.50	309	249	249	60	85	92	88	2
3	70.00	1335	1049.05	0.035	0.5	0.50	317	249	250	57	84	92	89	2
4	74.75	1339	1050.8	0.040	0.5	0.50	322	251	249	53	84	92	89	2
5	79.25	1343	1052.6	0.040	0.5	0.50	324	251	250	53	83	92	89	2
6	83.75	1348	1054.3	0.035	0.5	0.50	319	252	250	55	83	93	90	2
7	88.25	1353	1056.0	0.035	0.5	0.50	331	250	251	55	83	93	90	2
8	93.00	1358	1057.8	0.035	0.5	0.50	318	247	250	57	84	93	90	2
9	97.50	1403	1059.4	0.040	0.5	0.50	337	252	249	58	83	94	90	2
10	102.00	1407	1061.2	0.035	0.5	0.50	326	250	248	58	79	94	90	2
11	106.5	1412	1062.8	0.035	0.5	0.50	344	252	251	58	80	94	91	2
12	111.00	1416	1064.6	0.035	0.5	0.50	337	249	251	59	81	94	91	2

$$\Delta V_m = 42.639 \sqrt{\Delta p} = 0.1949 \quad \Delta H = 0.509 T_s = 32.6$$

$$0.038$$

$$T_m = 89$$

Plant: AK Steel White Sample Type: 2014/202 Operator: WLB/BS Nozzle ID: 0.342 Thermocouple #: TS-2  
 Sampling Location: Carbide for stack Pbar: 30.16 Ps: -0.75 Assumed Bws: 10 Filter #: 470922  
 Run Number: C-202-3 Date: 9/7/16 CO<sub>2</sub>: 3.0 O<sub>2</sub>: 15.0 Meter Box #: 2 Y: 1.009 AH@: 1.890  
 Pretest Leak Rate: — cfm @ — in.Hg. Probe Length/Type: 5'64" Pitot#: P5-2 Post-Test Leak Rate: 0.02 cfm @ 10 in.Hg.  
 Pretest Leak Check: Pitot: — Orsat: — Stack Diameter: 168" K: — Post-Test Leak Check: Pitot: 1.2 Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	1435	1064.619											
1	4.75	1420	1066.5	0.04	0.5	0.5	277	248	250	59	82	95	92	2
2	9.50	1425	1068.3	0.04	0.5	0.5	308	250	251	63	82	94	92	2
3	14.25	1430	1070.1	0.04	0.5	0.5	308	251	249	60	82	94	92	2
4	19.00	1436	1071.95	0.04	0.5	0.5	330	254	251	60	83	94	92	2
5	23.75	1441	1073.7	0.04	0.5	0.5	320	251	249	60	84	95	92	2
6	28.50	1446	1075.6	0.04	0.5	0.5	320	250	251	61	85	95	92	2
7	33.00	1451	1077.3	0.035	0.5	0.5	339	250	251	61	85	95	92	2
8	37.50	1456	1079.0	0.035	0.5	0.5	340	250	250	59	84	95	92	2
9	42.25	1500	1080.9	0.040	0.5	0.5	342	250	248	59	83	95	92	3
10	47.00	1505	1082.6	0.040	0.5	0.5	351	249	252	59	83	95	92	3
11	51.50	1510	1084.4	0.035	0.5	0.5	343	251	251	59	83	95	93	3
12	56.25	1515	1086.2	0.040	0.5	0.5	345	250	251	60	83	96	93	3
1	61.00	1520	1088.0	0.040	0.5	0.5	322	250	247	60	83	95	93	3
2	65.75	1525	1089.9	0.040	0.5	0.5	331	250	252	60	82	96	93	3
3	70.25	1530	1091.5	0.035	0.5	0.5	324	251	249	60	81	96	93	3
4	74.75	1534	1093.2	0.035	0.5	0.5	325	250	252	61	82	96	93	3
5	79.5	1539	1095.1	0.040	0.5	0.5	331	249	251	61	83	96	93	3
6	84.25	1543	1096.9	0.040	0.5	0.5	332	250	251	62	83	97	94	3
7	89.00	1548	1098.7	0.040	0.5	0.5	338	250	250	62	84	98	94	3
8	93.75	1554	1100.5	0.040	0.5	0.5	330	251	249	63	85	98	94	3
9	98.25	1558	1102.3	0.035	0.5	0.5	345	250	250	63	84	97	94	3
10	102.75	1602	1104.0	0.035	0.5	0.5	343	248	250	61	84	97	95	3
11	106.75	1606	1105.5	0.030	0.5	0.5	339	249	247	60	83	97	94	3
12	111.25	1610	1107.182	0.035	0.5	0.5	330	250	252	59	82	97	94	3

$$\Delta V_m = 42.563 \sqrt{\Delta p} = 0.1941 \Delta H = 0.000 T_s = 337$$

$$T_m = 92.72$$

0.0377 <sub>E2</sub>  
 0.504 <sub>E2</sub>  
 308 <sub>E2</sub>

✓ E2



## SAMPLE RECOVERY DATA

Plant AK Middletown Run No. C-202-3  
 Date 9/7/16 Sample Box No. H2B-3 Job No. SW74-0172  
 Sample Location Combustion Stack Filter No. 822609 470 922  
 Train Preparer EZ/CD Sample Head No. SH-11  
 Sample Recovery Person DA Barometer No. JWC  
 Comments AS-202 / 201A Balance No. 3

## Front Half

Acetone 3 <sup>> 8 PM 10 7 25</sup> <sub>< 8 PM 10 7 25</sub> Liquid

Container No. C-202-3 Level Marked — Sealed —

## Filter

Container No. 470922 Sealed ✓

Description of Filter Black

Samples Stored and Locked ✓

## Back Half/Moisture

Container No. H2O ; Acetone / Hexane

Liquid Level Marked ✓ Sealed ✓

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	—	—	519.5	718.4	198.9
2	—	—	658.8	658.4	-0.4
3	H2O	100	676.4	679.0	26
4	Silica Gel	250g	913.7	932.0	18.3
5					
6					
Total					219.4

Description of Impinger Catch: Clear

✓ EZ

## **HYDROGEN SULFIDE**

### METHOD 18 SAMPLING DATA

Company: AK STEEL

City: MIDDLETOWN

Date: 8/23/16

Location: COKE BATTERY BACKHOUSE Stack 1

Time: 1021-1509

Run No: P-15-1

Meter No: VB-1

Orifice, CC: 19 cc

Barometric Pressure, in.Hg: 29.95

Operator: BF

Ambient Temperature, EF: 85°F

### VACUUM LEAK CHECK DATA

	Initial, in.Hg	Final, in.Hg	Time, min
Pre-test	<u>25</u>	<u>25</u>	<u>1.00</u>
Post-test			

Sample time, min	START Clock time, (24-h)	STOP Clock time, (24-h)	Meter volume, liters	Rotameter Setting	Dry gas meter temp. EF	Vacuum, in.Hg
0.0	1021	1025	7626.88	19 cc	75	25
3.25	1032	1036	7626.95	19 cc	81	25
6.25	1045	1049	7627.02	19 cc	82	25
9.23	1113	1117	7627.13	19 cc	84	25
13.50	1126	1129	7627.29	19 cc	85	25
17.00	1142	1144	7627.38	19 cc	85	25
20.75	1200	1204	7627.48	19 cc	85	25
24.50	1219	1223	7627.53	19 cc	85	25
28.25	1239	1243	7627.57	19 cc	85	25
31.75	1256	1300	7627.59	19 cc	87	25
35.50	1316	1319	7627.61	19 cc	88	25
39.25	1334	1337	7627.62	19 cc	89	25
43.0	1352	1355	7627.63	19 cc	89	25

$$V_{std} = V_m \text{ liters} \times Y \times 17.647 \times \frac{P_b, \text{in. Hg}}{T_m, ^\circ R} \quad \text{Avg } 85^\circ \text{ F}$$

0.750 liters

### METHOD 18 SAMPLING DATA

Company: AK STEEL City: MIDDLETOWN  
 Date: 8/23/16 Location: COKE BATTERY BATHHOUSE  
 Time: 1021- 1509 Run No: P-15-1  
 Meter No: VB-1 Orifice, CC: 19 cc  
 Barometric Pressure, in.Hg: 29.95 Operator: BF  
 Ambient Temperature, EF: 85°F

### VACUUM LEAK CHECK DATA

*changed to 80cc orifice*

	Initial, in.Hg	Final, in.Hg	Time, min
Pre-test	<u>25</u>	<u>25</u>	<u>1.00</u>
Post-test	<u></u>	<u></u>	<u></u>

Sample time, min	START	STOP	Meter volume, liters	Rotameter Setting	Dry gas meter temp. EF	Vacuum, in.Hg
	Clock time, (24-h)					
46.25	1442	1446	7627.64	80cc Acc	89	25
50.50	1452	1456	7627.86	80cc	90	25
54.25	1505	1509	7628.07	80cc	93	25
			7628.37			

$$V_{std} = V_m \text{ liters} \times Y \times 17.647 \times \frac{P_b, \text{in. Hg}}{T_m, ^\circ R}$$

*1.45 liters*

*avg = 86.2°F*



## FIELD DATA SHEET

Plant: AK Middlelewh Sample Type: M15 Operator: NP/BF Nozzle ID: 13-6  
 Sampling Location: Baghouse 1 Pbar: 29.45 Ps: -1.1 Assumed Bws: 1.5 Filter #: —  
 Run Number: P-15-1 Date: 8-23-16 CO<sub>2</sub>: — Meter Box #: 11 Y: 1.016 ΔH@: 1.791  
 Pretest Leak Rate: — cfm @ — in.Hg. Probe Length/Type: 3' 6" Pitot#: 13-6 Post-Test Leak Rate: — cfm @ — in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: — Stack Diameter: 35.5" K: — Post-Test Leak Check: Pitot: ✓ Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (T <sub>s</sub> )	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
							<u>1022-1025</u>	<u>260</u>	<u>260</u>	<u>NA</u>	<u>NA</u>	<u>70</u>	<u>70</u>	<u>NA</u>
				<u>3.5</u>			<u>1033-1036</u>	<u>256</u>	<u>255</u>			<u>71</u>	<u>71</u>	
				<u>3.7</u>			<u>1045-1049</u>	<u>260</u>	<u>260</u>			<u>72</u>	<u>72</u>	
				<u>4.0</u>			<u>1113-1117</u>	<u>259</u>	<u>261</u>			<u>74</u>	<u>73</u>	
				<u>3.7</u>			<u>1126-1129</u>	<u>258</u>	<u>258</u>			<u>75</u>	<u>74</u>	
				<u>3.5</u>			<u>1142-1146</u>	<u>260</u>	<u>258</u>			<u>75</u>	<u>75</u>	
				<u>3.5</u>			<u>1200-1204</u>	<u>257</u>	<u>255</u>			<u>76</u>	<u>76</u>	
				<u>3.3</u>			<u>1214-1223</u>	<u>260</u>	<u>262</u>			<u>77</u>	<u>77</u>	
				<u>3.4</u>			<u>1239-1243</u>	<u>259</u>	<u>269</u>			<u>78</u>	<u>78</u>	
				<u>3.6</u>			<u>1256-1300</u>	<u>259</u>	<u>258</u>			<u>78</u>	<u>78</u>	
				<u>3.2</u>			<u>1316-1319</u>	<u>261</u>	<u>260</u>			<u>79</u>	<u>79</u>	
				<u>3.2</u>			<u>1334-1337</u>	<u>259</u>	<u>258</u>			<u>80</u>	<u>80</u>	
				<u>3.1</u>			<u>1352-1355</u>	<u>259</u>	<u>261</u>			<u>80</u>	<u>80</u>	
				<u>3.0</u>			<u>1412-1416</u>	<u>259</u>	<u>260</u>			<u>82</u>	<u>82</u>	
				<u>3.3</u>			<u>1452-1456</u>	<u>257</u>	<u>260</u>			<u>83</u>	<u>82</u>	
				<u>3.3</u>			<u>1505-1509</u>	<u>260</u>	<u>259</u>					
							<u>1522-1525</u>							
							<u>1540-1543</u>							
							<u>1557-1601</u>							
							<u>1614-1618</u>							
							<u>1653-1656</u>							
							<u>1707-1710</u>							
							<u>1722-1726</u>							

$$\Delta V_m = \frac{1.8494}{\sqrt{\Delta p}} = \frac{1.8494}{\sqrt{1.8459}} = 1.23$$

$$\Delta H = 1.23$$

$$T_m = N/A$$

$$\Delta p = 3.47$$

$$3.425$$

### METHOD 18 SAMPLING DATA

Company: AK STEEL City: MIDDLETOWN *small*  
 Date: 8/24/2016 Location: COKE BATTERY BACKHOUSE  
 Time: 1027-1509 Run No: P-15-2  
 Meter No: VB-1 Orifice, CC: 19cc  
 Barometric Pressure, in.Hg: 29.97 Operator: BIF  
 Ambient Temperature, EF: 85°F

### VACUUM LEAK CHECK DATA

	Initial, in.Hg	Final, in.Hg	Time, min
Pre-test	<u>25</u>	<u>25</u>	<u>1.00</u>
Post-test	<u>          </u>	<u>          </u>	<u>          </u>

Sample time, min	START Clock (24-h)	STOP time, (24-h)	Meter volume, liters	Rotameter Setting	Dry gas meter temp. EF	Vacuum, in.Hg
0	1027	1031	7628.54	19cc	76	25
3.75	1040	1044	7628.65	19cc	77	25
7.50	1054	1058	7628.75	19cc	77	25
11.00	1107	1111	7628.84	19cc	78	25
14.50	1124	1128	7628.95	19cc	77	25
18.25	1139	1142	7629.07	19cc	80	25
21.75	1158	1201	7629.21	19cc	81	25
25.50	1217	1221	7629.33	19cc	83	25
29.10	1234	1240	7629.37	19cc	85	25
32.75	1255	1259	7629.41	19cc	87	25
36.50	1314	1318	7629.43	19cc	89	25
40.25	1333	1336	7629.45	19cc	91	25
44.00	1350	1354	7629.47	19cc	92	25

$$V_{std} = V_m \text{ liters} \times Y \times 17.647 \times \frac{P_b, \text{in. Hg}}{T_m, ^\circ R}$$

**METHOD 18 SAMPLING DATA**

Company: AK STEEL City: MIDDLETOWN  
 Date: 8/28/16 Location: COLE BATTERY BATHHOUSE  
 Time: 1027-1509 Run No: P-15-2  
 Meter No: VB-1 Orifice, CC: 19  
 Barometric Pressure, in.Hg: 29.97 Operator: BF  
 Ambient Temperature, EF: 85°F

**VACUUM LEAK CHECK DATA**

Initial, in.Hg Final, in.Hg Time, min  
 Pre-test \_\_\_\_\_  
 Post-test \_\_\_\_\_

Sample time, min	START Clock (24-h)	STOP time, (24-h)	Meter volume, liters	Rotameter Setting	Dry gas meter temp. EF	Vacuum, in.Hg
48.0	1438	1442	7629.72	19cc	71	25
51.75	1453	1459	7629.94	19cc	92	25
55.25	1506	1509	7630.13	19cc	91	25
59.00			7630.35	19cc	92	25

$$V_{std} = V_m \text{ liters} \times Y \times 17.647 \times \frac{P_b, \text{in.Hg}}{T_m, ^\circ R} \quad \text{avg} = 84.8^\circ F$$

$V_m \approx 1,81 \text{ liters}$

Plant: AK / M, 1000 / 1000 Sample Type: M15 Operator: NP/BF  
 Sampling Location: P. Baghouse #1 Pbar: 29.97 Ps: -1.4  
 Run Number: P-15-2 Date: 8-24-16 CO<sub>2</sub>: \_\_\_\_\_ O<sub>2</sub>: \_\_\_\_\_  
 Pretest Leak Rate: \_\_\_\_\_ cfm @ \_\_\_\_\_ in. Hg. Probe Length/Type: 3' 6" Pitot#: 13-6  
 Pretest Leak Check: Pitot: ☒ Orsat: \_\_\_\_\_ Stack Diameter: 35.5" K: \_\_\_\_\_

Nozzle ID:            Thermocouple #: 77-6  
 Assumed Bws: 1.5 Filter #:             
 Meter Box #: 11 Y: 1.010 ΔH@: 1.79  
 Post-Test Leak Rate:            cfm @            in.Hg.  
 Post-Test Leak Check: Pitot:            Orsat:           

[illegible]
$$\Delta V_m = \frac{\sqrt{\Delta p} = 1.8655}{T_s = 17}$$
 $\overline{T_m} =$ 
$$\sqrt{\Delta p} = 1.8655$$

$\overline{10} = 3.48$

**METHOD 18 SAMPLING DATA**

Company: AK STEEL City: MIDDLETOWN *Stack 1*  
 Date: 8/25/2016 Location: COLE BATTERY BATHHOUSE  
 Time: 1028-1509 Run No: P-15-3  
 Meter No: VB-1 Orifice, CC: A  
 Barometric Pressure, in.Hg: 30.30 Operator: BF  
 Ambient Temperature, EF: 90°F

**VACUUM LEAK CHECK DATA**

	Initial, in.Hg	Final, in.Hg	Time, min
Pre-test	<u>25</u>	<u>25</u>	<u>1.00</u>
Post-test			

Sample time, min	START Clock time, (24-h)	STOP Clock time, (24-h)	Meter volume, liters	Rotameter Setting	Dry gas meter temp. EF	Vacuum, in.Hg
0.0	1028	1031	7633.20	19 cc	83	25
3.75	1042	1046	7633.32	19 cc	83	25
7.50	1054	1058	7633.39	19 cc	84	25
11.25	1123	1126	7633.42	19 cc	85	25
15.00	1134	1137	7633.44	19 cc	86	25
18.75	1145	1149	7633.52	19 cc	87	25
22.50	1159	1203	7633.59	19 cc	90	25
26.75	1218	1222	7633.67	19 cc	92	25
30.00	1238	1241	7633.72	19 cc	92	25
33.75	1257	1300	7633.98	19 cc	93	25
37.50	1316	1319	7634.16	19 cc	94	25
41.25	1335	1338	7634.50	19 cc	94	25
45.00	1350	1354	7634.71	19 cc	94	25

$$V_{std} = V_m \text{ liters} \times Y \times 17.647 \times \frac{P_b, \text{in. Hg}}{T_m, ^\circ R}$$

### METHOD 18 SAMPLING DATA

Company: AK STEEL City: MIDDLETOWN  
 Date: 8/25/2016 Location: COLE BATTERY BAGHOUSE  
 Time: 1028-1509 Run No: P-15-3  
 Meter No: VB-1 Orifice, CC: 19  
 Barometric Pressure, in.Hg: 30.30 Operator: BT  
 Ambient Temperature, EF: 90°F

### VACUUM LEAK CHECK DATA

	Initial, in.Hg	Final, in.Hg	Time, min
Pre-test	_____	_____	_____
Post-test	_____	_____	_____

Sample time, min	START Clock time, (24-h)	STOP Clock time, (24-h)	Meter volume, liters	Rotameter Setting	Dry gas meter temp. EF	Vacuum, in.Hg
48.75	1435	1439	7635.94	19cc	98	25
52.50	1445	1452	7635.19	19cc	100	25
56.25	1506	1509	7635.40	19cc	100	25
59.75			7635.50	19cc	100	25
			2.30 liters		avg = 91.7°F	

$$V_{std} = V_m \text{ liters} \times Y \times 17.647 \times \frac{P_b, \text{in. Hg}}{T_m, ^\circ R}$$

## FIELD DATA SHEET

AK Middleton

Plant: AK Middleton Sample Type: M-15 Operator: NP/BF  
Sampling Location: P. Baghouse 1 Pbar: 30.30 Ps: 80  
Run Number: 9-15-3 Date: 9-25-16 CO<sub>2</sub>:       
Pretest Leak Rate:      cfm @      in.Hg. Probe Length/Type: 3' 6L Pitot#: 73-6  
Pretest Leak Check: Pitot: ✓ Orsat:      Stack Diameter: 35.5" K:     

Nozzle ID: \_\_\_\_\_ Thermocouple #: 73-6  
 Assumed Bws: 15 Filter #: \_\_\_\_\_  
 Meter Box #: 4 Y: 1010  $\Delta H @$ : 1791  
 Post-Test Leak Rate: \_\_\_\_\_ cfm @ \_\_\_\_\_ in.Hg.  
 Post-Test Leak Check: Pitot: \_\_\_\_\_ Orsat: \_\_\_\_\_

[illegible]
$$\Delta V_m = \frac{\Delta V}{\sqrt{\Delta V^2 + \Delta V_{\text{rms}}^2}} = \frac{45.68 \cdot e}{\sqrt{45.68^2 + 12.4^2}} = 0.97$$

$T_m =$	45
---------	----

ST = 124

$$H^1 =$$
$$\underline{\underline{c \cdot \vec{v} = a \sqrt{v^2}}}$$
$$\Delta V_m =$$

12

1

**METHOD 18 SAMPLING DATA**

Company: AK STEEL City: MIDDLETOWN  
 Date: 8-29-2016 Location: COMBUSTION STACK  
 Time: 1024-1124 Run No: C-15-1  
 Meter No: VB-2 Orifice, CC: 15  
 Barometric Pressure, in.Hg: 30.11 Operator: BF  
 Ambient Temperature, EF: 90°F

**VACUUM LEAK CHECK DATA**

	Initial, in.Hg	Final, in.Hg	Time, min
Pre-test	<u>25</u>	<u>25</u>	<u>1.00</u>
Post-test			

Sample time, min	Clock time, (24-h)	Meter volume, liters	Rotameter Setting	Dry gas meter temp. EF	Vacuum, in.Hg
0	1024	4432.86	15 cc	87	25
5	1029	4432.94		91	
10	1034	4433.02		93	
15	1039	4433.10		94	
20	1044	4433.18		96	
25	1049	4433.26		97	
30	1054	4433.34		98	
35	1059	4433.42		99	
40	1104	4433.50		100	
45	1109	4433.58		101	
50	1114	4433.66		102	
55	1119	4433.74		103	
60	1124	4433.85		103	

$$V_{std} = V_m \text{ liters} \times Y \times 17.647 \times \frac{P_b, \text{in. Hg}}{T_m, ^\circ R} \quad \overline{T_m} = 97$$

0.996



Plant: AK 1 Sample Type: MOISTURE Operator: DS/BF  
 Sampling Location: Combustion Pbar: 30.11 Ps: -0.85  
 Run Number: M-1 Date: 8/29/2016 CO<sub>2</sub>: 3 O<sub>2</sub>: 15  
 Pretest Leak Rate: 0.002 cfm @ 10 in.Hg. Probe Length/Type: 7.6 Pitot#: —  
 Prefest Leak Check: Pitot: ✓ Orsat: — Stack Diameter: 16.8" K: —

Nozzle ID: — Thermocouple #: —  
 Assumed Bws: — Filter #: —  
 Meter Box #: 2 Y: 1.005 ΔH@: 1.687  
 Post-Test Leak Rate: 0.002 cfm @ 5 in.Hg.  
 Post-Test Leak Check: Pitot: ✓ Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
	0	1024	676.690											
1	5	1029	679.5	0.04	1.5	1.5	357	—	—	51	—	75	72	0
2	10	1034	683.7	0.04	1.5	1.5	350	—	—	54	—	77	72	0
3	15	1039	687.1	0.05	1.5	1.5	352	—	—	55	—	78	73	0
4	20	1044	690.4	0.05	1.5	1.5	350	—	—	57	—	80	73	0
5	25	1049	693.9	0.06	1.5	1.5	350	—	—	58	—	83	74	0
6	30	1054	697.3	0.06	1.5	1.5	350	—	—	56	—	85	75	0
1	35	1059	700.7	0.05	1.5	1.5	232	—	—	55	—	86	77	0
2	40	1104	704.2	0.05	1.5	1.5	240	—	—	57	—	88	78	0
3	45	1109	707.7	0.05	1.5	1.5	253	—	—	59	—	88	78	0
4				0.05			250							
5				0.06			250							
6				0.03			251							
1				0.04			250							
2				0.04			240							
3				0.05			225							
4				0.06			225							
5				0.05			230							
6				0.05			225							
1				0.02			260							
2				0.02			257							
3				0.04			258							
4				0.04			257							
5				0.05			250							
6				0.05			244							
							243							

ΔV<sub>m</sub> = 31.01  $\sqrt{\Delta p} = 0.2123$  ΔH = 1.5 T<sub>s</sub> = 270

T<sub>m</sub> = 70

ΔP = 0.046

✓BF

## SAMPLE RECOVERY DATA

Plant AK MIDDLETON Run No. C-15-1  
 Date 8/29/16 Sample Box No. \_\_\_\_\_ Job No. 050074.0172  
 Sample Location COMBUSTION STACK Filter No. \_\_\_\_\_  
 Train Preparer CT Sample Head No. 6  
 Sample Recovery Person CT Barometer No. TWC.COM  
 Comments M4 Balance No. 2

Front Half

Acetone

Liquid

Container No. N/A Level Marked \_\_\_\_\_ Sealed \_\_\_\_\_

Filter

Container No. \_\_\_\_\_ Sealed \_\_\_\_\_

Description of Filter \_\_\_\_\_

Samples Stored and Locked \_\_\_\_\_

Back Half/MoistureContainer No. N/A

Liquid Level Marked \_\_\_\_\_ Sealed \_\_\_\_\_

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	H <sub>2</sub> O	100	802.2	854.6	52.4
2	H <sub>2</sub> O	100	784.7	787.9	3.2
3	—	—	669.5	670.0	0.5
4	SG	250	942.1	958.1	16.0
5					
6					
Total					72.1

Description of Impinger Catch: greyB<sub>WS</sub> = 9.9%

✓BIF

**METHOD 18 SAMPLING DATA**

Company: AK STEEL City: MIDDLETOWN  
 Date: 8/29/2016 Location: COMBUSTION STACK  
 Time: 1135-1235 Run No: C-15-2  
 Meter No: VB-2 Orifice, CC: 15cc  
 Barometric Pressure, in.Hg: 30.11 Operator: BF  
 Ambient Temperature, EF: 90°F

**VACUUM LEAK CHECK DATA**

	Initial, in.Hg	Final, in.Hg	Time, min
Pre-test	<u>25</u>	<u>25</u>	<u>1.00</u>
Post-test	<u>                    </u>	<u>                    </u>	<u>                    </u>

Sample time, min	Clock time, (24-h)	Meter volume, liters	Rotameter Setting	Dry gas meter temp. EF	Vacuum, in.Hg
0	1135	4433.87	15cc	104	25
5	1140	4433.96		105	
10	1145	4434.08		105	
15	1150	4434.17		106	
20	1155	4434.28		106	
25	1200	4434.40		107	
30	1205	4434.49		107	
35	1210	4434.58		107	
40	1215	4434.69		107	
45	1220	4434.82		107	
50	1225	4434.93		107	
55	1230	4435.10		107	
60	1235	4435.21		107	

$$V_{std} = V_m \text{ liters} \times Y \times 17.647 \times \frac{P_b, \text{in. Hg}}{T_m, ^\circ R} \quad \bar{T}_m = 106$$

1.342

Plant: AK Sample Type: MOISTURE Operator: VS/BF Nozzle ID: ✓ Thermocouple #:           
 Sampling Location: COMBUSTION Pbar: 30.11 Ps: 0.82 Assumed Bws:          Filter #:           
 Run Number: M-2 Date: 8/29/2014 CO<sub>2</sub>:          Meter Box #: 2 Y: 6005 ΔH@: 1.687  
 Pretest Leak Rate: 0.000 cfm @ 5 in.Hg. Post-Test Leak Rate: 0.001 cfm @ 5 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat:          Post-Test Leak Check: Pitot: ✓ Orsat:         

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
1	5	1135	707.88	0.04	1.5	1.5	269	-	-	63	78	83	81	1
2	10	1140	711.3	0.04	1.5	1.5	287	-	-	64	-	87	82	1
3	15	1145	714.7	0.04	1.5	1.5	291	-	-	60	-	88	82	2
4	20	1150	718.2	0.04	1.5	1.5	285	-	-	60	-	88	82	2
5	25	1155	721.6	0.04	1.5	1.5	280	-	-	57	-	89	82	2
6	30	1200	725.0	0.05	1.5	1.5	271	-	-	55	-	90	83	3
1	35	1205	728.4	0.05	1.5	1.5	251	-	-	55	-	92	83	3
2	40	1210	731.8	0.03	1.5	1.5	250	-	-	54	-	93	84	3
3	45	1215	735.1	0.03	1.5	1.5	249	-	-	54	-	94	85	3
4		1220	738.66	0.04	1.5	1.5	248							
5				0.05			247							
6				0.06			246							
1				0.03			245							
2				0.04			240							
3				0.04			238							
4				0.04			237							
5				0.05			230							
6				0.03			313							
1				0.03			310							
2				0.03			309							
3				0.03			308							
4				0.04			307							
5				0.04			306							
6				0.04			305							

ΔV<sub>m</sub> = 30.78  $\sqrt{\Delta p}$  = 0.267  $\Delta H$  = 1.5  $T_s$  = 272

0.1498  $\Delta H$  = 0.045 0.0404

$T_m$  = 86

$\sqrt{0.5}$



## SAMPLE RECOVERY DATA

Plant AK Middleton Run No. C-15-2  
 Date 8/29/16 Sample Box No. 8 Job No. 050074.0172  
 Sample Location COMBUSTION STACK Filter No.         
 Train Preparer MP Sample Head No. 7  
 Sample Recovery Person CT Barometer No. TWC.COM  
 Comments        Balance No. 2

Front Half

Acetone        Liquid  
 Container No. N/A Level Marked        Sealed       

## Filter

Container No.        Sealed       

Description of Filter       

Samples Stored and Locked       

Back Half/Moisture

Container No. N/A

Liquid Level Marked        Sealed       

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	H <sub>2</sub> O	100	758.8	814.8	56.0
2	H <sub>2</sub> O	100	766.3	772.2	5.9
3	-	-	661.8	664.0	2.2
4	SG	250	931.5	946.2	6.7
5					
6					
Total					70.8

Description of Impinger Catch: grey

9.9%

**METHOD 18 SAMPLING DATA**

Company: AK STEEL City: MIDDLETOWN  
 Date: 8/29/2016 Location: COMBUSTION STACK  
 Time: 1245-1345 Run No: C-15-3  
 Meter No: V13-2 Orifice, CC: 15  
 Barometric Pressure, in.Hg: 30.11 Operator: BF  
 Ambient Temperature, EF: 90°F

**VACUUM LEAK CHECK DATA**

	Initial, in.Hg	Final, in.Hg	Time, min
Pre-test	<u>25</u>	<u>25</u>	<u>1.00</u>
Post-test			

Sample time, min	Clock time, (24-h)	Meter volume, liters	Rotameter Setting	Dry gas meter temp. EF	Vacuum, in.Hg
0	1245	4435.26	15	106	25
5	1250	4435.35		106	
10	1255	4435.43		105	
15	1300	4435.52		105	
20	1305	4435.61		106	
25	1310	4435.72		105	
30	1315	4435.80		105	
35	1320	4435.90		105	
40	1325	4436.02		104	
45	1330	4436.14		105	
50	1335	4436.22		105	
55	1340	4436.30		105	
60	1345	4436.41		105	

$$V_{std} = V_m \text{ liters} \times Y \times 17.647 \times \frac{P_b, \text{in. Hg}}{T_m, ^\circ R} \quad \bar{T}_m = 105$$

$V_m = 1.15 \text{ L}$

## FIELD DATA SHEET

Plant: AK Sample Type: MOLISTOPAL Operator: DS/BF Nozzle ID: - Thermocouple #: -  
 Sampling Location: COMBUSTION Pbar: 30.11 Ps: 0.85 Assumed Bws: - Filter #: -  
 C-15-3 Run Number: M-3 Date: 8/29/2016 CO<sub>2</sub>: - Meter Box #: 2 Y: 1,005 AH@: 1,687  
 Pretest Leak Rate: 0.000 cfm @ 0 in.Hg. Probe Length/Type: 7'6" 455 Pitot#: - Post-Test Leak Rate: - cfm @ - in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: - Stack Diameter: 16.8" K: - Post-Test Leak Check: Pitot: ✓ Orsat: -

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
1	0	1245	738.85	0.02	1.5	1.5	311	-	-	57	-	89	87	1
2	5	1250	742.3	0.03	1.5	1.5	312	-	-	58	-	90	87	1
3	10	1255	745.17	0.03	1.5	1.5	310	-	-	59	-	92	88	1
4	15	1300	749.1	0.04	1.5	1.5	308	-	-	60	-	94	88	1
5	20	1305	752.5	0.05	1.5	1.5	307	-	-	60	-	96	88	1
6	25	1310	756.0	0.06	1.5	1.5	306	-	-	61	-	98	90	1
1	30	1315	759.5	0.03	1.5	1.5	279	-	-	61	-	99	90	1
2	35	1320	762.9	0.03	1.5	1.5	277	-	-	62	-	100	91	1
3	40	1325	766.4	0.04	1.5	1.5	275	-	-	62	-	100	91	1
4	45	1330	769.91	0.04			273							
5				0.04			272							
6				0.05			271							
1				0.04			260							
2				0.03			259							
3				0.03			269							
4				0.04			268							
5				0.04			263							
6				0.05			260							
1				0.05			263							
2				0.04			262							
3				0.04			240							
4				0.05			258							
5				0.85			253							
6				0.06			251							

$$\Delta V_m = 31.06 \sqrt{\Delta p} = 0.206 \quad \Delta H = 1.5 \quad T_s = 276$$

$$T_m = 92$$

0.04

✓BF

## SAMPLE RECOVERY DATA

Plant AK MIDDLETOWN Run No. C-15-3  
 Date 8/29/16 Sample Box No. \_\_\_\_\_ Job No. 050074.0172  
 Sample Location COMBUSTION STACK Filter No. \_\_\_\_\_  
 Train Preparer CS Sample Head No. 4  
 Sample Recovery Person CS Barometer No. TWC.COM  
 Comments M4 Balance No. 2

Front Half

Acetone \_\_\_\_\_ Liquid \_\_\_\_\_  
 Container No. N/A Level Marked \_\_\_\_\_ Sealed \_\_\_\_\_

Filter

Container No. \_\_\_\_\_ Sealed \_\_\_\_\_

Description of Filter \_\_\_\_\_

Samples Stored and Locked \_\_\_\_\_

Back Half/Moisture

Container No. N/A

Liquid Level Marked \_\_\_\_\_ Sealed \_\_\_\_\_

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	H <sub>2</sub> O	100	813.9	880.7	66.8
2	H <sub>2</sub> O	100	782.5	789.1	6.6
3	—	—	669.9	671.3	1.4
4	SG	250	947.6	954.7	7.1
5					
6					
Total					81.9

Description of Impinger Catch: grey

BWS = 11.3%

✓BF



## **SULFUR DIOXIDE AND CARBON MONOXIDE**



Environmental Quality Management, Inc.

# CEM CALIBRATION DATA SHEET

Company: AK Steel  
 Location: Poughkeepsie, NY  
 Project No.: SD074.0172

Operator: Doug Allen  
 Date: 8/23/16

Averages  
 O<sub>2</sub> 20.656  
 CO<sub>2</sub> 0.428  
 CO 30.665  
 SO<sub>2</sub> 5.67

Pollutant/ Range/ Inst. ID	Cal Gas Conc.	Calibration Response		Post Test Run 1 Response				Post Test Run 2 Response				Post Test Run 3 Response				Cylinder No.
		Direct Time: 0855	System	ppm/% Time: 1205-1012	%Drift	%Bias	ppm/% Time: 1508-1515	%Drift	%Bias	ppm/% Time:	%Drift	%Bias	ppm/% Time:			
O <sub>2</sub>	Zero	0	0.182	0.176	0.23											
	Low	-	-	-												
	Mid	11.02	11.138	11.065											CC443432	
	High	21.89	22.069	21.837	21.85										CC443447	
CO	Zero	0	0.162	0.246	0.18											
	Low	-	-	-												
	Mid	11.23	11.308	11.077	11.10										CC443447	
	High	21.94	22.169	21.994											CC443450	
CO	Zero	0	-1.08	0.33	-0.8											
	Low	-	-	-												
	Mid	190.9	189.61	185.50	184.8										CC73678	
	High	454.8	456.54	447.56											CC73679	
SO <sub>2</sub>	Zero	0	0.14	0.55	0.56											
	Low	-	-	-												
	Mid	44.88	44.38	44.93	43.9										CC66198	
	High	89.09	88.12	89.28											SG934952B	
Vent Times Averages	Perish	start	stop	Perish	start	Perish	start	Perish	start	Perish	start	Perish	start	stop		
	1	1022	1025	5	1126	1129	9	1239	1243	13	1352	1355				
	2	1033	1037	6	1143	1146	10	1256	1300	14	1442	1446				
	3	1046	1049	7	1200	1204	11	1316	1320	15	1452	1456				
	4	1113	1117	8	1219	1223	12	1334	1337	16	1505	1509				



Environmental Quality Management, Inc.

# CEM CALIBRATION DATA SHEET

Averages  
O<sub>2</sub> 20.628  
CO<sub>2</sub> 0.420  
CO 21.87  
SO<sub>2</sub> 4.45

Company:  
Location:  
Project No.:

AK Steel  
Ashby Bayshore  
050074-0172

Operator:  
Date:

Doug Allen  
8/24/16

Pollutant/ Range/ Inst. ID	Cal Gas	Cal Gas Conc.	Calibration Response		Post Test Run 1			Post Test Run 2			Post Test Run 3			Cylinder No.	
			Direct Time:	System	ppm/% Time:	Response		ppm/% Time:	Response		ppm/% Time:	Response			
						%Drift	%Bias		%Drift	%Bias		%Drift	%Bias		
O <sub>2</sub>	Zero	0	0.234	0.180			0.26			0.204					
	Low	-													
	Mid	11.02	11.113	10.986											
	High	21.89	21.984	21.783			21.78			21.729					
CO <sub>2</sub>	Zero	0	0.233	0.193			0.15			0.209					
	Low	-													
	Mid	11.23	11.101	11.077			11.0			10.968					
	High	21.94	22.051	21.829											
CO	Zero	0	-0.04	1.01			0.55			-1.20					
	Low	-													
	Mid	190.9	189.74	186.87			186.1			183.75					
	High	454.0	455.81	448.62											
SO <sub>2</sub>	Zero	0	-0.44	0.81			0.9			1.26					
	Low	-													
	Mid	44.88	43.25	44.97			44.4			44.04					
	High	89.09	89.26	87.50											
Averages	Preish	Start	Stop				Preish	Start	Stop				Preish	Start	Stop
	1	102.1	103.1				5	112.4	112.6				9	123.6	124.0
	2	104.0	104.4				6	113.9	114.2				10	125.5	125.9
	3	105.4	105.6				7	115.4	120.1				11	131.4	131.8
Averages	4	116.7	117.1				8	121.7	122.1				12	133.3	133.7





Environmental Quality Management, Inc.

# CEM CALIBRATION DATA SHEET

Company:  
Location:  
Project No.:

Ak steel  
Pushing Bughouse  
050074.0172

Operator:  
Date:

Doug Allen  
8/23/16

Pollutant/ Range/ Inst. ID	Cal Gas	Cal Gas Conc.	Calibration Response		Post Test Run 1 Response			Post Test Run 2 Response			Post Test Run 3 Response			Cylinder No.
			Direct	System	ppm/%	%Drift	%Bias	ppm/%	%Drift	%Bias	ppm/%	%Drift	%Bias	
O <sub>2</sub>	Zero	0	0.193	0.233	0.23			0.195						
	Low	-	-	-	-									
	Mid	11.02	11.021	10.992										
	High	21.89	21.899	21.731	21.62			21.629						
CO <sub>2</sub>	Zero	0	0.245	0.241	0.25			0.180						
	Low	-	-	-	-									
	Mid	11.23	11.046	11.030	10.9			10.873						
	High	21.94	21.894	21.766										
CO	Zero	0	-0.25	-0.78	-2.1			-3.87						
	Low	-	-	-	-									
	Mid	190.9	186.80	184.33	184.1			179.14						
	High	454.0	454.97	447.69										
SO <sub>2</sub>	Zero	0	-0.28	0.06	0.3			0.99						
	Low	-	-	-	-									
	Mid	44.88	45.06	45.14	44.6			43.86						
	High	89.09	90.17	88.35										
Averages	1	1028	1031		5	1134	1137	9	1238	1241	13	1350	1354	
	2	1042	1046		6	1145	1149	10	1257	1300	14	1435	1439	
	3	1054	1058		7	1159	1203	11	1318	1319	15	1449	1452	
	4	1123	1126		8	1218	1222	12	1355	1338	16	1506	1509	

Averages  
O<sub>2</sub> 20.491  
CO<sub>2</sub> 0.463  
SO<sub>2</sub> 22.05  
CO 6.51



Environmental Quality Management, Inc.

# CEM CALIBRATION DATA SHEET

Company:  
Location:  
Project No.:

Ak steel Middletown  
Combustion Stack  
5074-0172

Operator:  
Date:

Allen  
8/29/16

Pollutant/ Range/ Inst. ID	Cal Gas	Cal Gas Conc.	Calibration Response		Post Test Run 1			Post Test Run 2			Post Test Run 3			Cylinder No.
			Direct	System	ppm/%	%Drift	%Bias	ppm/%	%Drift	%Bias	ppm/%	%Drift	%Bias	
O2	Zero	0	0.143	0.294	0.285									
	Low	-	-	-										
	Mid	11.02	11.125	11.113										
	High	21.89	22.036	21.827	21.669			21.600			21.744			
CO2	Zero	0	0.188	0.182	0.167									
	Low	-	-	-										
	Mid	11.73	11.070	11.052	10.813			10.773			10.940			
	High	21.94	22.034	21.756										
CO	Zero	0	0.92	0.19	0.17									
	Low	-	-	-										
	Mid	190.9	188.96	186.74	186.73			186.31			186.18			
	High	454.8	457.44	449.10										
SO2	Zero	0	0.56	0.66	0.79									
	Low	-	-	-										
	Mid	189.4	191.84	191.55	188.26			191.56			195.52			
	High	453.7	456.88	449.96										
Averages														
				O2	15.175			15.643			15.158			
				CO2	2.994			2.738			2.961			
				CO	55.07			63.79			85.19			
				SO2	254.01			230.40			230.30			

## **SPECIATED VOLATILE ORGANIC HAP (VOHAP)**

EQM

## FIELD DATA SHEET

Nozzle ID: 0152 Thermocouple #: 73-6  
 Assumed Bws: 1.5 Filter #: —  
 Meter Box #: 11 Y: 1.010 AH@: 1.791  
 Post-Test Leak Rate: .001 cfm @ 10 in.Hg.  
 Post-Test Leak Check: Pitot: ✓ Orsat: —

Sample Type: M36 Operator: NP  
 Pbar: 30.23 Ps: -1.1  
 CO<sub>2</sub>: 0.3 O<sub>2</sub>: 20.5  
 Probe Length/Type: 3' 6" Pitot#: 13-6  
 Stack Diameter: 35.5" K: .5562

Plant: AK Middletown  
 Sampling Location: Boehowse 1  
 Run Number: 8-316-1 Date: 8-30-16  
 Pretest Leak Rate: .001 cfm @ 8 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	AH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	1026	497.493											
1	3:28	1026-1029	500.051	3.4	1.8	1.8	100	264	264	65	NA	70	70	3
2	6:59	1043-1046	502.773	3.5	1.8	1.8	105	251	265	65		73	73	3
3	10:28	11:19-1122	505.060	3.6	1.9	1.9	106	266	266	64		74	74	3
4	13:55	1139-1142	507.615	3.5	1.8	1.8	110	260	267	64		76	76	3
5	17:25	1201-1204	510.252	3.7	1.9	1.9	112	261	269	63		78	77	3
6	20:53	1211-1214	512.850	3.8	2.0	2.0	115	252	262	63		79	79	3
1	24:26	1221-1224	515.399	3.8	2.0	2.0	116	263	267	63		80	79	3
2	27:37	1231-1234	518.073	3.9	2.0	2.0	118	255	265	62		81	80	3
3	31:09	1245-1248	520.851	3.6	2.0	2.0	120	264	265	62		81	81	3
4	34:43	1259-1302	523.616	3.6	1.9	1.9	121	262	265	62		83	81	3
5	38:19	1316-1319	526.515	3.7	1.9	1.9	122	266	265	63		83	83	3
6	41:53	1335-1338	529.357	3.7	1.9	1.9	125	265	260	62		84	84	3
1	43:31	1345-1348	530.615	3.7	1.9	1.9	126	265	264	62		85	85	3
2	47:00	1356-1359	533.322	3.7	1.9	1.9	127	261	262	62		86	85	3
3	50:22	1413-1416	535.976	3.6	1.9	1.9	127	263	267	63		87	86	3
4	53:58	1428-1431	538.865	3.5	1.8	1.8	125	265	266	63		87	87	3
5														
6														
1														
2														
3														
4														
5														
6														

$$\Delta V_m = 41.372 \quad \sqrt{\Delta p} = 1.9118 \quad \Delta H = 1.9 \quad T_s = 117$$

$$\text{Ave OR} = 3.6563$$

$$\overline{T_m} = 80 \quad \sqrt{OF}$$



## SAMPLE RECOVERY DATA

Plant AK MIDDLETOWN Run No. P-316-1  
Date 8/30/16 Sample Box No. \_\_\_\_\_ Job No. 050074.0172  
Sample Location Pushing Bighouse Filter No. NA  
Train Preparer CT Sample Head No. 5  
Sample Recovery Person BF Barometer No. TWC. com  
Comments 316 Balance No. FB-2

Front HalfAcetone P-316-1 LiquidContainer No. 301 Level Marked ✓ Sealed ✓

## Filter

Container No. NA Sealed NADescription of Filter NASamples Stored and Locked ✓Back Half/MoistureContainer No. NALiquid Level Marked NA Sealed NA

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	TYPE 1 H <sub>2</sub> O	100	789.1	794.8	5.7 ✓
2	TYPE 1 H <sub>2</sub> O	100	761.9	763.7	1.8 ✓
3	—	—	652.1	653.6	1.5 ✓
4	SC <sub>1</sub>	250	918.9	927.6	8.7 ✓
5					
6					
Total					17.7 ✓

Description of Impinger Catch: clear



## FIELD DATA SHEET

Plant: AK Middleboro Sample Type: M316 Operator: NP Nozzle ID: 152 Thermocouple #: 1326  
 Sampling Location: 0 Bughouse 1 Pbar: 30.05 Ps: -1.1 Assumed Bws: 1.5 Filter #: —  
 Run Number: P-316-2 Date: 8-31-16 CO<sub>2</sub>: CEM O<sub>2</sub>: CEM Meter Box #: 11 Y: 6.010 ΔH@: 1.791  
 Pretest Leak Rate: 0.001 cfm @ 10 in.Hg. Probe Length/Type: 3'64 Pitot#: 1326 Post-Test Leak Rate: 0.001 cfm @ 3 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: — Stack Diameter: 36.5" K: 5562 Post-Test Leak Check: Pitot: ✓ Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp. Tm		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	10:20	539.343				96	264	260	65	NA	70	70	3
1	3:26	10:20-10:21	541.984	3.9	2.1	2.1	100	261	265	65		73	73	3
2	6:59	10:25-10:26	544.760	3.9	2.1	2.1	102	258	261	64		74	73	3
3	10:32	10:44-10:52	547.393	3.8	2.0	2.0	105	264	262	64		75	75	3
4	13:56	11:01-11:07	550.133	3.7	1.9	1.9	108	264	262	63		76	75	3
5	17:26	11:11-11:15	552.875	3.6	1.9	1.9	110	261	260	63		77	76	3
6	21:04	11:16-11:20	555.619	3.8	2.0	2.0	115	263	264	63		78	77	3
1	24:36	12:00-12:04	558.305	3.8	2.0	2.0	120	263	263	62		80	78	3
2	28:10	12:04-12:08	561.087	3.9	2.0	2.0	123	260	263	62		81	80	3
3	31:44	12:09-12:10	563.897	3.7	1.9	1.9	125	262	263	62		82	81	3
4	35:16	12:16-12:17	566.660	3.7	1.9	1.9	120	262	263	61		83	83	3
5	38:47	13:16-13:20	569.443	3.7	1.9	1.9	122	264	264	61		84	84	3
6	42:20	13:25-13:30	572.246	3.7	1.9	1.9	121	264	263	62		85	85	3
1	45:52	13:35-13:40	576.037	3.7	1.9	1.9	123	263	263	60		86	85	3
2	49:26	14:05-14:52	577.849	3.6	1.9	1.9	126	264	263	60		86	86	3
3	52:49	14:59-15:02	580.545											
4														
5														
6														
1														
2														
3														
4														
5														
6														

ΔV<sub>m</sub> = 41.202  $\sqrt{\Delta p}$  = 1.9372  $\Delta H$  = 1.96  $T_s$  = 114.1  $T_m$  = 79 ✓

Ave ΔH = 3.7533

YUK



## SAMPLE RECOVERY DATA

Plant CK steel Middletown Run No. P-316-2  
 Date 8/31/16 Sample Box No. SB-7 Job No. 50074.0172  
 Sample Location Pushing Bay house Filter No. NA  
 Train Preparer CT Sample Head No. SK-3  
 Sample Recovery Person DA Barometer No. W.C. Co  
 Comments 316 Balance No. 2

Front Half

Acetone \_\_\_\_\_ Liquid \_\_\_\_\_  
 Container No. NA Level Marked \_\_\_\_\_ Sealed \_\_\_\_\_

Filter

Container No. NA Sealed \_\_\_\_\_

Description of Filter \_\_\_\_\_

Samples Stored and Locked \_\_\_\_\_

Back Half/Moisture

Container No. 2 1500 2 Imp. ; 300 Imp.

Liquid Level Marked \_\_\_\_\_ Sealed \_\_\_\_\_

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	TYPE 1 H <sub>2</sub> O	100	761.8	769.2	7.4 ✓
2	TYPE 1 H <sub>2</sub> O	100	776.9	779.3	2.4 ✓
3	—	—	689.1	689.7	0.6 ✓
4	SG	250	906.1	916.4	10.3 ✓
5					
6					
Total					20.7 ✓ <i>dk</i>

Description of Impinger Catch: Clear

BWS = 2.3%

B<sub>20</sub> = 100.6

Plant: AK Middleton Sample Type: M316 Operator: NP Nozzle ID: 152 Thermocouple #: 73-6  
 Sampling Location: Bighouse Stack Pbar: 30.08 Ps: -1.1 Assumed Bws: 1.5 Filter #: —  
 Run Number: P-316-3 Date: 9-1-16 CO<sub>2</sub>: CEM O<sub>2</sub>: CEM Meter Box #: 11 Y: 1.010 ΔH@: 1.791  
 Pretest Leak Rate: 0.001 cfm @ 10 in.Hg. Probe Length/Type: 3'6" Pitot#: 13-6 Post-Test Leak Rate: 0.001 cfm @ 3 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: — Stack Diameter: 35.5" K: 5562 Post-Test Leak Check: Pitot: ✓ Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. 9f	Aux. Temp.	Dry Gas Meter Temp. Tm		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	10:30	581.030											
1	3:29	10:20-10:31	583.738	3.9	2.1	2.1	90	262	263	65	NA	73	73	3
2	7:05	10:35-10:36	586.550	3.8	2.0	2.0	93	259	261	65		71	71	3
3	10:46	10:47-10:51	589.554	3.7	2.0	2.0	97	262	262	64		71	71	3
4	14:20	10:50-11:01	592.312	3.8	2.0	2.0	100	258	262	64		71	71	3
5	17:49	11:30-11:33	594.976	3.8	2.0	2.0	103	263	263	60		71	71	3
6	21:23	11:42-11:45	597.797	3.9	2.0	2.0	105	261	267	61		72	71	3
1	25:01	12:00-12:04	600.648	4.0	2.1	2.1	107	261	263	58		72	72	3
2	28:38	12:14-12:33	603.475	4.0	2.1	2.1	110	259	261	59		73	72	3
3	32:06	12:38-12:42	606.315	4.0	2.1	2.1	114	264	261	59		73	73	3
4	35:31	12:51-13:00	608.965	3.9	2.0	2.0	117	257	264	60		74	74	3
5	39:10	13:16-13:19	611.790	3.9	2.0	2.0	118	257	259	60		75	74	3
6	42:55	13:35-13:39	614.727	3.7	1.9	1.9	118	259	261	60		75	75	3
1	46:30	13:45-13:49	617.482	3.7	1.9	1.9	115	257	263	61		75	74	3
2	50:08	14:11-14:15	620.343	4.0	2.1	2.1	116	265	265	61		75	75	3
3	53:44	14:52-14:55	623.115	4.0	2.1	2.1	117	263	260	59		76	75	3
4	57:10	15:10-15:13	625.801	4.0	2.1	2.1	116	262	262	62		76	76	3
5														
6														
1	57:17 marks													
2														
3														
4														
5														
6														

$$\Delta V_m = 44.771 \sqrt{\Delta p} = 1.9649 \Delta H = 2.0312 T_s = 109$$

$$T_m = 73$$

$$Ave DP = 3.4813$$

## SAMPLE RECOVERY DATA

Plant AK Middletown Run No. P-316-3  
 Date 9/1/16 Sample Box No. SB 2 Job No. 050074-0172  
 Sample Location Pushing Bayhouse Filter No. NA  
 Train Preparer BF Sample Head No. SH-5  
 Sample Recovery Person BF Barometer No. TWC.com  
 Comments 316 Balance No. FB-2

Front Half

Acetone Liquid  
 Container No. NA Level Marked — Sealed —

## Filter

Container No. NA Sealed —

Description of Filter —

Samples Stored and Locked —

Back Half/Moisture

Container No. 2 1st & 2nd Empty vs; 3rd Impinger

Liquid Level Marked ✓ Sealed ✓

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	Type 1 H <sub>2</sub> O	100	791.7	793.5	1.8
2	Type 1 H <sub>2</sub> O	100	771.6	773.6	2.0
3	Empty	—	653.1	654.2	1.1
4	Silica Gel	250	927.6	936.9	9.3
5					
6					
Total			3144	3158.2	14.2 ✓/AK

Description of Impinger Catch: clear

Loss = 1.5%

2nd = 99.4%

**METHOD 18 SAMPLING DATA**

Company: AK MIDDLETOWN

City: MIDDLETOWN, OH

Date: 8/30/16

Location: PRESSURE BACKHOUSE (STACK)

Time: 1026 - 1602

Run No: P-0031-1

Meter No: VB-1

Orifice, CC: \_\_\_\_\_

Barometric Pressure, in.Hg: 30.23

Operator: CJ

Ambient Temperature, EF: 84

1A = 19.44 L, T<sub>m</sub> = 87

1B = 19.5 L, T<sub>m</sub> = 91.5

**VACUUM LEAK CHECK DATA**

	Initial, in.Hg	Final, in.Hg	Time, min
Pre-test	25	25	1
Post-test			

TRAP#

Sample time, min	Clock time, (24-h)	Meter volume, liters	Rotameter Setting	Dry gas meter temp. EF	Vacuum, in.Hg
0 -	<del>1026 - 1029</del>	7657.65	1 1/4 min	85 85	3
2:40	1026 - 1027	7660.50		85 85	3
6:03	1043 - 1046	7663.69		87 87	3
9:30	1119 - 1122	7666.92		88 88	3
13:00	1139 - 1142	7670.27		89 89	3
16:28	1200 - 1204	7673.54		89 89	3
20:00	1211 - 1214	7677.09		89 89	3
23:22	1231 - 1234	7680.42		89 89	3
26:47	1244 - 1248	7683.85		90 90	3
30:03	1258 - 1302	7686.93		91 91	3
33:18	1316 - 1319	7689.98		92 92	3
36:33	1335 - 1338	7693.24		92 93	3
38:00	1345 - 1347	7694.60		93 93	3
40:00	1348 - 1350	7696.59		93	3

Probe Color

264 61  
264 60  
266 60  
266 56  
263 62  
265 56  
264 58  
265 63  
266 60  
265 58  
265 55  
265 60  
265 52  
265 53

$$V_{std} = V_m \text{ liters} \times Y \times 17.647 \times \frac{P_b, \text{in. Hg}}{T_m, ^\circ R}$$



**METHOD 18 SAMPLING DATA**

Company: AK STEEL City: MIDDLETOWN, OH  
 Date: 8/31/16 Location: PUSHING BAGHOUSE  
 Time: 1020 - 1603 Run No: P-0031-2  
 Meter No: VB-1 Orifice, CC: \_\_\_\_\_  
 Barometric Pressure, in.Hg: 30.05 Operator: CJ  
 Ambient Temperature, EF: 79

2A = 19.672, Tm = 86  
 2B = 19.422, Tm = 93

**VACUUM LEAK CHECK DATA**

Initial, in.Hg Final, in.Hg Time, min  
 Pre-test 25 25 1  
 Post-test \_\_\_\_\_

TRAP #

29

19

Sample time, min	Clock time, (24-h)	Meter volume, liters	Rotameter Setting	Dry gas meter temp. EF	Vacuum, in.Hg
0	-	7736.44	-	-	-
3:20	1020-1024	7739.74	1 L/min	82 82	3
6:44	1035-1039	7743.10		84 84	3
10:05	1049-1052	7746.50		86 86	3
13:22	1104-1107	7749.76		87 87	3
16:40	1123-1126	7752.95		87 87	3
20:00	1141-1145	7756.11		89 89	3
23:21	1200-1204	7759.24		90 90	3
26:42	1220-1224	7762.57		92 92	3
30:00	1239-1242	7765.96		94 94	3
33:19	1257-1301	7769.26		94 94	3
36:41	1316-1319	7772.52		94 94	3
40:00	1335-1339	7775.53		94 94	3

PROBE CORR  
 268 64  
 269 64  
 262 62  
 263 63  
 262 65  
 261 66  
 263 62  
 259 60  
 260 60  
 263 59  
 263 60  
 260 62  
 261 64

$$V_{std} = V_m \text{ liters} \times Y \times 17.647 \times \frac{P_b, \text{in. Hg}}{T_m, ^\circ R}$$

**METHOD 18 SAMPLING DATA**

Company: AK STEEL City: MIDDLETOWN, OH  
 Date: 8/31/16 Location: PRESSURE BH  
 Time: 1020-1603 Run No: P-0031-2  
 Meter No: VB-1 Orifice, CC: \_\_\_\_\_  
 Barometric Pressure, in.Hg: 30.05 Operator: CJ  
 Ambient Temperature, EF: 79

**VACUUM LEAK CHECK DATA**

	Initial, in.Hg	Final, in.Hg	Time, min
Pre-test	<u>25</u>	<u>25</u>	<u>1</u>
Post-test	<u>25</u>	<u>25</u>	<u>1</u>

TRAP #

10

Sample time, min	Clock time, (24-h)	Meter volume, liters	Rotameter Setting	Dry gas meter temp. EF		Vacuum, in.Hg	PROBE	CONDENS
43:20	1448-1452	7778.49	1 L/min	92	92	3	262	61
46:40	1459-1503	7781.79		90	90	3	264	59
50:00	1510-1514	7784.99		87	87	3	267	56
53:23	1525-1529	7788.16		83	83	3	265	57
56:41	1543-1546	7791.27		82	82	3	268	62
60:00	1600-1603	7794.41		83	83	3	268	65
		$V_m = 57.972$		$Avg = 88.3^\circ F$				

$$V_{std} = V_m \text{ liters} \times Y \times 17.647 \times \frac{P_b, \text{in. Hg}}{T_m, ^\circ R}$$

15.92 L,  $T_m = 86$



**METHOD 18 SAMPLING DATA**

Company: AK STEEL

City: MIDDLETOWN, OH

Date: 9/1/16

Location: PUSHING BAGHOUSE

Time: 1020 -

Run No: P-0031-3

Meter No: VB-1

Orifice, CC: \_\_\_\_\_

Barometric Pressure, in.Hg: 30.08

Operator: CJ

Ambient Temperature, EF: 72

3A = 19.38L, T<sub>at</sub> = 72

**VACUUM LEAK CHECK DATA**

3B = 16.36L, T<sub>at</sub> = 71

	Initial, in.Hg	Final, in.Hg	Time, min
Pre-test	<u>24</u>	<u>24</u>	<u>1</u>
Post-test	_____	_____	_____

Sample time, min	Clock time, (24-h)	Meter volume, liters	Rotameter Setting	Dry gas meter temp. EF	Vacuum, in.Hg
0	—	7795.50	—	—	—
3:17	10:20-1023	7798.71	1 L/min	69 69	3
6:40	10:35-1038	7801.86		71 71	3
10:00	1047-1050	7805.08		72 72	3
13:20	1118-1122	7808.40		73 73	3
16:40	1130-1133	7811.66		73 73	3
20:00	1142-1145	7814.88		74 74	3
23:21	1200-1204	7818.40		74 74	3
26:40	1219-1223	7821.53		75 75	3
30:00	1238-1242	7824.84		76 76	3
33:20	1257-1300	7828.17		77 77	3
36:40	1316-1319	7831.47		77 77	3
40:00	1335-1338	7834.76		78 78	3

Pre-test	Cond
262	59
261	59
265	59
265	60
263	60
265	60
264	63
264	64
264	66
263	62
265	57
263	59

TRAP #  
15

✓ 25 7834.88  
25 7835.19

20

✓ 25 7834.76  
7835.33

$$V_{std} = V_m \text{ liters} \times Y \times 17.647 \times \frac{P_b, \text{in. Hg}}{T_m, ^\circ R}$$



Plant: AK MiddletonSample Type: M316 Operator: GDSampling Location: Combustion StackRun Number: C-316-1 Date: 9-8-16Pretest Leak Rate: .000 cfm @ 8 in.Hg.Pretest Leak Check: Pitot: ✓ Orsat: —Sample Type: M316 Operator: GDPbar: 30.00 Ps: 15CO<sub>2</sub>: 3 O<sub>2</sub>: 15Probe Length/Type: 5' 61" Pitot#: T5-8Stack Diameter: 168" K: 59.7454Nozzle ID: 0.50 Thermocouple #: T5-8Assumed Bws: 12 Filter #: By-passMeter Box #: 5 Y: .983 AH@: 1.906Post-Test Leak Rate: .000 cfm @ 4 in.Hg.Post-Test Leak Check: Pitot: ✓ Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	AH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	0953	083.757											
1	2.5	0955	085.4	.03	1.1	1.1	370	236	261	67	N.A.	68	68	0
2	5	0958	087.2	.03	1.1	1.1	374	237	265	63		69	69	0
3	7.5	1000	088.3	.03	1.1	1.1	377	236	264	57		70	69	0
4	10	1003	089.7	.03	1.1	1.1	379	237	267	56		71	69	0
5	12.5	1005	091.2	.03	1.1	1.1	371	238	265	56		71	69	0
6	15	1008	092.6	.03	1.1	1.1	375	239	261	55		72	70	0
7	17.5	1010	094.0	.03	1.1	1.1	378	240	263	54		74	70	0
8	20	1013	095.4	.03	1.1	1.1	378	241	261	56		74	70	0
9	22.5	1015	097.0	.03	1.1	1.1	376	240	260	56		74	70	0
10	25	1018	098.5	.04	1.5	1.5	380	241	261	57		76	71	0
11	27.5	1020	099.9	.04	1.5	1.5	379	247	267	58		76	71	0
12	30	1023	101.9	.04	1.5	1.5	380	248	267	59		77	71	0
1	32.5	1025	103.6	.04	1.5	1.5	385	250	260	59		78	71	0
2	35	1028	105.2	.04	1.5	1.5	387	251	258	60		79	72	0
3	37.5	1030	106.9	.04	1.5	1.5	390	252	262	61		79	72	0
4	40	1033	108.6	.04	1.5	1.5	392	253	260	59		80	72	0
5	42.5	1035	110.0	.03	1.1	1.1	397	260	261	59		81	72	0
6	45	1038	111.5	.03	1.1	1.1	398	260	262	59		81	72	0
7	47.5	1040	113.0	.03	1.1	1.1	398	259	268	61		81	72	0
8	50	1043	114.5	.03	1.1	1.1	380	260	266	56		82	72	0
9	52.5	1045	116.0	.03	1.2	1.2	370	265	264	58		83	73	0
10	55	1048	117.6	.03	1.2	1.2	372	264	265	59		83	75	0
11	57.5	1050	119.2	.03	1.2	1.2	372	264	261	60		84	75	0
12	60	1053	120.718	.03	1.2	1.2	373	263	265	58		85	76	0

$$\Delta V_m = 36.961 \quad \sqrt{\Delta p} = 10.07 \quad \Delta H = 1.2 \quad T_s = 380$$

$$\Delta P = 1466 \quad \Delta P = 1466 \quad \Delta P = 1466$$

$$T_m = 74$$

## SAMPLE RECOVERY DATA

Plant AK Steel Middletown Run No. C-3/6-1  
 Date 9/8/16 Sample Box No. SB-7 Job No. SDW74.0172  
 Sample Location Combustion Filter No. NA  
 Train Preparer DA Sample Head No. SA-3  
 Sample Recovery Person DA Barometer No. TWC  
 Comments M316 formaldehyde Balance No. 2

Front Half

Acetone Liquid  
 Container No. NA Level Marked Sealed

Filter  
 Container No. NA Sealed

Description of Filter

Samples Stored and Locked

Back Half/Moisture

Container No. 1st: ZND Impinger, 3RD Impinger

Liquid Level Marked Sealed

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	H <sub>2</sub> O	100	759.2	839.7	80.5
2	H <sub>2</sub> O	100	786.7	800.2	13.5
3	<del>empty</del>	693.8	<del>689.7</del>	697.8 <sup>2</sup>	3.4
4	SG	250	916.4	924.6	8.2
5					
6					
Total					105.6

Description of Impinger Catch: Blackish 1st Imp.

BWS = 12.0%

ISO = 94.6%

WAP

Plant: AK Middleton Sample Type: M3/6 Operator: GD Nozzle ID: 0.50 Thermocouple #: 15-8  
 Sampling Location: Combustion Stack Pbar: 30.00 Ps: -.8 Assumed Bws: 12 Filter #: Bypass  
 Run Number: C-316-2 Date: 9/8/16 CO<sub>2</sub>: 3 O<sub>2</sub>: 15 Meter Box #: 5 Y: 0.993 ΔH@: 1.906  
 Pretest Leak Rate: .000 cfm @ 7 in.Hg. Probe Length/Type: 5'61 Pitot#: 15-8 Post-Test Leak Rate: 1000 cfm @ 4 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: — Stack Diameter: 168" K: 59.7154 Post-Test Leak Check: Pitot: ✓ Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	1246	120.953											
1	2.5	1248	122.5	.03	1.2	1.2	372	254	267	66	N.A.	76	76	0
2	5.0	1251	124.0	.03	1.2	1.2	373	260	269	63		78	78	0
3	7.5	1253	125.5	.03	1.2	1.2	374	261	268	62		79	78	0
4	10	1256	127.0	.03	1.2	1.2	375	266	270	60		80	79	0
5	12.5	1258	128.6	.03	1.2	1.2	376	258	268	59	✓	81	79	0
6	15	1301	130.2	.03	1.2	1.2	378	258	266	58		82	79	0
7	17.5	1303	131.7	.03	1.2	1.2	379	257	265	59		83	79	0
8	20	1305	133.3	.03	1.2	1.2	382	256	269	62		84	79	0
9	22.5	1308	134.8	.03	1.2	1.2	371	258	263	63		85	80	0
10	25	1310	136.3	.03	1.2	1.2	378	260	265	59		85	80	0
11	27.5	1313	137.9	.03	1.2	1.2	380	263	267	60		87	81	0
12	30	1315	139.5	.04	1.5	1.5	380	265	263	59		87	81	0
1	32.5	1318	141.4	.04	1.5	1.5	383	266	268	58		88	81	0
2	35	1320	143.0	.04	1.5	1.5	384	264	266	57		89	81	0
3	37.5	1323	144.7	.04	1.5	1.5	385	264	268	58		90	81	0
4	40	1325	146.5	.04	1.5	1.5	387	262	267	58		90	82	0
5	42.5	1328	148.0	.04	1.5	1.5	386	263	267	58		90	82	0
6	45	1330	149.4	.03	1.2	1.2	388	263	265	57		91	83	0
7	47.5	1333	151.2	.03	1.2	1.2	389	265	266	59		91	83	0
8	50	1335	152.8	.03	1.2	1.2	392	265	261	63		91	83	0
9	52.5	1338	154.4	.03	1.2	1.2	394	267	265	64		92	83	0
10	55	1340	155.8	.03	1.1	1.1	396	265	266	60		93	84	0
11	57.5	1343	157.3	.03	1.2	1.2	372	260	267	58		93	85	0
12	60	1346	158.837	.03	1.2	1.2	370	263	264	57		94	85	0

$$\Delta V_m = 37.884 \quad \sqrt{\Delta p} = 1.799 \quad \Delta H = 1.27 \quad T_s = 381$$

$$T_m = 84$$

$$\Delta p = .0325$$

NP

## SAMPLE RECOVERY DATA

Plant Ak steel Middletown Run No. C-316-2  
 Date 9/8/16 Sample Box No. SB-2 Job No. SDU 74-972  
 Sample Location Combustion stack Filter No. NA  
 Train Preparer DA/BR Sample Head No. 5  
 Sample Recovery Person DA Barometer No. TWC-com  
 Comments method 316 formaldehyde Balance No. 2

Front Half

Acetone Liquid  
 Container No. NA Level Marked NA Sealed NA

Filter  
 Container No. NA Sealed —

Description of Filter —

Samples Stored and Locked —

Back Half/Moisture

Container No. 1st } 2ND Imps; 3RD Imps

Liquid Level Marked ✓ Sealed ✓

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	Type I H <sub>2</sub> O	100	789.5	868.0	78.5
2	Type I H <sub>2</sub> O	100	772.4	784.6	12.2
3	empty	—	655.2	658.0	2.8
4	SG	250	965.6	976.6	11.0
5					
6					
Total					104.5

Description of Impinger Catch: 1st } 2ND Imps Blackish

aws = 11.8%

Σ = 104.0%

*(Signature)*

## FIELD DATA SHEET

Plant: AK Middleton Sample Type: M316 Operator: NP Nozzle ID: 0.50 Thermocouple #: T5-8  
 Sampling Location: Combustion Stack Pbar: 30.00 Ps: 20 Assumed Bws: 10 Filter #: NA  
 Run Number: C-316-3 Date: 9-8-16 CO<sub>2</sub>: 3 O<sub>2</sub>: 15 Meter Box #: 5 Y: .993 ΔH@: 1.906  
 Pretest Leak Rate: .001 cfm @ 10 in.Hg. Probe Length/Type: 5'61 Pitot#: T5-8 Post-Test Leak Rate: .002 cfm @ 8 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: — Stack Diameter: 168" K: 59.7954 Post-Test Leak Check: Pitot: ✓ Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	1549	159.005											
1	2.5	1551	160.5	.03	1.2	1.2	390	252	266	65	NA	87	86	0
2	5	1554	162.1	.03	1.2	1.2	375	263	267	65		87	87	0
3	7.5	1556	163.5	.03	1.2	1.2	376	264	270	65		87	87	0
4	10	1559	165.0	.03	1.2	1.2	378	264	270	64		87	87	0
5	12.5	1601	166.5	.03	1.2	1.2	376	264	269	64		88	87	0
6	15	1604	168.1	.03	1.2	1.2	375	263	268	63		88	87	0
7	17.5	1606	164.7	.03	1.2	1.2	378	266	275	63		88	87	0
8	20	1609	171.0	.03	1.2	1.2	378	267	276	63		88	87	0
9	22.5	1611	172.8	.03	1.2	1.2	379	264	272	63		90	87	0
10	25	1614	174.4	.03	1.2	1.2	379	263	268	63		90	88	0
11	27.5	1616	175.9	.03	1.2	1.2	380	264	260	62		90	88	0
12	30	1619	177.6	.03	1.2	1.2	379	267	259	62		90	88	0
1	32.5	1621	179.4	.03	1.2	1.2	379	263	269	61		91	87	0
2	35	1624	180.6	.03	1.2	1.2	378	264	263	61		92	87	0
3	37.5	1626	182.2	.03	1.2	1.2	378	264	269	61		93	88	0
4	40	1629	183.8	.03	1.2	1.2	380	267	271	60		93	88	0
5	42.5	1631	185.1	.03	1.2	1.2	379	265	264	60		93	88	0
6	45	1634	186.8	.03	1.2	1.2	382	262	272	61		94	88	0
7	47.5	1636	188.4	.03	1.2	1.2	380	262	271	61		94	88	0
8	50	1639	189.9	.03	1.2	1.2	376	265	272	62		95	89	0
9	52.5	1641	191.5	.03	1.2	1.2	389	265	264	62		95	89	0
10	55	1644	193.0	.03	1.2	1.2	386	264	268	62		95	89	0
11	57.5	1646	194.5	.03	1.2	1.2	381	264	273	63		96	90	0
12	60	1649	196.276	.03	1.2	1.2	384	264	271	64		96	90	0

$$\Delta V_m = 37.251 \sqrt{\Delta p} = .1732 \sqrt{\Delta H} = 1.2 \quad T_s = 380$$

$$T_m = 89$$

$$\text{Ave } O_2 = .03$$

## SAMPLE RECOVERY DATA

Plant Ak steel Middletown Run No. E-316-3  
 Date 9/8/16 Sample Box No. 7 Job No. 50074.0172  
 Sample Location Combustion Stack Filter No. NA  
 Train Preparer DA Sample Head No. 3  
 Sample Recovery Person DA Barometer No. TWC  
 Comments M316 - formaldehyde Balance No. 2

Front Half

Acetone Liquid  
 Container No. NA Level Marked \_\_\_\_\_ Sealed \_\_\_\_\_

Filter

Container No. NA Sealed \_\_\_\_\_

Description of Filter NA

Samples Stored and Locked NA

Back Half/Moisture

Container No. 1st; 2nd Impingers; 3rd Impinger

Liquid Level Marked \_\_\_\_\_ Sealed ✓

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	H <sub>2</sub> O	100	766.0	824.4	58.4
2	H <sub>2</sub> O	100	780.4	790.0	9.6
3	empty	-	692.5	696.0	3.5
4	SO <sub>2</sub>	200	909.8	924.1	14.3
5					
6					
Total					85.8

Description of Impinger Catch: 1st; 2nd Impingers - Duct Gas

$$B_{ws} = 10.1\%$$

$$T_{60} = 103.6\%$$

NA



Operator: AP

Sample Type:

Pbar: 30.24 . Pp

CO <sub>2</sub> :	3	O <sub>2</sub> :	15
CO <sub>2</sub> :	3 <td>O<sub>2</sub>:</td> <td>15</td>	O <sub>2</sub> :	15

Probe Length/Type: 6' 6L Pitot#: 76-15P

Stack Diameter: 168" K: 53 113

1

Nozzle ID: 500 Thermocouple #: 76-1570  
 Assumed Bws: 10 Filter #: —  
 Meter Box #: 2 Y: 1.005  $\Delta H @$ : 1.687  
 Post-Test Leak Rate: 0.01 cfm @ 10 in.Hg.  
 Post-Test Leak Check: Pitot: ✓ Orsat: —

[illegible]
$$\Delta V_m = \underline{10.917} \quad \sqrt{\Delta p} = \underline{2020} \quad \Delta H = \underline{1425} \quad T_s = \underline{356}$$

Tm = 67

avg Df = 0.4083

Formaldehyde

**SAMPLE RECOVERY DATA**

Plant AK Middletown Run No. C-316-4  
 Date 9/15/16 Sample Box No. SB-2 Job No. 050074.0172  
 Sample Location Combustion Stack Filter No. NA  
 Train Preparer BF Sample Head No. SH-5  
 Sample Recovery Person BF Barometer No. TWC.000  
 Comments M 316 Balance No. FB-2

Front Half

~~Acetone~~ Liquid  
 Container No. e-316-4 Level Marked ☒ Sealed ☒

Filter  
 Container No. NA Sealed NA

Description of Filter NA

Samples Stored and Locked ☒

Back Half/Moisture

Container No. NA

Liquid Level Marked NA Sealed NA

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	H <sub>2</sub> O	100	788.5	881.9	93.4
2	H <sub>2</sub> O	100	772.1	789.6	1.1
3	—	—	653.8	656.5	2.7
4	Silica Gel	250	964.0	973.8	9.8
5					
6					
Total					107.0

Description of Impinger Catch: clear

107

VOLATILE ORGANIC SAMPLING TRAIN (VOST) SAMPLING DATA  
EPA METHOD 30

C-0031-1A  
1B  
1C

Company: AK Steel Mill  
Date: 9/9/16  
Time: 0935-0955-1A  
Meter #: V/B-2  
Barometric Pressure, in. Hg: 30.00  
Ambient Temperature, °F: \_\_\_\_\_  
City: Millersburg  
Location: Conductivity Creek  
Run #: C-0031-1A  
Y-Factor: 1.085  
Operator: MLL  
Purge Time: 10 min

Vacuum Leak Check Data

Pre-test: Initial, in. Hg 22  
Post-test: Final, in. Hg 22  
Time, min. 1  
Pre-test: Initial, in. Hg 22  
Post-test: Final, in. Hg 22  
Time, min. 1

Sample Time (min)	Clock Time (24-hr)	Meter Volume (liter)	Rotameter Setting	Dry Gas Meter Temp. (°F)	Vacuum (in. Hg)	Probe Temp. °F
0	0935	4449.03	1.0	86	3	260
5	0940	4453.4	1.0	88	3	258
10	0945	4458.4	1.1	88	3	262
15	0950	4463.4	1.1	90	3	262
20	0955	4468.36	1.1	90	3	260
0	1008	4466.10	1.1	92	3	259
5	1013	4474.30	1.1	92	3	257
10	1018	4479.10	1.1	95	3	258
15	1023	4484.05	1.1	94	3	259
20	1028	4488.84	1.1	97	3	258

Nitrogen purge/activated carbon packing in sample holding container:

$$V_{std} = V_m(\text{liters}) \times Y \times 17.647 \times \frac{P_b(\text{in. Hg})}{T_m(^{\circ}R)}$$

1A = L1803694-34 Vost to 10 #9 = 19.33L, Tm = 98  
1B = L1803694-57 Vost to 10 #32 = 19.74L, Tm = 94

1028-1008-1B

1A

Conductivity

C-0031-1C  
L 1803694-29 Tmo #4

19.91 l, Tm = 95

**EPA METHOD 30**  
**VOLATILE ORGANIC SAMPLING TRAIN (VOST) SAMPLING DATA**

Company: AK Steel  
 Date: 9/8/16  
 Time: 1041-1101  
 Meter #: V/B-2  
 Barometric Pressure, in.Hg: 30.00  
 Ambient Temperature, °F: \_\_\_\_\_

City: Middlebourn MA  
 Location: Coniston Brook  
 Run #: C-0031-1C  
 Y-Factor: 1.085  
 Operator: ML  
 Purge Time: 5

Vacuum Leak Check Data

	Initial, in.Hg	Final, in.Hg	Time, min.	
Pre-test:	25	25	1	0.00 l 1C
Post-test:	5	5	1	0.00 l

Sample Time (min)	Clock Time, (24-hr)	Meter Volume, (liter)	Rotameter Setting	Dry Gas Meter Temp., (°F)		Vacuum, (in.Hg)	Probe Temp, °F	
0	1041	4489.69	1.1	94	94	3	258	54
5	1046	4495.5	1.1	96	95	3	259	54
10	1051	4500.0	1.1	96	95	3	260	54
15	1056	4504.75	1.1	96	95	3	260	55
20	1101	4509.60	1.1	95	95	3	258	56
0	1112	4510.25	1.1	94	94	3	261	57
5	1117	4515.1	1.1	94	94	3	261	60
10	1122	4520.1	1.1	95	95	3	262	56
15	1127	4525.2	1.1	95	95	3	258	50
20	1132	4530.19	1.1	96	96	3	260	48
Rate for 8" l/min = 0.00 l								

Nitrogen purge/activated carbon packing in sample holding container: \_\_\_\_\_

$$V_{std} = V_m(\text{liters}) \times Y \times 17.647 \times \frac{P_b(\text{in.Hg})}{T_m(^{\circ}\text{R})}$$

C-0031-1D = 19.94 l  
 L 1803694-30 Tm = 95  
 Tmo #5

**EPA METHOD 30  
VOLATILE ORGANIC SAMPLING TRAIN (VOST) SAMPLING DATA**

Company: AK Steel - MiddletownCity: Middletown, OHDate: 9/8/16Location: Combustion StackTime: 1144<sup>1E</sup> - 1204 / 1FRun #: C-0031-1EMeter #: VB-2Y-Factor: 1.085Barometric Pressure, in.Hg: 30.00Operator: pk

Ambient Temperature, °F: \_\_\_\_\_

Purge Time: \_\_\_\_\_

Vacuum Leak Check Data

	Initial, in.Hg	Final, in.Hg	Time, min.
Pre-test: <u>1E</u>	<u>22</u>	<u>22</u>	<u>1 0.00 l</u>
Post-test: <u>1F</u>	<u>21</u>	<u>21</u>	<u>1 0.00 l</u>

Pack test5" e / min = 0.00 l5" e / min = 0.00 l

Sample Time (min)	Clock Time, (24-hr)	Meter Volume, (liter)	Rotameter Setting	Dry Gas Meter Temp., (°F)		Vacuum, (in.Hg)	Probe Temp, °F	
0	1144	4530.85	1.1	97	96	3	267	48
5	1149	4535.83	1.1	98	97	3	258	49
10	1154	4540.05	1.1	97	97	3	261	49
15	1159	4544.8	1.1	98	98	3	259	50
20	1204	4549.68	1.1	98	97	3	262	49
0	1215	4550.32	1.1	99	99	2	257	50
5	1220	4555.4	1.1	99	99	2	260	52
10	1225	4560.2	1.1	101	99	2	258	51
15	1230	4564.55	1.1	102	100	2	259	52
20	1235	4569.32	1.1	102	100	2	263	53
<u>Post test</u>								

Nitrogen purge/activated carbon packing in sample holding container: \_\_\_\_\_

$$V_{std} = V_m (\text{liters}) \times Y \times 17.647 \times \frac{P_b (\text{in.Hg})}{T_m (^\circ R)}$$

C-0031-1E = L1803694-52  $T_{m} \#27 = 18.83^\circ C$ ,  $T_m = 97$

C-0031-1F = L1803694-36  $T_{m} \#11 = 19.00^\circ C$ ,  $T_m = 100$

C-0031-2A + 2B

## EPA METHOD 30

## VOLATILE ORGANIC SAMPLING TRAIN (VOST) SAMPLING DATA

Company: AK Steel  
 Date: 9/8/16  
 Time: 1245-1305  
 Meter #: VB-2  
 Barometric Pressure, in.Hg: 30.00  
 Ambient Temperature, °F: \_\_\_\_\_

City: Middlebush OH  
 Location: Continuum Stack  
 Run #: 2A / 2B  
 Y-Factor: 1.085  
 Operator: mlh  
 Purge Time: \_\_\_\_\_

## Vacuum Leak Check Data

	Initial, in.Hg	Final, in.Hg	Time, min.	
Pre-test: <u>2A</u>	<u>22</u>	<u>22</u>	<u>1</u>	<u>0.00 l</u>
Post-test: <u>2B</u>	<u>25</u>	<u>25</u>	<u>1</u>	<u>0.00 l</u>

Sample Time (min)	Clock Time, (24-hr)	Meter Volume, (liter)	Rotameter Setting	Dry Gas Meter Temp., (°F)		Vacuum, (in.Hg)	Probe Temp, °F	Conduct
0	1245	4569.70	1.1	102	101	3	266	57
5	1250	4575.2	1.1	103	102	3	266	58
10	1255	4579.76	1.1	103	102	3	259	63
15	1300	4584.8	1.1	104	103	3	258	59
20	1305	4589.29	1.1	104	102	3	260	51
Purge Purge = 0.00 l @ 5"								
0	1315	4589.85	1.1	101	101	3	262	49
5	1320	4594.53	1.1	102	101	3	259	49
10	1325	4599.5	1.1	102	102	3	259	49
15	1330	4604.4	1.1	103	102	3	259	49
20	1335	4608.75	1.1	102	101	3	258	50
Purge Purge								

Nitrogen purge/activated carbon packing in sample holding container: \_\_\_\_\_

$$V_{std} = V_m (\text{liters}) \times Y \times 17.647 \times \frac{P_b (\text{in. Hg})}{T_m (^\circ \text{R})}$$

C-0031-2A = L1803694-42 Tr/b 17 = 19.59 l,  $T_m = 102.6$

C-0031-2B = L1803694-37 Tr/b 12 = 18.90 l,  $T_m = 102$

**EPA METHOD 30  
VOLATILE ORGANIC SAMPLING TRAIN (VOST) SAMPLING DATA**

Company: AK Steel  
 Date: 9/8/16  
 Time: 1345-1405 / 1415-1435  
 Meter #: VB-2  
 Barometric Pressure, in.Hg: 30.00  
 Ambient Temperature, °F: \_\_\_\_\_

City: Middletown OH  
 Location: Combustion Stack  
 Run #: 2C / 2D  
 Y-Factor: 1.085  
 Operator: nm  
 Purge Time: \_\_\_\_\_

Vacuum Leak Check Data

	Initial, in.Hg	Final, in.Hg	Time, min.
Pre-test: <u>2C</u>	<u>25</u>	<u>25</u>	<u>1</u> <u>0.00 l</u>
Post-test: <u>2D</u>	<u>23</u>	<u>23</u>	<u>1</u> <u>0.00 l</u>

Sample Time (min)	Clock Time, (24-hr)	Meter Volume, (liter)	Rotameter Setting	Dry Gas Meter Temp., (°F)		Vacuum, (in.Hg)	Probe Temp, °F	
0	1345	4609.50	1.1	102	102	4	265	52
5	1350	4614.5	1.1	102	102	4	266	51
10	1355	4619.2	1.1	103	102	4	259	51
15	1400	4624.1	1.1	102	102	4	261	52
20	1405	4628.90	1.1	103	103	4	257	52
Per test 5" @ 1 m.u. = 0.00 l								
0	1415	4629.55	1.1	103	102	4	258	54
5	1420	4634.45	1.1	103	102	4	260	55
10	1425	4639.2	1.1	104	103	4	260	55
15	1430	4644.1	1.1	104	103	4	257	58
20	1435	4648.95	1.1	105	105	4	259	61

Nitrogen purge/activated carbon packing in sample holding container: \_\_\_\_\_

$$V_{std} = V_m (\text{liters}) \times Y \times 17.647 \times \frac{P_b (\text{in. Hg})}{T_m (^\circ R)}$$

C-0031-2C L1803694-61  $T_{no} 36 = 19.34^\circ C$   
 $T_{m1} = 102$   
 C-0031-2D L1803694-27  $T_{no} 2 = 19.40^\circ C$   
 $T_{m1} = 103$

**EPA METHOD 30  
VOLATILE ORGANIC SAMPLING TRAIN (VOST) SAMPLING DATA**

Company: AK Steel  
 Date: 9/8/16  
 Time: 2E 1445-1505 / 2F  
 Meter #: VB-2  
 Barometric Pressure, in.Hg: 30.00  
 Ambient Temperature, °F: \_\_\_\_\_

City: Middletown, OH  
 Location: Carbonian Steel  
 Run #: 2E / 2F  
 Y-Factor: 1.085  
 Operator: MLL  
 Purge Time: \_\_\_\_\_

Vacuum Leak Check Data

	Initial, in.Hg	Final, in.Hg	Time, min.
Pre-test: <u>2E</u>	<u>25</u>	<u>25</u>	<u>1 0.00 l</u>
Post-test: <u>2E</u>	<u>23</u>	<u>23</u>	<u>1 0.00 l</u>

Sample Time (min)	Clock Time, (24-hr)	Meter Volume, (liter)	Rotameter Setting	Dry Gas Meter Temp., (°F)	Vacuum, (in.Hg)	Probe Temp, °F	Carbon
0	1445	4649.46	1.1	105 105	3	262	53
5	1450	4654.5	1.1	108 108	3	258	52
10	1455	4659.25	1.1	108 107	3	258	54
15	1500	4663.6	1.1	106 106	3	259	54
20	1505	4668.54	1.1	108 108	3	260	54
Post test LE 5" @ 1/min = 0.00 l							
0	1512	4669.76	1.1	106 106	2	261	60
5	1517	4674.0	1.1	107 107	2	260	58
10	1522	4678.9	1.1	107 106	2	262	56
15	1527	4684.3	1.1	108 107	2	261	60
20	1532	4688.17	1.1	107 106	2	262	60

Nitrogen purge/activated carbon packing in sample holding container: \_\_\_\_\_

$$V_{std} = V_m (\text{liters}) \times Y \times 17.647 \times \frac{P_b (\text{in. Hg})}{T_m (^\circ \text{R})}$$

C-0031-2E L1803694-26 T<sub>10</sub> #1 = 19.08 l,  
 T<sub>m</sub> = 107

C-0031-2F L1803694-60 T<sub>10</sub> #35 = 18.41 l  
 T<sub>m</sub> = 107



**EPA METHOD 30  
VOLATILE ORGANIC SAMPLING TRAIN (VOST) SAMPLING DATA**

Company: AK Steel  
 Date: 9/8/16  
 Time: 1548-1608 / 1616-1636  
 Meter #: VB-2  
 Barometric Pressure, in.Hg: 30.00  
 Ambient Temperature, °F: \_\_\_\_\_

City: Middlebush OH  
 Location: Combustion Stack  
 Run #: 3A / 3B  
 Y-Factor: 1.085  
 Operator: AKS  
 Purge Time: \_\_\_\_\_

Vacuum Leak Check Data

	Initial, in.Hg	Final, in.Hg	Time, min.	
Pre-test:	<u>25</u>	<u>25</u>	<u>1</u>	<u>0.00 l.</u>
Post-test:	<u>25</u>	<u>25</u>	<u>1</u>	<u>0.00 l.</u>

Sample Time (min)	Clock Time, (24-hr)	Meter Volume, (liter)	Rotameter Setting	Dry Gas Meter Temp., (°F)		Vacuum, (in.Hg)	Probe Temp, °F	
0	1548	4689.81	1.1	105	105	2	275	63
5	1553	4693.4	1.1	107	105	2	261	62
10	1558	4698.4	1.1	108	106	2	267	58
15	1603	4703.3	1.1	108	108	2	258	60
20	1608	4707.90	1.1	107	106	2	256	62
Per for 5" @ 1/min = 0.00 l								
0	1616	4708.05	1.1	109	108	2	259	60
5	1621	4712.75	1.1	109	108	2	257	62
10	1626	4717.5	1.1	110	107	2	257	56
15	1631	4722.1	1.1	110	110	2	258	57
20	1636	4726.90	1.1	108	109	2	259	53
Per for 5" @ 1/min = 0.00 l								

Nitrogen purge/activated carbon packing in sample holding container: \_\_\_\_\_

$$V_{std} = V_m (\text{liters}) \times Y \times 17.647 \times \frac{P_b (\text{in. Hg})}{T_m (^\circ \text{R})}$$

C-0031-3A L1803694-51  $T_{m10} \#26 = 18.03^\circ \text{C}, T_m = 107$

C-0031-3B L1803694-49  $T_{m10} \#24 = 18.85^\circ \text{C}, T_m = 109$

**EPA METHOD 30  
VOLATILE ORGANIC SAMPLING TRAIN (VOST) SAMPLING DATA**

Company: AK SteelCity: Middlebarn, OHDate: 9/8/16Location: Combustion StackTime: 1647-1707 / 1715-1735Run #: 3C/3DMeter #: VB-2Y-Factor: 1.085Barometric Pressure, in.Hg: 30.0Operator: DKR

Ambient Temperature, °F: \_\_\_\_\_

Purge Time: \_\_\_\_\_

Vacuum Leak Check Data

	Initial, in.Hg	Final, in.Hg	Time, min.	
Pre-test:	<u>25</u>	<u>25</u>	<u>1</u>	<u>0.00 L</u>
Post-test:	<u>24</u>	<u>24</u>	<u>1</u>	<u>0.00 L</u>

	Sample Time (min)	Clock Time, (24-hr)	Meter Volume, (liter)	Rotameter Setting	Dry Gas Meter Temp., (°F)		Vacuum, (in.Hg)	Probe Temp, °F	Condenser
20	0	1647	4727.28	1.1	110	110	4	269	56
	5	1652	4732.4	1.1	110	109	4	260	58
	10	1657	4737.4	1.1	110	110	4	266	59
	15	1702	4742.5	1.1	110	109	4	266	60
40	20	1707	4747.67	1.1	110	109	4	258	60
		Post test	6" @ 1/min = 0.00 l						
40	0	1715	4748.05	1.1	110	109	2	260	52
	5	1720	4753.0	1.1	110	109	2	258	51
	10	1725	4757.7	1.1	109	108	2	258	53
	15	1730	4762.5	1.1	110	110	2	257	55
60	20	1735	4767.50	1.1	110	109	2	261	57
		Post test	LC = 6" @ 1/min = 0.00 l						

Nitrogen purge/activated carbon packing in sample holding container: \_\_\_\_\_

$$V_{std} = V_m (\text{liters}) \times Y \times 17.647 \times \frac{P_b (\text{in. Hg})}{T_m (^\circ \text{R})}$$

C-0031-3C L1803694-59 Tribo # 34 =  
20.39 L, T<sub>m</sub> = 110

C-0031-3D L1803694-39 Tribo # 14 =  
19.45 L, T<sub>m</sub> = 109

**EPA METHOD 30  
VOLATILE ORGANIC SAMPLING TRAIN (VOST) SAMPLING DATA**

Company: AK Steel  
 Date: 9/8/16  
 Time: <sup>3E</sup> 1744-1804 / <sup>3F</sup> 1811-1831  
 Meter #: VB-2  
 Barometric Pressure, in.Hg: 30.00  
 Ambient Temperature, °F: \_\_\_\_\_

City: Middleburg, OH  
 Location: Carbon Steel  
 Run #: 3E / 3F  
 Y-Factor: 1.085  
 Operator: WJL  
 Purge Time: \_\_\_\_\_

Vacuum Leak Check Data

	Initial, in.Hg	Final, in.Hg	Time, min.	
Pre-test:	<u>25</u>	<u>25</u>	<u>1</u>	<u>0.00 L</u>
Post-test:	<u>24</u>	<u>24</u>	<u>1</u>	<u>0.00 L</u>

Sample Time (min)	Clock Time, (24-hr)	Meter Volume, (liter)	Rotameter Setting	Dry Gas Meter Temp., (°F)	Vacuum, (in.Hg)	Probe Temp, °F	Conduct
0	1744	4767.25	1.1	107 107	2	260	50
5	1749	4772.7	1.1	107 107	2	260	51
10	1754	4777.75	1.1	107 106	2	260	51
15	1759	4782.6	1.1	106 106	2	258	53
20	1804	4787.27	1.1	106 105	2	262	53
Post test leak check = 5" @ 1/min = 0.00 L							
0	1811	4787.73	1.1	103 103	4	260	49
5	1816	4793.05	1.1	104 103	4	261	51
10	1821	4797.7	1.1	104 104	4	260	50
15	1826	4802.6	1.1	104 104	4	260	53
20	1831	4807.04	1.1	103 103	4	257	52
Post test LC = 5" @ 1/min = 0.00 L							

Nitrogen purge/activated carbon packing in sample holding container: \_\_\_\_\_

$$V_{std} = V_m (\text{liters}) \times Y \times 17.647 \times \frac{P_b (\text{in. Hg})}{T_m (^\circ \text{R})}$$

C-0031-3E L 1803694-31 Tris #6 =  
19.52 L, T<sub>m</sub> = 106

C-0031-3F L 1803694-56 Tris #31 =  
19.31 L, T<sub>m</sub> = 104

**EPA METHOD 30  
VOLATILE ORGANIC SAMPLING TRAIN (VOST) SAMPLING DATA**

Company: AK Steel  
 Date: 9/15/16  
 Time: <sup>4A</sup> 0945-1005 / <sup>4B</sup> 1020-1040  
 Meter #: Vβ-2  
 Barometric Pressure, in.Hg: 30.24  
 Ambient Temperature, °F: \_\_\_\_\_

City: Middle town, OH  
 Location: Combustion Stack  
 Run #: C-0031-4A  
 Y-Factor: 1.085  
 Operator: WLL  
 Purge Time: \_\_\_\_\_

Vacuum Leak Check Data

	Initial, in.Hg	Final, in.Hg	Time, min.	
Pre-test:	<u>25</u>	<u>25</u>	<u>1</u>	<u>0.00 L</u>
Post-test:	<u>22</u>	<u>22</u>	<u>1</u>	<u>0.00 L</u>

Sample Time (min)	Clock Time, (24-hr)	Meter Volume, (liter)	Rotameter Setting	Dry Gas Meter Temp., (°F)		Vacuum, (in.Hg)	Probe Temp, °F	Condenser °F
<sup>140</sup> 0	0945	4811.00	1.0 L	68	68	2	252	43
5	0950	4815.30	1.0 L	70	68	2	257	43
<sup>4A</sup> 10	0955	4819.9	1.0 L	71	69	2	259	44
15	1000	4824.8	1.0 L	72	70	2	259	46
20	1005	4829.44	1.0 L	74	71	2	260	43
Post test 5" Hg @ 1 min = 0.00 L								
0	1020	4829.84	1.0 L	74	74	2	258	45
<sup>4B</sup> 5	1025	4834.75	1.0 L	75	75	2	259	47
10	1030	4839.4	1.0 L	76	75	2	266	48
15	1035	4843.9	1.0 L	77	76	2	264	48
20	1040	4848.72	1.0 L	76	76	2	264	47
Post test 5" Hg @ 1 min = 0.00 L								

Nitrogen purge/activated carbon packing in sample holding container: \_\_\_\_\_

$$V_{std} = V_m (\text{liters}) \times Y \times 17.647 \times \frac{P_b (\text{in. Hg})}{T_m (^\circ R)}$$

4A L1826178-2  $T_{1/2} = 18.44^\circ \text{C}, T_m = 70$   
 4B L1826178-5  $T_{1/2} = 18.88^\circ \text{C}, T_m = 75$

**EPA METHOD 30  
VOLATILE ORGANIC SAMPLING TRAIN (VOST) SAMPLING DATA**

Company: AK SteelCity: Milwaukee, WIDate: 9/18/16Location: Combustion SparkTime: 4C 1055-1115 4D 1126-1146Run #: 00031-4C/00031-4DMeter #: 1A2Y-Factor: 1.085Barometric Pressure, in.Hg: 30.24Operator: AKS

Ambient Temperature, °F: \_\_\_\_\_

Purge Time: \_\_\_\_\_

Vacuum Leak Check Data

	Initial, in.Hg	Final, in.Hg	Time, min.	
Pre-test:	<u>25</u>	<u>25</u>	<u>1</u>	<u>0.00 l</u>
Post-test:	<u>25</u>	<u>25</u>	<u>1</u>	<u>0.00 l</u>

	Sample Time (min)	Clock Time, (24-hr)	Meter Volume, (liter)	Rotameter Setting	Dry Gas Meter Temp., (°F)	Vacuum, (in.Hg)	Probe Temp, °F	Condensed °F
220	0	1055	4849.15	1.0 l	75 75	2	260	48
4C	5	1100	4854.0	1.0 l	76 77	2	256	49
	10	1105	4858.7	1.0 l	77 78	2	256	50
	15	1110	4863.4	1.0 l	78 78	2	257	50
	20	1115	4868.26	1.0 l	79 77	2	258	48
	Purge for 5" R/min = 0.00 l							
	0	1126	4868.67	1.0	78 78	3	257	48
4D	5	1131	4873.5	1.0	79 79	3	258	48
	10	1136	4878.1	1.0	80 79	3	258	48
	15	1141	4882.8	1.0	82 80	3	258	47
	20	1146	4887.65	1.0	83 80	3	261	49
	Purge for 5" R/min = 0.00 l							

Nitrogen purge/activated carbon packing in sample holding container: \_\_\_\_\_

$$V_{std} = V_m (\text{liters}) \times Y \times 17.647 \times \frac{P_b (\text{in.Hg})}{T_m (^\circ R)}$$

$$4C = 21826178 - 10$$

$$4D = 21826178 - 11$$

$$T_{m10} \pm 10 = 19.11 \text{ l}, T_m = 77$$

$$T_{m11} \pm 11 = 18.98 \text{ l}, T_m = 80$$

**EPA METHOD 30  
VOLATILE ORGANIC SAMPLING TRAIN (VOST) SAMPLING DATA**

Company: AK Steel  
 Date: 9/16/16  
 Time: 1158-1218 / 1228-1248  
 Meter #: VB-2  
 Barometric Pressure, in.Hg: 30.24  
 Ambient Temperature, °F: \_\_\_\_\_

City: Middleburg, OH  
 Location: Combustion Stack  
 Run #: C-0031-4E/4F  
 Y-Factor: \_\_\_\_\_  
 Operator: MM  
 Purge Time: \_\_\_\_\_

Vacuum Leak Check Data

	Initial, in.Hg	Final, in.Hg	Time, min.	
Pre-test:	<u>25</u>	<u>25</u>	<u>1</u>	<u>0.00 L</u>
Post-test:	<u>25</u>	<u>25</u>	<u>1</u>	<u>0.00 L</u>

Sample Time (min)	Clock Time, (24-hr)	Meter Volume, (liter)	Rotameter Setting	Dry Gas Meter Temp., (°F)		Vacuum, (in.Hg)	Probe Temp, °F	Conc. °F
4E	0	4888.816	1.0 L	83	83	2	260	49
	5	4893.15	1.0 L	86	84	2	257	50
	10	4898.10	1.0 L	87	85	2	261	50
	15	4903.05	1.0 L	88	85	2	255	50
	20	4907.63	1.0 L	90	87	2	266	50
	Post Air 5" 1/2 @ 1/min = 0.00 L							
4F	0	4908.42	1.0 L	89	88	2	255	51
	5	4913.0	1.0 L	90	89	2	255	51
	10	4917.9	1.0 L	89	88	2	258	51
	15	4922.5	1.0 L	90	89	2	257	51
	20	4927.34	1.0 L	88	88	2	260	51
	Post Air 5" 1/2 @ 1/min = 0.00 L							

Nitrogen purge/activated carbon packing in sample holding container: \_\_\_\_\_

$$V_{std} = V_m (\text{liters}) \times Y \times 17.647 \times \frac{P_b (\text{in.Hg})}{T_m (^\circ R)}$$

4E = L1826178-6      T<sub>no</sub> #6 = 19.47 L, T<sub>m</sub> = 86  
 4F = L1826178-3      T<sub>no</sub> #3 = 19.0 L, T<sub>m</sub> = 89

## **HYDROGEN CHLORIDE AND HYDROGEN FLUORIDE**

Plant: AK Middleton  
 Sampling Location: Baghouse 3  
 Run Number: 826-1 Date: 8/23/16  
 Pretest Leak Rate: 0.02 cfm @ 10 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: -

Sample Type: HCL/26A Operator: GD  
 Pbar: 29.95 Ps: -1.9  
 CO<sub>2</sub>: CEM O<sub>2</sub>: CEM  
 Probe Length/Type: 3'61 Pitot#: 73-5  
 Stack Diameter: 35.5" K: 2-130  
2.0991

Nozzle ID: 0.213 Thermocouple #: T3-5  
 Assumed Bws: 1.7 Filter #: Untared  
 Meter Box #: 13 Y: 0.989 ΔH@: 1.783  
 Post-Test Leak Rate: 0.02 cfm @ 18 in.Hg.  
 Post-Test Leak Check: Pitot: ✓ Orsat: ND

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	1021-	828.052											
1	330	1025	831.771	3.1	6.1	4.2	94	250	260	58	N.A.	67	67	18
2	640	1032	835.063	3.1	6.1	4.2	99	252	260	56		67	67	18
3	10:00	1045	838.507	3.3	6.5	4.2	101	260	259	57		68	68	18
4	13:22	1113	842.025	3.4	6.7	4.2	104	254	259	58		69	69	18
5	16:38	1129	845.423	3.2	6.3	4.0	104	261	260	59		70	70	18
6	20:01	1143	849.020	3.0	5.8	4.0	112	258	259	59		71	71	18
1	23:10	1204	852.238	3.0	5.9	3.8	112	256	260	57		72	72	18
2	26:29	1214	855.778	3.2	6.3	4.0	109	258	258	61		73	73	17
3	29:52	1234	859.174	3.1	6.0	4.0	120	251	260	62		74	74	18
4	33:15	1256	862.534	2.9	5.6	3.8	121	256	260	62		74	74	17.5
5	36:17	1317	865.717	3.2	6.2	3.9	123	249	259	61		75	75	17.5
6	39:37	1334	869.202	3.1	6.0	4.0	118	256	259	62		75	75	17.5
1														
2														
3	39.62 mins													
4														
5														
6														
1														
2														
3														
4														
5														
6														

$$\Delta V_m = 41.150 \sqrt{\Delta p} = 1.7698 \Delta H = 4.025 T_s = 110$$

$$\Delta p = 3.1333$$

$$T_m = 71$$

✓ E2





## SAMPLE RECOVERY DATA

Plant AK Middletown Run No. P-26-1  
 Date 8/23/16 Sample Box No. 5 Job No. 500740172  
 Sample Location Pushing Bayhouse Stack 1 Filter No. Teflon  
 Train Preparer EZ/GD Sample Head No. 2  
 Sample Recovery Person DA Barometer No. TWC: co-  
 Comments Method 26A Balance No. 2

Front Half

Acetone

Liquid

Container No. NA Level Marked — Sealed —FilterContainer No. Teflon Sealed ✓Description of Filter CleanSamples Stored and Locked NABack Half/MoistureContainer No. H<sub>2</sub>SO<sub>4</sub> ImpingersLiquid Level Marked — Sealed ✓

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	0.1 N H <sub>2</sub> SO <sub>4</sub>	50	706.8	709.4	2.6
2	0.1 N H <sub>2</sub> SO <sub>4</sub>	100	763.9	766.5	2.6
3	0.1 N H <sub>2</sub> SO <sub>4</sub>	100	774.4	773.3	-1.1
4	0.1 N NaOH	100	756.2	754.7	-1.5
5	0.1 N NaOH	100	762.0	762.2	0.2
6	Silica Gel	250g	926.1	936.5	10.4
Total					13.2

Description of Impinger Catch: clear  
 BWS = 1.5%

D<sub>20</sub> = 73.7%

Plant: AK Middletown Sample Type: HCL/M26A Operator: GA Nozzle ID: 0.213 Thermocouple #: T3-4  
 Sampling Location: P. Baghouse 3 Pbar: 29.95 Ps: -1.9 Assumed Bws: 1.7 Filter #: Untared  
 Run Number: P. 26-2 Date: 8-23-16 CO<sub>2</sub>: CEM O<sub>2</sub>: CEM Meter Box #: 13 Y: 0.989 ΔH@: 1.783  
 Pretest Leak Rate: .001 cfm @ 18 in.Hg. Probe Length/Type: 3'61 Pitot#: T3-4 Post-Test Leak Rate: .002 cfm @ 19 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: - Stack Diameter: 35.5" K: 2.0999 Post-Test Leak Check: Pitot: ✓ Orsat: -

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (T's)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.			Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Tm	Outlet	
0	0	1352	870.268												
1	326	1355	873.264	2.8	5.4	2.9	123	250	262	60	N.A.	76	76	76	17.5
2	630	1442	876.855	3.0	5.9	3.0	113	249	258	59		77	77	77	18.0
3	928	1452	880.639	3.0	5.9	3.5	116	251	259	61		77	77	77	18.0
4	1227	1505	884.488	3.0	5.9	3.1	118	253	258	60		78	78	78	18.0
5	1420	1525	887.799	2.9	5.7	3.2	118	253	259	59		78	78	78	18.0
6	1644	1545	891.500	3.0	5.9	3.2	117	250	258	58		79	79	79	18.0
1	1923	1557	895.018	2.9	5.7	2.7	119	251	260	55		80	79	79	18.5
2	2145	1618	898.342	2.9	5.7	2.9	112	255	260	54		80	80	80	18.5
3	2430	1631	901.736	2.8	5.6	2.8	112	258	260	56		80	80	80	18.5
4	2650	1653	905.167	2.8	5.6	2.9	111	261	259	58		80	80	80	18.5
5	2837	1707	908.529	2.8	5.6	2.8	111	255	258	58		79	79	79	18.0
6	3120	1728	912.268	2.8	5.6	2.9	108	261	260	59		78	79	79	18.0
1															
2															
3	31.93	minutes													
4															
5															
6															
1															
2															
3															
4															
5															
6															

$$\Delta V_m = \frac{42.000}{\sqrt{\Delta p}} = \frac{1.7003}{\sqrt{\Delta H}} = \frac{2.997}{T_s} = 115$$

$$T_m = 78.5 \quad 15^\circ \quad 97.8$$

$$AP = 2.8917$$

✓



## SAMPLE RECOVERY DATA

Plant AK Middletown Run No. P-26-2  
 Date 8/23/16 Sample Box No. 4 Job No. 050074.0172  
 Sample Location Pressing Baghouse Filter No. Untard Teflon  
 Train Preparer EZ/GD Sample Head No. 11  
 Sample Recovery Person CJ Barometer No. TUC.com  
 Comments Method 26 Balance No. 4

Front Half

Acetone \_\_\_\_\_ Liquid \_\_\_\_\_  
 Container No. NA Level Marked ✓ Sealed \_\_\_\_\_

Filter

Container No. Teflon Sealed ✓

Description of Filter Clean

Samples Stored and Locked \_\_\_\_\_

Back Half/Moisture

Container No. P26-2 H<sub>2</sub>SO<sub>4</sub> IMPINGERS

Liquid Level Marked ✓ Sealed ✓

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	0.1N H <sub>2</sub> SO <sub>4</sub>	50	686.9	689.9	3.0
2	0.1N H <sub>2</sub> SO <sub>4</sub>	100	766.3	767.5	1.2
3	0.1N H <sub>2</sub> SO <sub>4</sub>	100	740.9	741.1	0.2
4	0.1N NaOH	100	752.8	752.5	-0.3
5	0.1N NaOH	100	771.4	770.0	-1.4
6	Silica Gel	250	932.6	943.3	10.7
Total					13.4

Description of Impinger Catch: clean

Bus = 1.5%

Nozzle ID: 156 Thermocouple #: T3-4  
 Assumed BWS: 1.7 Filter #: UNTAPED  
 Meter Box #: 13 Y: 0.989 ΔH@: 1.783  
 Post-Test Leak Rate: 0.0 cfm @ 10 in.Hg.  
 Post-Test Leak Check: Pitot: ✓ Orsat: —

Sample Type: HCL/26A Operator: GD  
 Pbar: 29.97 Ps: -1.9  
 CO<sub>2</sub>: —  
 Probe Length/Type: 3' 61 Pitot#: T3-4  
 Stack Diameter: 35.5" K: 6106

Plant: AK Middleton  
 Sampling Location: P. Baghouse #3  
 Run Number: 1-26-3 Date: 8/24/16  
 Pretest Leak Rate: 0.0 cfm @ 10 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	10:27	912.702											
1	3:04	10:31	915.527	3.2	1.9	1.9	87	260	260	64	N.A.	73	72	5.0
2	5:52	10:40	918.155	3.0	1.8	1.8	99	258	260	59		76	74	5.0
3	9:24	10:44	920.515	3.0	1.7	1.7	110	256	260	57		77	75	4.5
4	12:57	10:57	923.061	3.3	1.9	1.9	111	267	260	58		78	77	5.0
5	16:14	11:24	925.588	3.3	1.9	1.9	115	261	259	63		79	78	5.0
6	19:52	11:39	928.157	3.1	1.8	1.8	114	255	260	58		80	78	5.0
1	23:30	11:58	930.742	3.1	1.8	1.8	108	257	259	57		79	78	5.0
2	27:03	12:17	933.309	3.2	1.8	1.8	112	260	259	58		78	77	5.0
3	30:37	12:36	936.012	3.3	1.9	1.9	114	257	260	60		77	77	5.0
4	34:07	12:54	938.640	3.0	1.7	1.7	115	261	260	57		77	77	5.0
5	37:30	13:14	941.244	3.1	1.8	1.8	112	259	259	56		78	77	10.0
6	40:59	13:33	943.592	3.0	1.7	1.7	113	257	260	58		78	77	7.0
1	44:21	13:50	946.018	3.3	1.9	1.9	112	258	260	59		78	78	6.5
2	47:45	14:08	948.438	3.2	1.8	1.8	112	262	259	57		77	77	5.5
3	51:18	14:25	951.134	3.3	1.9	1.9	111	257	260	56		78	77	6.5
4	54:51	14:44	954.025	3.2	1.8	1.8	113	259	259	58		78	77	7.0
5	58:01	15:03	956.627	3.2	1.8	1.8	114	259	259	59		78	78	6.0
6														
1														
2														
3														
4														
5														150=98.7
6														

Tm = 77

$$\Delta V_m = 43.925 \sqrt{\Delta p} = 1.7787 \Delta H = 1.82 T_s = 110$$

150 - 3 1647

## SAMPLE RECOVERY DATA

Plant AK Steel Middletown Run No. P-26-3  
 Date 8/24/16 Sample Box No. \_\_\_\_\_ Job No. 050074.0172  
 Sample Location Pressure Baghouse Filter No. \_\_\_\_\_  
 Train Preparer EZ/CD Sample Head No. 6  
 Sample Recovery Person CJ Barometer No. TWC.com  
 Comments M26 Balance No. 2

Front Half

Acetone \_\_\_\_\_ Liquid \_\_\_\_\_  
 Container No. \_\_\_\_\_ Level Marked \_\_\_\_\_ Sealed \_\_\_\_\_

Filter \_\_\_\_\_  
 Container No. \_\_\_\_\_ Sealed \_\_\_\_\_

Description of Filter \_\_\_\_\_

Samples Stored and Locked \_\_\_\_\_

Back Half/Moisture P-26-3  
 Container No. 0.1 N H<sub>2</sub>SO<sub>4</sub>

Liquid Level Marked ✓ Sealed ✓

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	0.1 N H <sub>2</sub> SO <sub>4</sub>	50	687.8	693.1	5.3
2	↓	100	790.6	793.9	3.3
3	↓	100	773.5	773.6	0.1
4	0.1 N NaOH	100	778.6	777.9	-0.7
5	↓	100	763.2	764.0	0.8
6	SG	250	928.8	941.0	12.2
Total					21.0

Description of Impinger Catch: clear BWS = 2.2%

## FIELD DATA SHEET

Plant: AK Middletown Sample Type: HCC/MZGA Operator: GD  
 Sampling Location: 1 Baghouse #3 Pbar: 30.30 Ps: -1.9  
 Run Number: 8-26-4 Date: 8-25-16 CO<sub>2</sub>: CSM O<sub>2</sub>: CSM  
 Pretest Leak Rate: .002 cfm @ 11 in.Hg. Probe Length/Type: 3'61 Pitot#: T3-4  
 Pretest Leak Check: Pitot: ✓ Orsat: — Stack Diameter: 35.5 K: .6106

Nozzle ID: .156 Thermocouple #: T3-4  
 Assumed Bws: 1.7 Filter #: UNTRAPED  
 Meter Box #: 13 Y: 0.989 ΔH@: 1.783  
 Post-Test Leak Rate: .001 cfm @ 9 in.Hg.  
 Post-Test Leak Check: Pitot: ✓ Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature BF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	10:28	958.406											
1	3:30	10:31	961.020	3.2	1.9	1.9	102	248	259	62	N.A.	77	77	5.5
2	6:58	10:42	963.632	3.1	1.8	1.8	106	250	258	59		77	77	5.5
3	10:29	10:54	966.268	3.1	1.8	1.8	112	260	259	57		77	77	5.5
4	13:55	11:23	969.075	3.4	1.9	1.9	120	257	259	58		78	77	6.0
5	17:30	11:34	971.803	3.2	1.8	1.8	126	261	259	60		78	78	6.0
6	21:00	11:58	974.496	3.1	1.7	1.7	123	260	259	57		79	78	6.0
1	24:37	12:03	977.068	3.0	1.7	1.7	119	258	258	56		79	78	5.5
2	28:16	12:32	979.656	2.8	1.6	1.6	115	257	259	57		80	79	7.0
3	31:50	12:38	982.213	2.9	1.7	1.7	117	258	259	58		80	79	7.0
4	35:20	12:57	984.770	3.0	1.7	1.7	118	254	260	59		80	80	7.0
5	38:54	13:19	987.491	3.3	1.9	1.9	116	260	260	57		81	80	8.0
6	42:17	13:35	990.131	3.1	1.8	1.8	118	259	258	58		81	81	8.0
1	45:50	13:50	992.868	3.0	1.7	1.7	123	254	259	59		82	81	7.5
2	49:15	14:28	995.411	3.0	1.7	1.7	122	254	259	60		83	83	7.0
3	52:40	14:52	998.048	3.2	1.8	1.8	123	259	260	57		84	83	7.0
4	55:18	15:06	1000.733	3.2	1.8	1.8	121	263	261	59		84	84	7.0
5		15:09												
6														
1														
2														
3														
4														
5														
6														

$$\Delta V_m = 42.327 \sqrt{\Delta p} = 1.760 \Delta H = 1.77 T_s = 118$$

$$\Delta p = 3.1$$

$$T_m = 80$$

Prox  
Sample

## SAMPLE RECOVERY DATA

Plant AK Steel - Middletown Run No. P-26-4  
 Date 8/25/16 Sample Box No. 50-5 Job No. 52074.0172  
 Sample Location Pushing Bay, house stack 3 Filter No. Refln  
 Train Preparer DA Sample Head No. 2  
 Sample Recovery Person DA Barometer No. 72C.22  
 Comments Method: 26 Balance No. 2

Front Half

Acetone Liquid  
 Container No. NA Level Marked — Sealed —

Filter  
 Container No. Refln Sealed —

Description of Filter clean

Samples Stored and Locked —

Back Half/Moisture

Container No. H2SO4 Impingers

Liquid Level Marked — Sealed —

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	0.1N H <sub>2</sub> SO <sub>4</sub>	500	703.4	709.1	5.7
2	0.1N H <sub>2</sub> SO <sub>4</sub>	100	777.6	775.5	3.9
3	0.1N H <sub>2</sub> SO <sub>4</sub>	100	781.8	782.2	0.4
4	0.1N NaOH	100	754.7	755.9	1.2
5	0.1N NaOH	100	762.2	762.1	-0.1
6	SG	250	936.5	953.8	17.3
Total					28.4

Description of Impinger Catch: clean

✓  
122

EQM

C-26-1

## FIELD DATA SHEET

Plant: PK Steel Sample Type: HCL/HF Operator: NR Nozzle ID: 0.500 Thermocouple #: 76-150  
 Sampling Location: Camden St Pbar: 30.20 Ps: -0.80 Assumed Bws: LO Filter #: 76-150  
 Run Number: C-HCL-1 Date: 7/6/16 CO<sub>2</sub>: 3 O<sub>2</sub>: 15 Meter Box #: 2 Y: 1005 ΔH@: 1607  
 Pretest Leak Rate: 0.00 cfm @ 12 in. Hg. Probe Length/Type: 16.16 Pitot#: 76-150 Post-Test Leak Rate: 0.02 cfm @ 18 in. Hg.  
 Pretest Leak Check: Pitot: 1.5 Orsat: — Stack Diameter: 16.8" K: 53.113 Post-Test Leak Check: Pitot: 1.5 Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	1450	898.160											
1	2.5	1452	849.8	0.04	1.5	1.5	302	266	255	65	14	88	89	4
2	5.0	1455	901.5	.03	1.2	1.2	298	264	262	65		88	89	4
3	7.5	1457	903.2	.04	1.5	1.5	305	264	265	62		88	89	3
4	10	1500	904.9	.04	1.5	1.5	300	264	266	58		88	89	3
5	12.5	1502	906.6	.04	1.5	1.5	311	264	264	57		89	93	4
6	15	1505	906.3	.04	1.5	1.5	304	264	264	57		90	89	4
7	17.5	1517	910.1	.04	1.5	1.5	300	264	264	57		89	89	5
8	20	1530	911.8	.04	1.5	1.5	291	264	263	58		89	89	5
9	22.5	1532	913.6	.04	1.5	1.5	292	264	264	58		90	89	5
10	25	1525	915.4	.04	1.5	1.5	300	264	262	59		90	89	5
11	27.5	1527	917.2	.03	1.2	1.2	292	263	264	60		91	89	5
12	30	1530	918.9	.04	1.5	1.5	308	266	260	61		93	89	5
1	32.5	1535	920.6	.04	1.5	1.5	306	263	265	64		94	90	7
2	35	1537	922.3	.04	1.5	1.5	306	265	269	64		91	90	10
3	37.5	1540	924.1	.04	1.5	1.5	280	262	263	56		92	90	10
4	40	1542	925.8	.04	1.5	1.5	265	264	263	56		92	90	10
5	42.5	1545	927.5	.03	1.2	1.2	285	265	265	55		93	90	10
6	45	1547	929.2	.04	1.5	1.5	299	262	262	55		93	90	11
7	47.5	1550	930.9	.03	1.1	1.1	314	265	264	56		93	90	13
8	50	1553	932.5	.04	1.5	1.5	307	264	263	57		93	90	14
9	52.5	1555	934.2	.04	1.5	1.5	311	263	265	57		93	90	15
10	55	1558	935.9	.04	1.5	1.5	309	263	263	58		93	90	15
11	57.5	1600	937.5	.04	1.5	1.5	314	264	264	59		94	90	17
12	60	1602	939.057	.04	1.5	1.5	310	264	263	59		94	90	17

$$\Delta V_m = 40.897 \sqrt{\Delta p} = 19.55 \quad \Delta H = 1.445 \quad T_s = 300$$

$$T_m = 90$$

$$150 = 98.0$$

$$\Delta V_m = 0.083$$



## SAMPLE RECOVERY DATA

Plant Aksteel Middletown Run No. 26 C-HET-1  
 Date 9/6/16 Sample Box No. 3B-5 Job No. 5W74-0172  
 Sample Location Combustion Stack Filter No. Teflon  
 Train Preparer DA Sample Head No. 54-9  
 Sample Recovery Person CS/RK Barometer No. 72C-07  
 Comments M26 Balance No. 2

Front Half

Acetone Liquid  
 Container No. N/A Level Marked N/A Sealed N/A

Filter  
 Container No. N/A Sealed N/A

Description of Filter N/A

Samples Stored and Locked N/A

Back Half/Moisture

Container No. C-HCI-1 H<sub>2</sub>SO<sub>4</sub>

Liquid Level Marked / Sealed /

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	0.1N H <sub>2</sub> SO <sub>4</sub>	50	710.2	762.0	51.8
2	0.1N H <sub>2</sub> SO <sub>4</sub>	100	782.0	809.9	27.9
3	0.1N H <sub>2</sub> SO <sub>4</sub>	100	953.8	772.4	4.6
4	0.1N NaOH	100	755.9	755.0	-0.9
5	0.1N NaOH	100	762.1	772.5	10.4
6	SW	250	953.8	966.1	12.3
Total					106.1

Description of Impinger Catch: yellow fruit

BWS = 11.1-1

KMP

## FIELD DATA SHEET

Plant: AK Middletown Sample Type: HCL/26A Operator: NP Nozzle ID: .500 Thermocouple #: 76-05P

Sampling Location: Combustion Stack Pbar: 30.00 Ps: -20 Assumed Bws: 10 Filter #: untared QZ

Run Number: C26A-2 Date: 9-8-66 CO<sub>2</sub>: 3 O<sub>2</sub>: 15 Meter Box #: 2 Y: 1005 ΔH@: 1.637

Pretest Leak Rate: .001 cfm @ 10 in.Hg. Probe Length/Type: 6' 6L Pitot#: 76-15P Post-Test Leak Rate: .001 cfm @ 10 in.Hg.

Pretest Leak Check: Pitot: ✓ Orsat: - Stack Diameter: 168" K: 53.113 Post-Test Leak Check: Pitot: ✓ Orsat: -

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	1008	199.274											
1	2.5	1010	200.9	.04	1.4	1.4	324	260	260	65	NA	70	70	3
2	5	1013	202.7	.04	1.4	1.4	312	265	264	65		75	77	3
3	7.5	1015	204.4	.04	1.4	1.4	321	263	266	65		73	73	3
4	10	1018	206.2	.04	1.4	1.4	322	263	263	65		73	72	3
5	12.5	1020	207.9	.04	1.5	1.5	319	265	266	64		74	73	3
6	15	1023	209.7	.04	1.5	1.5	323	262	265	64		75	73	3
7	17.5	1025	211.4	.04	1.5	1.5	330	263	261	64		76	73	3
8	20	1028	213.2	.04	1.5	1.5	344	265	264	66		77	74	3
9	22.5	1030	214.8	.04	1.4	1.4	387	263	264	65		78	74	3
10	25	1033	216.5	.04	1.3	1.3	340	264	263	64		79	74	3
11	27.5	1035	218.2	.04	1.3	1.3	343	262	264	59		81	75	3
12	30	1038	219.5	.04	1.3	1.3	346	265	264	58		82	75	3
1	32.5	1040	221.6	.04	1.3	1.3	347	265	264	58		82	75	3
2	35	1043	223.2	.04	1.3	1.3	347	264	264	58		82	75	3
3	37.5	1045	224.9	.04	1.4	1.4	367	265	264	57		84	77	3
4	40	1048	226.5	.04	1.4	1.4	368	265	264	57		85	77	3
5	42.5	1050	228.4	.04	1.4	1.4	369	265	264	57		86	78	3
6	45	1053	230.1	.04	1.4	1.4	370	265	264	57		86	78	3
7	47.5	1055	231.9	.04	1.4	1.4	372	264	265	58		86	79	3
8	50	1058	233.5	.04	1.4	1.4	371	264	264	58		86	79	3
9	52.5	1100	235.3	.04	1.4	1.4	370	265	265	54		87	79	3
10	55	1103	237.2	.04	1.4	1.4	368	265	265	54		87	80	3
11	57.5	1105	239.0	.04	1.4	1.4	372	264	265	54		87	80	3
12	60	1108	240.436	.04	1.4	1.4	371	265	264	60	✓	88	81	3

$$\Delta V_m = 41.62 \quad \sqrt{\Delta p} = .2 \quad \Delta H = 1.4 \quad T_s = 361$$

Ave 0.04

$$T_m = 78$$

NP

## SAMPLE RECOVERY DATA

Plant AK Steel Middletown Run No. C-26-2  
 Date 9/8/16 Sample Box No. SB-5 Job No. 50074.0172  
 Sample Location Combustion Stack Filter No. Quartz  
 Train Preparer CS Sample Head No. 9  
 Sample Recovery Person DK Barometer No. TWC  
 Comments Method 26A Balance No. 2

## Front Half

Acetone NA Liquid NA  
 Container No. NA Level Marked NA Sealed NA

## Filter

Container No. NA Sealed NA

Description of Filter NA

Samples Stored and Locked NA

## Back Half/Moisture

Container No. 0.1N H<sub>2</sub>SO<sub>4</sub> Imps

Liquid Level Marked NA Sealed NA

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	H <sub>2</sub> SO <sub>4</sub>	50	708.3	756.3	48.0
2	H <sub>2</sub> SO <sub>4</sub>	100	786.1	827.7	41.6
3	H <sub>2</sub> SO <sub>4</sub>	100	757.7	767.2	9.5
4	H <sub>2</sub> O	100	755.0	772.8	17.8
5	H <sub>2</sub> O	100	772.5	754.5	-18.0
6	SB	250	966.1	974.8	8.7
Total					107.6

Description of Impinger Catch: Clear

Loss = 11.0%  
 Rec = 102.0%

UMP

Plant: AK Middleton Sample Type: HCL Operator: NP Nozzle ID: 500 Thermocouple #: TE-15P  
 Sampling Location: Combustion Stage Pbar: 30.00 Psi: -80 Assumed Bws: 10 Filter #: Untared Q2  
 Run Number: C-26A-3 Date: 9-8-66 CO<sub>2</sub>: 15 Meter Box #: 2 Y: 1.005 ΔH@: 1.657  
 Pretest Leak Rate: .001 cfm @ 10 in.Hg. Post-Test Leak Rate: .001 cfm @ 10 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	1155	241.600											
1	2.5	1157	243.2	.04	1.5	1.5	326	250	264	65		79	80	3
2	5	1200	245.1	.04	1.4	1.4	374	264	270	65		80	80	3
3	7.5	1202	246.9	.04	1.4	1.4	375	265	268	65		79	80	3
4	10	1205	248.7	.04	1.4	1.4	376	264	265	65		80	80	3
5	12.5	1207	250.6	.04	1.4	1.4	379	264	267	57		82	80	3
6	15	1210	252.3	.04	1.4	1.4	380	264	267	57		82	80	3
7	17.5	1212	254.7	.04	1.4	1.4	380	265	268	57		83	80	3
8	20	1215	256.3	.04	1.4	1.4	381	264	264	56		83	81	3
9	22.5	1217	257.6	.04	1.4	1.4	381	262	263	58		87	81	3
10	25	1220	259.4	.04	1.4	1.4	381	263	263	58		87	81	3
11	27.5	1222	261.1	.04	1.4	1.4	382	261	263	58		88	81	3
12	30	1225	262.9	.04	1.4	1.4	382	265	264	59		88	81	3
1	32.5	1227	264.7	.04	1.4	1.4	383	265	263	58		88	81	3
2	35	1230	266.4	.04	1.4	1.4	395	262	263	62		91	83	3
3	37.5	1232	268.2	.04	1.4	1.4	392	262	264	62		91	83	3
4	40	1235	270.3	.04	1.4	1.4	391	263	264	63		91	83	3
5	42.5	1237	271.7	.04	1.4	1.4	390	263	264	63		92	83	3
6	45	1240	273.4	.04	1.4	1.4	389	264	264	63		92	83	3
7	47.5	1242	275.4	.04	1.4	1.4	395	265	266	65		92	84	3
8	50	1245	277.0	.04	1.4	1.4	377	264	264	65		93	84	3
9	52.5	1247	278.8	.04	1.4	1.4	373	264	264	65		93	84	3
10	55	1250	280.5	.04	1.4	1.4	381	263	264	63		93	85	3
11	57.5	1252	282.3	.04	1.4	1.4	382	264	264	63		94	85	3
12	60	1255	284.046	.04	1.4	1.4	379	264	264	61		94	85	3

AVM =  $\frac{42.446}{\sqrt{\Delta p}} = \frac{0.27}{\sqrt{\Delta p}}$   $\frac{\Delta H}{T_s} = \frac{1.4}{386}$   $\frac{\Delta H}{T_s} = \frac{1.4}{380}$   $\frac{\Delta H}{T_s} = \frac{1.4}{380}$   
 ARE  $\frac{1.4}{380} = 0.004$

## SAMPLE RECOVERY DATA

Plant Ak steel Middle town Run No. C-26-3  
 Date 9/8/16 Sample Box No. 521 Job No. 50074.0172  
 Sample Location Combustion Filter No. Quartz  
 Train Preparer CJ Sample Head No. 11  
 Sample Recovery Person DA Barometer No. 1WC  
 Comments He1 26 Balance No. 2

Front Half

Acetone Liquid  
 Container No. MA Level Marked \_\_\_\_\_ Sealed \_\_\_\_\_

Filter  
 Container No. MA Sealed \_\_\_\_\_

Description of Filter \_\_\_\_\_

Samples Stored and Locked \_\_\_\_\_

Back Half/Moisture

Container No. H<sub>2</sub>SO<sub>4</sub> Imp.

Liquid Level Marked \_\_\_\_\_ Sealed \_\_\_\_\_

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	0.1N H <sub>2</sub> SO <sub>4</sub>	50	693.2	751.9	58.7
2	↓	100	800.0	834.4	34.4
3	↓	100	773.2	779.2	6.0
4	0.1N NaOH	100	777.9	778.5	0.6
5	↓	100	764.0	764.4	0.4
6	SG	250	941.0	950.8	9.8
Total					109.9

Description of Impinger Catch: Clear

Bws = 11.1%

Z<sub>80</sub> = 105.1

Exp

## **HYDROGEN CYANIDE**

## FIELD DATA SHEET

Plant: AK Middleton Sample Type: DTM 29 Operator: EL Nozzle ID: 0.145 Thermocouple #: T3-2  
 Sampling Location: Baghouse 2 Pbar: 2.95 Ps: -1.8 Assumed Bws: 2.5 Filter #: Q2-416  
 Run Number: P-HW-1 Date: 8/23/16 CO<sub>2</sub>: CEM O<sub>2</sub>: CEM Meter Box #: 5 Y: 0.993 ΔH@: 1.906  
 Pretest Leak Rate: 0.001 cfm @ 15 in.Hg. Probe Length/Type: 3' 6" Pitot#: T3-2  
 Pretest Leak Check: Pitot: √ Orsat: - Stack Diameter: 35.5" K: 1.56

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (T <sub>s</sub> )	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	10:21	700.715											
1	3:41	10:21	704.773	3.8	5.7	5.7	89	263	260	65	N/A	70	69	4.5
2	7:20	10:33	708.095	3.1	4.5	4.5	100	261	258	57		70	70	3
3	10:24	10:45	711.732	3.3	4.9	4.9	101	265	260	58		71	70	3
4	13:48	11:13	715.497	3.4	5.0	5.0	104	256	260	59		72	72	4
5	17:13	11:26	719.494	3.6	5.3	5.3	107	260	259	59		73	72	4
6	20:40	11:33	723.606	3.7	5.4	5.4	111	261	259	59		73	73	4.5
1	23:44	12:49	727.120	3.3	4.8	4.8	114	255	261	60		74	74	3.5
2	27:09	12:53	731.046	3.3	4.8	4.8	111	261	249	60		75	75	3.5
3	30:34	12:57	735.030	3.5	5.1	5.1	111	265	252	59		75	75	4
4														
5														
6														
1														
2														
3														
4														
5														
6														
1														
2														
3														
4														
5														
6														

$$\Delta V_m = 34.315 \sqrt{\Delta p} = 1.8551 \Delta H = 5.06 T_s = 105$$

$$\Delta p = 3.44444$$

$$T_m = 72$$

✓

**SAMPLE RECOVERY DATA**

Plant Ak Steel Middletown Run No. P-HCN-1  
 Date 8/22/16 Sample Box No. #1 Job No. 50074.0172  
 Sample Location Pushing Bayhouse Stack 2 Filter No. QZ-446  
 Train Preparer CJ Sample Head No. 12  
 Sample Recovery Person DA Barometer No. TWC. Co.  
 Comments OTM 29 Balance No. 2

Front Half

Acetone Liquid  
 Container No. NA Level Marked — Sealed —

Filter

Container No. NA Sealed —

Description of Filter clean

Samples Stored and Locked —

Back Half/Moisture

Container No. 2 - 1st 2ND Impingers, 3rd Impinger

Liquid Level Marked — Sealed —

PH  
 13.6  
 13.5  
 13.7

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	6N NaOH	100	779.5	781.4	1.9
2	6N NaOH	100	769.8	772.5	2.7
3	6N NaOH	100	804.6	805.7	1.1
4	SC	250	879.6	887.3	7.7
5			<del>882.6</del>		
6					
Total					13.4

w/cap on  
 ✓

Description of Impinger Catch: Clear

BWS = 1.8%  
 ISO = 90.96%



## FIELD DATA SHEET

Sample Type: OFM 29 Operator: F2  
Pbar: 21.95 Ps: -1.8  
CO<sub>2</sub>: 454 O<sub>2</sub>: 454  
Probe Length/Type: 36L Pitot#: T3-2  
Stack Diameter: 35.5" K: 1.56

Nozzle ID: Q145 Thermocouple #: 13-2  
Assumed Bws: 25 Filter #: QZ-447  
Meter Box #: 5 Y: 0493 AH@: 1906  
Post-Test Leak Rate: 001 cfm @ 9 in.Hg.  
Post-Test Leak Check: Pitot: ✓ Orsat: —

[illegible]

$$\Delta V_m = 32.027 \quad \sqrt{\Delta p} = 1.8037 \quad \Delta H = 4.74 \quad T_s = 118$$

$\Delta p = 3.2625$

$$\underline{Tm} = 80$$



## SAMPLE RECOVERY DATA

Plant AK Steel Middletown Run No. P-HCN-2  
 Date 8/23/16 Sample Box No. 13 Job No. 52074.0172  
 Sample Location Pushing Bayhouse Stack 2 Filter No. CRZ-447  
 Train Preparer CT Sample Head No. 4  
 Sample Recovery Person DA Barometer No. 7WC100  
 Comments OTM 2a-HCN Balance No. 2

Front Half

Acetone \_\_\_\_\_ Liquid \_\_\_\_\_  
 Container No. NA Level Marked \_\_\_\_\_ Sealed \_\_\_\_\_

Filter

Container No. Quartz Sealed ✓

Description of Filter Clean

Samples Stored and Locked ✓

Back Half/Moisture

Container No. 2 1st 2 ND Impingers, 3RD Impinger

Liquid Level Marked ✓ Sealed \_\_\_\_\_

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	6N NaOH	100	796.0	798.7	2.7
2	6N NaOH	100	740.8	743.0	2.2
3	6N NaOH	100	800.4	800.7	0.3
4	SG	250	909.1	915.0	5.9
5					
6					
Total					11.1

Description of Impinger Catch: Clean

BWS = 1.6%

T<sub>20</sub> = 100%

## FIELD DATA SHEET

Plant: AK Middlebrook Sample Type: HGN/OTM 29 Operator: AP  
 Sampling Location: P. Bayhouse #2 Pbar: 24.97 Ps: -1.1  
 Run Number: P-HGN-3 Date: 8-24-16 CO<sub>2</sub>: SEM  
 Pretest Leak Rate: 0.01 cfm @ 9 in.Hg. Probe Length/Type: 3' 1/4 Pitot#: 73-2  
 Pretest Leak Check: Pitot: ✓ Orsat: - Stack Diameter: 3.55" K: 6655 B

Nozzle ID: .156 Thermocouple #: 73-2  
 Assumed Bws: 2.5 Filter #: G2-449  
 Meter Box #: 5 Y: .993 AH@: 1.906  
 Post-Test Leak Rate: .002 cfm @ 8 in.Hg.  
 Post-Test Leak Check: Pitot: ✓ Orsat: -

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	10:37	767.757											
1	3:29	10:38	770.751	3.4	2.2	2.2	80	265	264	65	NA	72	72	1
2	5:48	10:40-10:44	773.505	3.0	1.9	1.9	96	265	265	65		74	73	1
3	9:17	10:54-10:58	775.715	2.7	1.7	1.7	103	266	265	64		75	74	0
4	12:48	11:07-11:11	778.234	3.0	1.9	1.9	106	266	265	64		76	75	1
5	16:18	11:24-11:28	780.544	3.0	1.9	1.9	110	266	265	63		77	76	1
6	19:48	11:39-11:43	782.961	3.1	1.9	1.9	112	265	267	63		78	77	1
1	23:17	11:58-12:01	785.255	2.7	1.7	1.7	105	266	265	62		78	77	1
2	26:48	12:17-12:21	787.620	2.6	1.6	1.6	106	263	266	62		77	77	1
3	30:12	12:36-12:40	790.122	3.3	2.0	2.0	108	269	245	62		78	77	1
4	33:43	12:55-12:59	792.725	3.0	1.9	1.9	112	260	264	62		78	78	1
5	37:15	13:14-13:18	795.370	3.4	2.1	2.1	113	263	264	61		78	78	1
6	40:44	13:33-13:36	798.122	3.3	2.0	2.0	115	256	264	60		79	79	1
1	44:16	13:50-13:54	800.867	3.1	1.9	1.9	117	259	264	60		80	79	1
2														
3	44:27	14:14-14:18												
4														
5														
6														
1														
2														
3														
4														
5														
6														

$$\Delta V_m = 33.110 \sqrt{\Delta p} = 1.743 \Delta H = 1.90 \overline{Ts} = 106$$

$$\overline{T_m} = 77$$

Area = 3.0462

✓

**SAMPLE RECOVERY DATA**

Plant AK Steel - Middletown Run No. P-HCN-3  
 Date 8/24/16 Sample Box No. H30-5 Job No. 52074-0172  
 Sample Location Pushing Bayhouse Stack #2 Filter No. Q2-449  
 Train Preparer CT Sample Head No. 6  
 Sample Recovery Person DA Barometer No. TWC-60m  
 Comments OTM 29 - HCN Balance No. 2

Front Half

Acetone Liquid  
 Container No. MA Level Marked Sealed

Filter  
 Container No. MA Sealed Sealed

Description of Filter clean

Samples Stored and Locked Sealed

Back Half/Moisture

Container No. 2 1st 2ND Impinger, 3RD Impinger

Liquid Level Marked Sealed

pH	Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
				Initial	Final	Net
<u>13.3</u>	1	<u>6N NaOH</u>	<u>100</u>	<u>777.0</u>	<u>781.5</u>	<u>4.5</u>
<u>13.6</u>	2	<u>6N NaOH</u>	<u>100</u>	<u>775.6</u>	<u>779.8</u>	<u>4.2</u>
<u>13.7</u>	3	<u>6N NaOH</u>	<u>100</u>	<u>797.0</u>	<u>794.2</u>	<u>-2.8</u>
	4	<u>SG</u>	<u>250</u>	<u>908.8</u>	<u>916.2</u>	<u>7.4</u>
	5					
	6					
	Total					<u>13.3</u>

Description of Impinger Catch: clear BW = 1.98

250 = 99.1%

Plant: AK Middle town Sample Type: OTM 29 Operator: NP  
 Sampling Location: P. Baghouse 2 Pbar: 30.30 Ps: -1.1  
 Run Number: P-HW-4 Date: 8-25-16 CO<sub>2</sub>:  
 Pretest Leak Rate: .001 cfm @ 10 in.Hg. Probe Length/Type: 3' 6" Pitot#: T3-2  
 Pretest Leak Check: Pitot: ✓ Orsat: — Stack Diameter: 35.5" K: .6558

Nozzle ID: .156 Thermocouple #: T3-2  
 Assumed Bws: 1.5 Filter #: QZ-447  
 Meter Box #: 5 Y: 993 ΔH@: 1.966  
 Post-Test Leak Rate: .001 cfm @ 8 in.Hg.  
 Post-Test Leak Check: Pitot: ✓ Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp. Tm		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	3:32	10:28	801.301											
1	3:33	10:31	803.988	3.3	2.1	2.1	93	265	271	65	NA	79	78	0
2	3:34	10:32	806.581	3.0	1.9	1.9	104	263	262	65		78	78	0
3	10:31	10:34	809.432	3.3	2.0	2.0	109	260	266	64		78	78	0
4	14:01	10:35	811.948	3.0	1.9	1.9	112	265	269	64		78	78	0
5	17:30	10:36	814.372	3.0	1.8	1.8	120	267	265	64		78	78	0
6	20:58	10:37	816.798	3.0	1.8	1.8	125	265	261	63		79	79	0
1	24:28	10:38	819.363	3.1	1.9	1.9	130	263	265	62		79	79	0
2	27:55	10:39	821.876	2.9	1.7	1.7	132	270	260	62		80	79	0
3	31:30	10:40	824.397	3.0	1.8	1.8	135	270	265	62		80	80	0
4	35:03	10:41	827.022	2.7	1.7	1.7	120	265	263	63		81	80	0
5	38:34	10:42	829.675	3.2	1.9	1.9	127	266	267	63		81	80	0
6	42:02	10:43	832.243	3.2	1.9	1.9	130	266	265	64		82	81	0
1	45:32	10:44	834.810	3.0	1.8	1.8	135	264	264	63		83	82	0
2														
3														
4														
5														
6														
1														
2														
3														
4														
5														
6														

$$\Delta V_m = 33.509 \sqrt{\Delta p} = 1.7470 \Delta H = 1.96 \quad T_s = 121$$

$$T_m = 79$$

$$150 = 99.6$$

$$Ave \Delta H = 3.0536$$

✓

## SAMPLE RECOVERY DATA

Plant Ak Steel Middletown Run No. P-HCN-4  
 Date 8/25/16 Sample Box No. 13 Job No. 5074-0172  
 Sample Location ~~AK MS~~ Pressure BH Filter No. Quartz  
 Train Preparer DA Sample Head No. 12  
 Sample Recovery Person CS Barometer No. WC-100  
 Comments Other Method 29-HCN Balance No. 2

Front Half

Acetone Liquid  
 Container No. \_\_\_\_\_ Level Marked \_\_\_\_\_ Sealed \_\_\_\_\_

## Filter

Container No. \_\_\_\_\_ Sealed \_\_\_\_\_

Description of Filter \_\_\_\_\_

Samples Stored and Locked \_\_\_\_\_

Back Half/Moisture

Container No. (2) 1st & 2nd IMPINGERS  
3rd IMPINGER

Liquid Level Marked ✓ Sealed ✓

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	6N NaOH	100	796.0	809.8	13.8
2	6N NaOH	100	740.0	748.9	8.9
3	6N NaOH	100	805.9	797.7	-8.2
4	SG	200	915.0	922.4	7.4
5					
6					
Total					21.9

Description of Impinger Catch: clear

✓ E2 BWS = 3.0%

PH  
 13.0  
 13.2  
 12.9

Sample Type: HCN/OTM 2.9 Operator: RP  
Pbar: \_\_\_\_\_ Ps: \_\_\_\_\_  
CO<sub>2</sub>: \_\_\_\_\_ O<sub>2</sub>: \_\_\_\_\_  
Probe Length/Type: 3' 6" L Pitot#: T3-2  
Stack Diameter: 35.5" K: \_\_\_\_\_

Nozzle ID: 156 Thermocouple #: 13-2  
 Assumed Bws: \_\_\_\_\_ Filter #: \_\_\_\_\_  
 Meter Box #: 11 Y: .993 ΔH@: 1.793  
 Post-Test Leak Rate: .001 cfm @ 10 in.Hg.  
 Post-Test Leak Check: Pitot: \_\_\_\_\_ Orsat: \_\_\_\_\_

[illegible]

$\Delta V_m$	$\sqrt{\Delta p}$	$\overline{\Delta H}$	$\overline{T_s}$
--------------	-------------------	-----------------------	------------------

$$\overline{TT} =$$



## SAMPLE RECOVERY DATA

Plant AK Steel Middletown Run No. P-HCN-FB  
 Date 8/1/16 Sample Box No. 11- Job No. SDU74.0172  
 Sample Location PRESSURE BAGHOUSE Filter No. Quartz  
 Train Preparer DA Sample Head No. 12  
 Sample Recovery Person CJ Barometer No. ML.com  
 Comments 5M 2g - HCN Balance No. 2

Front Half

Acetone \_\_\_\_\_ Liquid \_\_\_\_\_  
 Container No. \_\_\_\_\_ Level Marked \_\_\_\_\_ Sealed \_\_\_\_\_

Filter

Container No. \_\_\_\_\_ Sealed \_\_\_\_\_

Description of Filter \_\_\_\_\_

Samples Stored and Locked \_\_\_\_\_

Back Half/Moisture

Container No. 1<sup>st</sup> & 2<sup>nd</sup> IMPINGER / 3<sup>rd</sup> IMPINGER

Liquid Level Marked ✓ Sealed ✓

	Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
				Initial	Final	Net
pH 13.76 13.85 13.78	1	6N NaOH	100	780.1	780.0	-0.1
	2	6N NaOH	100	781.7	781.7	0.0
	3	6N NaOH	100	804.8	804.7	-0.1
	4	SG	250	887.3	887.8	0.3
	5					
	6					
Total						0.1 ✓

Description of Impinger Catch: clear



Plant: AK Steel Sample Type: Cleaned Operator: ph Nozzle ID: 0.500 Thermocouple #: 75-2  
 Sampling Location: Carbon in Stack Pbar: 30/20 Ps: -0.75" Assumed Bws: 10 Filter #: Q2447  
 Run Number: C-05m29-1 Date: 9/6/16 CO<sub>2</sub>: 3 O<sub>2</sub>: 15 Meter Box #: 3 Y: 1.009 ΔH@: 1.880  
 Prefest Leak Rate: 0.002 cfm @ 12 in.Hg. Probe Length/Type: 6'6" Pitot#: P5-2  
 Prefest Leak Check: Pitot: ± Orsat: — Stack Diameter: 16.8" K: 59.452  
 Post-Test Leak Check: Pitot: 1.1 Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp. Tm		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	1450	916.214											
1	2.5	1452	918.2	0.04	1.7	1.7	296	248	254	68		94	93	1
2	5.0	1455	920.0	0.04	1.8	1.8	290	249	253	67		92	92	1
3	7.5	1457	922.0	0.04	1.8	1.8	270	245	251	60		92	92	1
4	10.0	1500	923.6	0.04	1.8	1.8	260	240	251	57		93	92	1
5	12.5	1502	925.3	0.035	1.6	1.6	260	248	251	57		95	92	1
6	15.0	1505	927.210	0.040	1.8	1.8	270	249	250	57		96	92	1
7	17.5	1507	929.0	0.040	1.8	1.8	283	252	251	50		94	92	1
8	20.0	1520	930.85	0.040	1.8	1.8	286	249	250	61		94	92	1
9	22.5	1522	932.7	0.040	1.8	1.8	290	249	251	60		95	92	1
10	25.0	1525	934.6	0.040	1.8	1.8	292	250	250	58		96	92	1
11	27.5	1527	936.4	0.035	1.5	1.5	293	247	250	59		97	92	1
12	30.0	1530	938.180	0.050	2.2	2.2	292	250	250	61		97	92	1
1533	32.5	1535	940.1	0.040	1.8	1.8	300	249	249	62		93	92	1
2	35.0	1537	941.7	0.035	1.5	1.5	302	246	249	63		96	92	1
3	37.5	1540	943.4	0.035	1.5	1.5	300	244	249	63		97	92	1
4	40.0	1542	945.2	0.040	1.8	1.8	297	245	250	63		97	92	1
5	42.5	1545	947.1	0.040	1.8	1.8	298	246	251	62		97	92	1
6	45.0	1547	948.9	0.040	1.8	1.8	295	250	250	62		97	92	1
7	47.5	1550	950.570	0.035	1.5	1.5	292	248	250	63		98	92	1
8	50.0													
9	52.5													
10	55.0													
11	57.5													
12	60.0													

$$\Delta V_{tm} = 34.35 \sqrt{\Delta p} = 0.1978 \quad \Delta H = 1.74 \quad T_s = 288$$

$$T_m = 93.5$$

$$150 = 98.8$$

L941.2

0.00991

(100)

## SAMPLE RECOVERY DATA

Plant AK Steel Middletown Run No. C-HCN-1  
 Date 9/16/16 Sample Box No. \_\_\_\_\_ Job No. 50074.0172  
 Sample Location Carlisle in tank Filter No. 122 447  
 Train Preparer CS Sample Head No. SH-2  
 Sample Recovery Person CS Barometer No. 1  
 Comments HCN train Balance No. 1

## Front Half

Acetone \_\_\_\_\_ Liquid \_\_\_\_\_  
 Container No. N/A Level Marked \_\_\_\_\_ Sealed \_\_\_\_\_

## Filter

Container No. N/A Sealed \_\_\_\_\_

Description of Filter \_\_\_\_\_

Samples Stored and Locked \_\_\_\_\_

## Back Half/Moisture

Container No. 1st & 2nd IMPINGER / 3rd IMPINGER

Liquid Level Marked \_\_\_\_\_ Sealed \_\_\_\_\_

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	6N NaOH	100	776.6	776.7	30.1
2	↓	↓	791.3	802.8	11.5
3	↓	↓	796.8	808.7	12.1
4	SG	250	922.4	929.9	7.5
5					
6					
Total					61.2

Description of Impinger Catch: 1st imp yellowish, 2 & 3 are clear

BWS = 7.9%



Plant: AK MiddletonSample Type: HCVOperator: FEZPbar: 30.00 Ps: -0.98Sampling Location: Combustion StackRun Number: CS-HCV-2 Date: 9/8/16Pretest Leak Rate: 0.23 cfm @ 15 in.Hg.Pretest Leak Check: Pitot: ✓ Orsat: —CO<sub>2</sub>: CEMProbe Length/Type: 66 Pitot#: 75-2Stack Diameter: 68" K: 51.66Nozzle ID: 0483Thermocouple #: T5-2Assumed Bws: 10 Filter #: 4462 Q2Meter Box #: 3 Y: 1.009 ΔH@: 1.890Post-Test Leak Rate: 0.21 cfm @ 10 in.Hg.Post-Test Leak Check: Pitot: ✓ Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp. Tm		Pump Vacuum (in. Hg)
					Desired	Actual	Probe	Filter			Inlet	Outlet	
0	0	1008	107.1444										
1	2.5	1010	109.6	0.07	2.5	2.5	251	250	65	N/A	74	73	2
2	5	1013	111.5	0.06	2.2	2.2	248	255	63		74	73	2
3	7.5	1015	113.6	0.07	2.5	2.5	248	253	59		75	74	2
4	10	1018	115.7	0.07	2.5	2.5	250	252	58		77	74	2
5	12.5	1020	117.3	0.04	1.4	1.4	250	252	59		74	75	2
6	15	1023	118.8	0.04	1.4	1.4	251	250	59		80	75	1
7	17.5	1025	120.3	0.04	1.3	1.3	253	250	59		80	75	1
8	20	1028	121.6	0.03	0.98	0.98	253	250	60		81	76	1
9	22.5	1030	123.0	0.03	0.98	0.98	251	250	61		82	76	1
10	25	1033	124.3	0.03	0.98	0.98	250	250	61		82	77	1
11	27.5	1035	125.6	0.03	0.98	0.98	250	250	61		83	77	1
12	30	1038	126.9	0.03	0.98	0.98	249	250	61		83	78	1
1	32.5	1040	128.5	0.04	1.4	1.4	250	250	59		84	78	1
2	35	1043	129.9	0.03	1.0	1.0	251	250	55		85	78	1
3	37.5	1045	131.2	0.03	1.0	1.0	251	250	52		86	78	1
4	40	1048	132.6	0.03	1.0	1.0	250	249	51		86	79	1
5	42.5	1050	133.9	0.03	1.0	1.0	250	251	50		87	80	1
6	45	1053	135.3	0.03	1.0	1.0	250	250	50		87	80	1
7	47.5	1055	136.7	0.03	1.0	1.0	251	250	50		87	81	1
8	50	1058	138.0	0.03	1.0	1.0	249	250	50		88	81	1
9	52.5	1100	139.4	0.03	1.0	1.0	249	250	50		88	81	1
10	55	1103	140.7	0.03	1.0	1.0	250	250	50		89	82	1
11	57.5	1105	141.7	0.02	0.67	0.67	250	250	51		89	82	1
12	60	1108	142.425	0.02	0.67	0.67	249	251	52		89	83	1

$$\Delta V_m = 34.981 \sqrt{\Delta p} = 0.1894 \Delta H = 1.27 T_s = 360$$

$$\Delta p = 0.0371$$

$$T_m = 80$$

## SAMPLE RECOVERY DATA

Plant AK steel Run No. C-HCN 2  
 Date 9/8/16 Sample Box No. - Job No. 50074-0172  
 Sample Location Combustion Stack Filter No. Quartz  
 Train Preparer OS/PK Sample Head No. 6  
 Sample Recovery Person DA Barometer No. TWC  
 Comments OTM 29 Balance No. 2

Front Half

Acetone Liquid  
 Container No. NA Level Marked - Sealed -

Filter  
 Container No. NA Sealed -

Description of Filter -

Samples Stored and Locked -

Back Half/Moisture

Container No. 1st; 2ND Empty; 3RD Impinger

Liquid Level Marked - Sealed -

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	6N NaOH	100	739.3	816.3	77.0
2	6N NaOH	100	799.8	822.9	23.1
3	6N NaOH	100	796.7	803.6	6.9
4	SG	250	929.8	936.3	6.5
5					
6					
Total					113.5

pH  
 13  
 13.2  
 13.5

Description of Impinger Catch: yellowish - 1st Impinger

hws = 13.32

ISO = 100.2%

(MP)

## FIELD DATA SHEET

Plant: AK Middletown Sample Type: OT-1 29 Operator: EZ Nozzle ID: 0483 Thermocouple #: 75-2  
 Sampling Location: Comb Stack Pbar: 30.00 Ps: -0.93 Assumed Bws: 10 Filter #: untared 32  
 Run Number: 65-46N-3 Date: 9/8/16 CO<sub>2</sub>: CEM O<sub>2</sub>: CEM Meter Box #: 3 Y: 1.009 AH@: 1.890  
 Pretest Leak Rate: 0.002 cfm @ 15 in.Hg. Probe Length/Type: 5' 6" Pitot#: T5-2 Post-Test Leak Rate: 0.001 cfm @ 1 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: - Post-Test Leak Check: Pitot: ✓ Orsat: -

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg.)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	1155	142.800											
1	2.5	1157	144.4	0.04	1.3	1.3	373	249	253	65	N/A	83	82	1
2	5	1200	148.9	0.04	1.3	1.3	375	252	254	62		82	82	1
3	7.5	1202	147.5	0.04	1.3	1.3	377	252	254	60		83	82	1
4	10	1205	149.0	0.04	1.3	1.3	378	250	251	60		84	81	1
5	12.5	1207	150.5	0.04	1.3	1.3	370	249	251	59		85	82	1
6	15	1210	152.0	0.04	1.3	1.3	376	251	251	59		86	82	1
1	17.5	1212	153.5	0.04	1.3	1.3	378	248	249	61		87	83	1
2	20	1215	154.8	0.03	1.0	1.0	380	250	249	61		88	83	1
3	22.5	1217	156.2	0.03	1.0	1.0	384	251	250	61		89	83	1
4	25	1220	157.5	0.03	1.0	1.0	386	250	251	62		89	83	1
5	27.5	1222	158.8	0.03	1.0	1.0	388	249	251	63		89	84	1
6	30	1225	160.2	0.03	1.0	1.0	390	250	250	63		90	84	1
1	32.5	1227	161.5	0.03	1.0	1.0	391	249	249	63		90	84	1
2	35	1230	162.6	0.02	0.66	0.66	393	250	249	63		90	84	1
3	37.5	1232	163.8	0.02	0.66	0.66	394	250	251	64		90	85	1
4	40	1235	169.1	0.03	1.0	1.0	397	250	251	65		90	85	1
5	42.5	1237	166.5	0.03	1.0	1.0	397	251	250	65		91	85	1
6	45	1240	167.9	0.03	1.0	1.0	367	260	250	64		92	85	1
1	47.5	1242	169.4	0.02	0.69	0.69	367	250	251	63		92	86	1
2	50	1245	170.6	0.02	0.69	0.69	367	251	250	63		92	86	1
3	52.5	1247	171.7	0.02	0.69	0.69	369	250	250	64		92	86	1
4	55	1250	172.8	0.02	0.69	0.69	370	260	250	64		92	86	1
5	57.5	1252	174.2	0.03	1.0	1.0	372	260	249	64		92	87	1
6	60	1255	175.764	0.04	1.4	1.4	373	260	250	64		93	87	1

$$\Delta V_m = 32.964 \sqrt{\Delta p} = 0.1742 \Delta H = 1.02 \quad T_s = 380$$

$$\Delta p = 0.0308$$

$$T_m = 86$$

NP

## SAMPLE RECOVERY DATA

Plant AK Steel - Middletown Run No. C-HCN-3  
 Date 9/8/16 Sample Box No. HSD-5 Job No. SW74.0172  
 Sample Location Combustion Stack Filter No. Quartz  
 Train Preparer DA Sample Head No. 6  
 Sample Recovery Person DA Barometer No. WC. Co  
 Comments OTM29 - HCN Balance No. 2

Front Half

Acetone Liquid  
 Container No. NA Level Marked \_\_\_\_\_ Sealed \_\_\_\_\_

Filter  
 Container No. NA Sealed \_\_\_\_\_

Description of Filter \_\_\_\_\_

Samples Stored and Locked \_\_\_\_\_

Back Half/Moisture

Container No. 1st & 2nd Imps; 3rd Imp

Liquid Level Marked \_\_\_\_\_ Sealed \_\_\_\_\_

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	6N NaOH	100	777.7	854.9	77.2
2	6N NaOH	100	772.0	792.5	20.5
3	6N NaOH	100	807.7	811.4	3.7
4	SG	250	916.2	921.7	5.5
5					
6					
Total					106.9

Description of Impinger Catch: @ Yellowish 1st Imps =

BWS = 13.5%

TSO = 102.8%

WSP

## SAMPLE RECOVERY DATA

Plant Ak Steel Middletown Run No. C-HCN-FB  
 Date 9/8/16 Sample Box No. 13 Job No. 52074-0172  
 Sample Location Combustion Stack Filter No. QV4-12  
 Train Preparer DA Sample Head No. 2  
 Sample Recovery Person DA Barometer No. TWC  
 Comments OTM 29 HCN Balance No. 2

Front Half

Acetone Liquid  
 Container No. NA Level Marked        Sealed       

Filter  
 Container No. NA Sealed       

Description of Filter       

Samples Stored and Locked       

Back Half/Moisture

Container No. 1ST 2ND Imps, 3RD Imp

Liquid Level Marked ✓ Sealed       

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	6N NaOH	100	779.8	779.6	-0.2
2	"	100	791.7	791.5	-0.2
3	"	100	782.9	782.8	-0.1
4	SW	250	936.3	935.8	-0.5
5					
6					
Total					-1.2

pH  
 13.2  
 13.2  
 13.3

Description of Impinger Catch: clean

(Signature)

## **SEMI-VOLATILE ORGANIC HAP**



## FIELD DATA SHEET

pg. 1 of 3

Plant: AK Middleton  
 Sampling Location: Baghouse #3  
 Run Number: P-Carb-1 Date: 9-12-16  
 Pretest Leak Rate: 0.01 cfm @ 10 in.Hg.  
 Pretest Leak Check: Pitot: ☒ Orsat: ☒

Sample Type: D/F/Carb Operator: GD  
 Pbar: 30.20 Ps: -2.0  
 CO<sub>2</sub>: 0.5 O<sub>2</sub>: 20.5  
 Probe Length/Type: 3' G1 Pitot#: 73-1  
 Stack Diameter: 35.5" K: .6096

Nozzle ID: .156 Thermocouple #: 73-1  
 Assumed Bws: 1.8 Filter #: UNTARDED  
 Meter Box #: 13 Y: 0.989 ΔH@: 1.783  
 Post-Test Leak Rate: .001 cfm @ 8 in.Hg.  
 Post-Test Leak Check: Pitot: ☒ Orsat: ☒

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	10:26	358.286											
1	3:11	10:29	360.643	3.2	1.8	1.8	95	262	265	65	64	63	63	5.0
2	6:31	10:45	363.119	3.1	1.8	1.8	99	258	259	60	61	63	63	5.0
3	9:43	11:02	365.476	3.0	1.7	1.7	106	259	259	57	59	63	63	5.0
4	12:57	11:16	367.897	2.9	1.6	1.6	110	258	260	58	59	65	64	5.0
5	16:20	11:34	370.194	2.8	1.6	1.6	112	260	260	59	58	66	65	5.0
6	19:45	11:51	372.582	3.0	1.7	1.7	114	253	253	60	58	67	67	5.0
1	23:00	12:01	374.841	3.0	1.7	1.7	116	258	258	57	59	68	67	5.0
2	26:24	12:21	377.476	3.1	1.7	1.7	113	259	255	57	60	70	69	5.0
3	29:47	12:38	379.943	3.1	1.7	1.7	115	257	261	58	61	71	70	5.5
4	33:05	12:57	382.363	3.0	1.7	1.7	116	259	257	56	59	72	71	5.5
5	36:30	13:16	384.941	3.2	1.8	1.8	114	261	264	57	59	73	72	5.5
6	39:46	13:36	387.317	3.0	1.7	1.7	115	259	265	58	59	74	73	5.5
1	43:06	13:54	389.861	3.1	1.8	1.8	116	262	260	57	58	74	73	5.5
2	46:16	14:13	392.138	2.8	1.6	1.6	118	258	260	60	56	74	74	5.0
3	49:30	14:32	394.518	2.8	1.6	1.6	120	257	257	58	55	74	74	5.0
4	52:46	14:51	396.903	2.9	1.6	1.6	115	252	261	57	53	75	74	5.0
5	56:04	15:10	399.355	3.0	1.7	1.7	119	252	256	59	54	75	75	5.0
6	59:25	15:28	401.855	3.1	1.8	1.8	112	257	256	58	54	75	75	5.5
1	62:53	15:47	404.429	3.1	1.8	1.8	115	254	258	58	56	75	75	5.5
2	66:16	16:05	407.016	3.4	1.9	1.9	117	260	264	59	55	75	75	6.0
3	69:40	16:24	409.623	3.4	1.9	1.9	118	259	260	58	55	75	75	6.0
4	73:04	16:43	412.181	3.2	1.8	1.8	122	261	259	57	53	75	75	6.0
5	76:55	17:02	415.024	3.3	1.8	1.8	124	257	262	58	54	75	75	6.0
6	80:16	17:21	417.702	3.3	1.9	1.9	115	262	259	59	52	75	75	6.0
1	83:35	17:38	420.315	3.4	1.9	1.9	113	262	261	57	53	75	75	6.0

$$\Delta V_m = 62.024 \sqrt{\Delta p} =$$

$$T_s =$$

$$T_m =$$

Plant: Atk Middleboro Sample Type: CARB 428/429 Operator: DA Nozzle ID: 0156 Thermocouple #: T3-1  
 Sampling Location: Boylston Bay Pbar: 30.20 Ps: -1-6 Assumed Bws: 1.8 Filter #: untreated  
 Run Number: 1-CAE8-1 Date: 9/12-13/16 CO<sub>2</sub>: 0.5 O<sub>2</sub>: 20.5 Meter Box #: 13 Y: 0.589 ΔH@: 1.783  
 Pretest Leak Rate: .82 cfm @ 8 in.Hg. Post-Test Leak Rate: .003 cfm @ 8 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: NA Post-Test Leak Check: Pitot: ✓ Orsat: NA

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
	After Leak Check		420.417											
2	86:45	22:26	423.086	3.3	1.9	1.9	90	262	260	69.4	43	69	70	5.5
3	90:00	23:23	425.486	3.1	1.8	1.8	91	260	261	62	43	69	69	6
4	93:20	24:48	428.045	3.1	1.8	1.8	100	256	260	61	44	69	69	6
5	96:45	25:08	430.649	3.1	1.8	1.8	98	240	260	56	44	68	69	6
6	100:05	25:26	433.224	3.1	1.8	1.8	97	241	258	58	42	68	69	6
1	103:30	25:42	435.833	3.1	1.8	1.8	95	240	259	53	42	67	68	6
2	107:00	26:07	438.345	3.2	1.9	1.9	93	236	257	56	42	67	68	6
3	110:30	26:19	441.131	3.2	1.9	1.9	92	241	266	53	43	67	68	6
4	114:00	26:38	442.640	3.2	1.9	1.9	90	245	258	58	43	66	67	6
5	117:30	26:57	446.268	3.1	1.8	1.8	97	234	258	53	43	66	66	6
6	121:00	27:19	448.809	3.1	1.8	1.8	102	237	260	53	45	66	66	6
1	124:15	27:35	451.352	3.1	1.8	1.8	97	243	263	55	49	66	66	6
2	127:30	27:49	453.896	3.2	1.9	1.9	91	242	262	55	49	66	67	6
3	131:00	28:09	456.580	3.2	1.9	1.9	90	261	260	61	57	66	66	6
4	134:15	28:30	459.085	3.2	1.9	1.9	89	241	258	57	52	66	67	6
5	137:30	28:50	461.637	3.2	1.9	1.9	91	234	259	58	53	67	67	6
6	140:45	29:11	464.185	3.2	1.9	1.9	92	238	251	59	54	68	67	6
1	144:00	29:31	466.738	3.2	1.9	1.9	93	235	257	58	54	68	67	6
2	147:15	29:52	469.326	3.2	1.9	1.9	96	239	260	59	54	69	68	6
3	150:30	30:13	471.870	3.1	1.8	1.8	100	233	260	59	55	71	69	6
4	153:45	30:33	474.400	3.1	1.8	1.8	104	231	259	60	56	72	70	6
5	157:00	30:54	476.958	3.1	1.8	1.8	100	238	261	59	56	73	71	6
6	160:15	31:15	479.422	3.1	1.8	1.8	99	237	256	60	57	74	73	6
1	163:30	31:36	481.920	3.1	1.8	1.8	96	237	256	60	57	75	74	6
2	166:45	31:58	484.485	3.1	1.8	1.8	93	245	256	61	57	76	75	6

$$\Delta V_m = C_d \cdot 0.68 \sqrt{\Delta p} = \quad \Delta H = \quad T_s = \quad T_m =$$

## FIELD DATA SHEET

pg 3 of 3

Plant: AK Middleton  
 Sampling Location: P. Bughouse #3  
 Run Number: P-carb-1 Date: 9-13-16  
 Pretest Leak Rate: .001 cfm @ 8 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: -

Sample Type: Carb 428-429 Operator: GD  
 Pbar: 30.15 Ps: -1.9  
 CO<sub>2</sub>: 0.5 O<sub>2</sub>: 20.5  
 Probe Length/Type: 3' 6" Pitot#: 73-1  
 Stack Diameter: 35.5" K: 0.6096

Nozzle ID: .156 Thermocouple #: 73-1  
 Assumed Bws: 1.8 Filter #: Untared  
 Meter Box #: 13 Y: 0.989 ΔH@: 1.783  
 Post-Test Leak Rate: .001 cfm @ 10 in.Hg.  
 Post-Test Leak Check: Pitot: ✓ Orsat: -

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp, °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	166:45	1036	484.681		1.9	1.9	98	260	261	64	59	64	64	6.0
3	169:58	1039	487.130	3.3	1.8	1.8	107	256	256	60	54	67	66	6.0
4	173:15	1042	489.604	3.2	1.8	1.8	113	263	265	58	52	68	67	6.0
5	176:30	1105	492.028	3.2	1.7	1.7	115	261	260	57	51	69	69	6.0
6	179:36	1116	494.514	3.1	1.7	1.7	119	264	259	59	50	71	70	6.0
1	182:50	1133	497.056	3.1	1.8	1.8	120	260	261	58	50	73	71	6.0
2	185:56	1144	499.390	3.3	1.8	1.8	118	260	263	57	49	73	72	6.0
3	189:09	1158	501.804	3.2	1.9	1.9	113	262	257	58	49	73	73	6.0
4	192:26	1217	504.237	3.3										
5														
6														
7														
8														
9														
10														
11														
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27														
28														
29														
30														

$$F_{\text{flow}} \Delta V_m = 145.653 \sqrt{\Delta p} = 1.7691 \quad \Delta H = 1.79 \quad T_s = 106$$

$$\Delta P = 3.1310$$

$$T_m = 70$$

✓



## SAMPLE RECOVERY DATA

Plant AK Middletown Run No. P-CARB-1  
 Date 9/12-9/13/16 Sample Box No. 6 Job No. 50074.0172  
 Sample Location Pushing Baghouse Outlet Filter No. Untreated Quartz  
 Train Preparer NR Sample Head No. 3  
 Sample Recovery Person AK/BF Barometer No. 1  
 Comments CARB Balance No. 1

Front Half

Acetone

Liquid

Container No. P-CARB-1 Level Marked ✓ Sealed ✓FilterContainer No. Untreated P-CARB-1 Sealed ✓Description of Filter lighter whiteSamples Stored and Locked ✓Back Half/MoistureContainer No. NALiquid Level Marked NA Sealed NA

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	—	—	488.2	510.0	21.8
2	H <sub>2</sub> O	100	767.7	762.7	-5.0
3	—	—	689.3	690.0	0.7
4	Silica	250	941.4	973.2	31.8
5					
6					
Total					49.3

Description of Impinger Catch: clear

Plant: AK Middleton  
Sampling Location: P. Baghouse #3  
Run Number: P-Carb-2 Date: 9-13-16  
Pretest Leak Rate: 001 cfm @ 9 in.Hg.  
Pretest Leak Check: Pitot: ☒ Orsat: ☐

Sample Type: Diff Car. 6423429 Operator: GA / DA  
Pbar: 30.15 Ps: -1.8  
CO<sub>2</sub>: 0.5 O<sub>2</sub>: 20.5  
Probe Length/Type: 3' 61 Pitot#: T3-1  
Stack Diameter: 35.5 K: 0.6096

Nozzle ID: 156 Thermocouple #: 73-1  
 Assumed Bws: 1.3 Filter #: UNTARRED  
 Meter Box #: 13 Y: 0.989  $\Delta H @$ : 1.783  
 Post-Test Leak Rate: .001 cfm @ 8 in.Hg.  
 Post-Test Leak Check: Pitot: 1/2 Orsat: ---

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	AH		Stack Temp (T <sub>s</sub> )	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	1339	504.820											
1	3:13	1342	507.174	3.1	1.8	1.8	110	257	253	62	54	74	74	4.0
2	6:27	1433	509.507	2.9	1.6	1.6	118	255	264	60	51	76	73	4.0
3	9:46	1439	512.056	2.9	1.6	1.6	117	259	259	57	50	76	76	4.0
4	13:05	1457	514.388	2.9	1.6	1.6	118	262	262	54	48	76	76	4.0
5	16:24	1524	516.752	2.9	1.6	1.6	121	256	262	55	48	78	78	4.0
6	19:51	1532	519.151	3.0	1.7	1.7	116	261	262	54	49	79	78	4.5
1	23:17	1550	521.646	2.9	1.6	1.6	120	258	259	52	49	79	79	5.0
2	26:30	1605	523.946	3.0	1.7	1.7	123	257	257	53	48	80	79	4.5
3	29:48	1620	526.308	3.0	1.7	1.7	119	260	255	54	49	80	80	5.0
4	33:05	1645	528.483	3.1	1.8	1.8	114	263	257	55	50	80	80	4.5
5	36:23	1657	530.875	3.0	1.7	1.7	120	257	255	57	46	80	80	5.0
6	39:38	1703	533.514	3.0	1.7	1.7	125	254	263	58	45	80	80	5.5
1	42:50	1709	536.012	3.0	1.7	1.7	123	263	256	57	44	80	79	5.0
2	46:13	1721	538.488	2.8	1.6	1.6	116	260	263	58	45	80	79	5.0
3	49:23	1733	541.017	2.8	1.6	1.6	112	263	258	57	44	79	79	5.5
4	53:30	1736	544.228	2.9	1.7	1.7	95	264	266	68	55	70	70	5.5
5	57:00	1749	546.780	2.9	1.7	1.7	95	257	265	64	57	71	71	5
6	60:30	1753	549.273	3.0	1.7	1.7	103	261	264	64	58	73	72	5
1	63:45	1756	551.676	3.0	1.7	1.7	96	258	259	65	60	74	73	5
2	67:15	1759	554.264	2.9	1.7	1.7	97	256	263	59	45	75	74	5
3	70:45	1800	556.843	2.9	1.7	1.7	111	253	260	57	47	76	75	5
4	74:00	1803	559.271	3.0	1.7	1.7	100	257	260	59	51	76	75	5
5	77:30	1806	561.925	3.1	1.8	1.8	105	259	266	61	54	76	76	5
6	80:45	1809	564.466	3.1	1.8	1.8	102	255	250	60	56	76	76	6

$$\Delta V_m = 59,524 \sqrt{\Delta p} \quad \overline{H V} = \quad \overline{T S} =$$
$$\overline{T_m} =$$

## FIELD DATA SHEET

page 2 of 3

Nozzle ID: 01156 Thermocouple #: 73-1  
 Assumed Bws: 18 Filter #: 1111111  
 Meter Box #: 13 Y: 0.989 ΔH@: 1.783  
 Post-Test Leak Rate: .001 cfm @ 7 in.Hg.  
 Post-Test Leak Check: Pitot: ✓ Orsat: —

Sample Type: CAnS 425/429 Operator: DA/60  
 Pbar: 70-15 Ps: -1.8  
 CO<sub>2</sub>: 0.5 O<sub>2</sub>: 20.5  
 Probe Length/Type: 361 Pitot#: 73-1  
 Stack Diameter: 35.5 K: 0.6096

Plant: AL Middle town  
 Sampling Location: Ashby Gas house #3  
 Run Number: 8-CAnS-2 Date: 9-14-16  
 Pretest Leak Rate: 0.002 cfm @ 8 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: NA

Night  
 crew  
 10/20/16

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature BF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
1	84:00	0116	564.466	2.9	1.7	1.7	101	262	255	62	57	77	76	5
2	87:30	0135	569.695	2.9	1.7	1.7	99	259	260	62	58	76	76	5
3	90:45	0145	572.211	3.1	1.8	1.8	101	251	263	63	60	76	76	5
4	94:00	0150	574.627	2.9	1.7	1.7	101	259	251	63	60	77	76	5
5	97:15	0200	577.139	3.0	1.8	1.8	95	257	250	63	62	74	75	5
6	100:30	0208	579.632	3.0	1.8	1.8	95	262	265	63	63	75	75	5
1	103:45	0224	582.092	2.9	1.7	1.7	98	252	267	64	63	75	75	5
2	107:00	0242	584.617	3.0	1.8	1.8	96	263	261	64	64	75	75	5
3	110:15	0259	587.048	3.0	1.8	1.8	98	263	258	59	50	75	75	5
4	113:30	0316	589.479	2.9	1.7	1.7	95	255	255	57	51	74	74	4.5
5	116:45	0333	591.976	3.1	1.8	1.8	92	258	257	59	53	74	74	5
6	120:00	0351	594.366	2.9	1.7	1.7	96	261	261	58	55	74	74	5
1	123:15	0408	596.826	3.0	1.8	1.8	96	265	261	60	56	73	74	5
2	126:30	0425	599.271	3.0	1.8	1.8	94	265	261	60	57	73	73	5
3	129:45	0442	601.655	3.0	1.8	1.8	93	257	255	60	58	73	73	5
4	133:03	0459	604.248	3.1	1.8	1.8	97	252	260	58	51	70	69	5.0
5	136:25	0516	606.702	3.2	1.8	1.8	100	254	264	56	48	71	70	5.5
6	139:39	0533	609.000	3.3	1.9	1.9	108	257	259	58	48	73	72	5.0
1	142:54	0550	611.318	2.9	1.7	1.7	110	254	260	57	47	73	73	5.0
2	146:14	0607	613.716	3.0	1.7	1.7	112	254	258	58	48	74	74	5.0
3	149:34	0624	616.146	2.9	1.6	1.6	118	260	257	59	50	75	74	5.0
4	152:55	0641	618.556	3.0	1.7	1.7	117	263	258	58	49	75	75	5.0
5	155:47	0658	620.500	2.8	1.6	1.6	126	260	256	57	49	77	76	5.0
6	159:07	0715	622.946	3.1	1.7	1.7	125	254	256	56	48	77	77	5.0

565  
 601.748  
 10/20/16

$$\Delta Vm = 117.842 \sqrt{\Delta p} =$$

$$\Delta H =$$

$$Ts =$$

$$Tm =$$

## FIELD DATA SHEET

Plant: AK Middleton  
Sampling Location: P. Baghouse #3  
Run Number: P-Carb-2 Date: 9-14-16  
Pretest Leak Rate: .001 cfm @ 7 in.Hg.  
Pretest Leak Check: Pitot: ☒ Orsat: ☐

Sample Type: b/F ca-c 423/429 Operator: GD  
Pbar: 30.21 Ps: -1.8  
CO<sub>2</sub>: 0.5 O<sub>2</sub>: 20.5  
Probe Length/Type: 3'61 Ptoth#: 73-1  
Stack Diameter: 35.5" K: 0.6096

Nozzle ID: 156 Thermocouple #: 73-1  
 Assumed Bws: 1.8 Filter #: untared  
 Meter Box #: 13 Y: 0.481  $\Delta H @$ : 1.783  
 Post-Test Leak Rate: 0.01 cfm @ 8 in.Hg.  
 Post-Test Leak Check: Pitot: ✓ Orsat: —

[illegible]

$$F_{100} \Delta V_m = 145.058 \sqrt{\Delta p} = 1.7332 \overline{\Delta H} = 1.73 \overline{T_s} = 108$$

$$\sqrt{\Delta p} = 1.7332$$

Tm = 76

Total  
Checks  
\$24

For

## SAMPLE RECOVERY DATA

Plant AK Middletown Run No. P-CARB-2  
 Date 9/14/16 Sample Box No. SR-7 Job No. 052074.0172  
 Sample Location Pushing Baghouse Filter No. NA UNTARED  
 Train Preparer NP Sample Head No. SH-3  
 Sample Recovery Person BF/RK Barometer No. FWC.com  
 Comments CARB Balance No. FB-2

Front Half

Acetone Liquid  
 Container No. P-CARB-2 Level Marked ☒ Sealed ☒

Filter

Container No. P-CARB-2 Sealed ☒

Description of Filter light grey loading

Samples Stored and Locked ☒

Back Half/Moisture

Container No. NA

Liquid Level Marked NA Sealed NA

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	-	-	510.0	537.5	27.5
2	H <sub>2</sub> O	100	761.6	754.6	-7.0
3	-	-	667.6	669.5	1.9
4	Silica Gel	250	923.7	966.8	43.1
5					
6					
Total					65.5

Description of Impinger Catch: clear

✓BF



## FIELD DATA SHEET

Plant: AK Middleton  
Sampling Location: P. Baghouse #3  
Run Number: P-Carb-3 Date: 9/14/16  
Pretest Leak Rate: 001 cfm @ 7 in.Hg.  
Pretest Leak Check: Pitot: ✓ Orsat: -

Sample Type: NE carb 428/429 Operator: GD/DA  
Pbar: 30.21 Ps: -1.9  
CO<sub>2</sub>:            O<sub>2</sub>:             
Probe Length/Type: 3' 61 Pitot#: 73-1  
Stack Diameter: 35.5" K: 0.6096

Nozzle ID: .156 Thermocouple #: 73-1  
 Assumed Bws: 1.8 Filter #: Unafared  
 Meter Box #: 13 Y: 0.989 ΔH@: 1.783  
 Post-Test Leak Rate: 200 cfm @ 7 in.Hg.  
 Post-Test Leak Check: Pitot: ☒ Orsat: ☐

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. of	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	16:35	650.382											
1	3:16	16:38	652.812	3.1	1.8	1.8	113	249	261	60	50	79	79	6.0
2	6:37	16:48	655.151	3.2	1.8	1.8	114	250	261	58	48	80	79	6.5
3	9:57	17:05	657.598	3.1	1.8	1.8	115	251	260	57	49	80	79	7.0
4	13:19	17:25	660.129	3.1	1.8	1.8	118	247	259	58	49	79	79	7.0
5	16:39	17:35	662.818	3.1	1.8	1.8	116	253	261	59	50	80	79	7.0
6	20:15	17:41	665.774	3.2	1.9	1.9	92	263	259	67	57	71	71	8.0
1	23:45	17:51	668.393	3.0	1.8	1.8	94	260	259	59	57	70	71	7.0
2	27:00	18:04	670.878	3.1	1.8	1.8	96	259	259	58	58	70	71	7.0
3	30:15	18:10	673.292	3.0	1.7	1.7	97	258	260	60	58	70	71	7.0
4	32:45	18:26	675.822	3.0	1.7	1.7	102	259	258	60	57	70	71	7.0
5	37:00	18:46	678.278	2.9	1.7	1.7	97	255	259	63	59	70	70	7.0
6	40:15	18:52	680.672	2.9	1.7	1.7	100	257	259	63	58	70	70	7.0
1	43:30	19:09	683.153	2.9	1.7	1.7	98	258	259	63	59	70	70	7.0
2	46:45	19:24	685.560	2.9	1.7	1.7	99	258	259	64	60	70	70	7.0
3	50:00	19:57	688.003	2.9	1.7	1.7	99	260	260	64	60	70	70	7.0
4	53:30	20:16	690.555	2.9	1.7	1.7	100	254	259	65	60	70	70	7.0
5	56:45	20:38	693.006	2.9	1.7	1.7	95	257	257	65	60	70	70	7.0
6	60:00	20:45	695.405	2.9	1.7	1.7	95	261	259	65	61	70	69	7.0
1	63:15	20:58	697.868	2.9	1.7	1.7	97	259	259	65	61	70	70	7.0
2	66:30	21:38	700.200	3.0	1.8	1.8	84	258	260	65	62	70	69	7.0
3	69:45	21:54	702.699	3.0	1.8	1.8	85	258	259	62	53	69	69	7.0
4	73:00	22:26	705.178	3.0	1.8	1.8	85	259	257	61	52	70	69	7.0
5	76:15	22:50	707.662	3.0	1.8	1.8	86	256	260	60	53	70	69	7.0
6	79:30	23:13	710.095	3.0	1.8	1.8	86	257	257	60	54	71	69	7.0

$$\overline{T_{79}} =$$
$$\underline{TS} =$$
$$= \underline{H \nabla}$$
$$\overline{\Delta p} =$$
$$\Delta V_m =$$

1  
2  
3

1000

Nozzle ID: 01/56 Thermocouple #: T3-1  
 Assumed Bws: 1.2 Filter #: untwined  
 Meter Box #: 13 Y: 0.959  $\Delta H @$ : 1.78  $^{\circ}\text{C}$   
 Post-Test Leak Rate: \_\_\_\_\_ cfm @ \_\_\_\_\_ in.Hg.  
 Post-Test Leak Check: Pitot: ☒ Orsat: ☐

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
			710.095											
1	82:45	0419	712.612	3.0	1.8	1.8	84	260	261	59	54	71	70	7.0
2	86:00	0433	714.873	3.0	1.8	1.8	87	259	258	59	53	71	70	7.0
3	89:15	0454	717.352	3.0	1.8	1.8	86	262	258	61	54	71	70	7.0
4	92:30	0508	719.722	2.9	1.7	1.7	87	255	260	60	54	70	70	7.0
5	95:45	0525	722.178	3.1	1.8	1.8	85	258	260	61	56	70	70	7.0
6	99:00	0538	724.555	3.0	1.8	1.8	86	243	261	61	55	70	69	7.0
1	102:16	1037	727.268	2.9	1.7	1.7	94	245	260	63	54	65	65	7.0
2	105:32	1046	729.557	2.9	1.7	1.7	100	248	260	61	52	66	65	7.0
3	108:53	1057	731.959	2.9	1.6	1.6	110	250	263	58	49	66	66	7.0
4	112:11	1131	734.339	3.0	1.7	1.7	108	264	259	57	50	67	67	7.0
5	115:35	1141	736.775	2.8	1.6	1.6	113	259	254	56	50	68	67	7.0
6	118:56	1233	739.180	2.9	1.6	1.6	111	263	262	58	51	69	68	7.0
1	122:15	1244	741.425	2.9	1.6	1.6	112	261	260	59	50	71	70	7.0
2	125:29	1253	743.792	3.2	1.8	1.8	114	258	261	60	49	72	71	7.0
3	128:43	1358	746.108	3.0	1.7	1.7	118	265	258	57	50	73	71	7.0
4	132:01	1307	748.466	3.1	1.8	1.8	112	260	260	58	48	73	72	7.0
5	135:17	1318	750.839	3.1	1.8	1.8	113	264	259	57	48	73	72	7.0
6	138:41	1332	753.328	3.0	1.7	1.7	118	263	259	58	48	74	73	7.0
1	142:03	1344	755.818	3.0	1.7	1.7	115	256	260	57	47	74	73	7.0
2	145:16	1436	758.150	2.9	1.6	1.6	117	254	261	56	47	75	74	7.0
3	148:33	1448	760.643	3.0	1.7	1.7	114	259	258	58	48	76	75	7.0
4	151:57	1504	763.203	3.0	1.7	1.7	119	257	258	59	50	76	76	7.0
5	155:15	1521	765.656	3.2	1.8	1.8	118	259	257	58	49	76	76	7.0
6	158:33	1539	768.145	3.1	1.8	1.8	115	263	261	56	47	77	76	7.0

$$\Delta V_m = 57.872 \sqrt{\Delta p} = \overline{\Delta H} = \overline{T_S} =$$
$$= \mathcal{M}_T$$

Plant: AK Middle town  
Sampling Location: P. Bayhouse # 3  
Run Number: P-Carb-3 Date: 9/15/16  
Pretest Leak Rate: .001 cfm @ 8 in.Hg.  
Pretest Leak Check: Pitot: ☒ Orsat: -

Sample Type: Carb/428/429 Operator: GD/ΔA  
Pbar: 30.24 Ps: -1.9  
CO<sub>2</sub>: 0 O<sub>2</sub>: 0  
Probe Length/Type: 3' G1 Pto#/: 73-1  
Stack Diameter: 35.5" K: 0.6096

Nozzle ID: 156 Thermocouple #: 73-1  
 Assumed Bws: 1.8 Filter #: Unfired  
 Meter Box #: 13 Y: 0.989 ΔH@: 1.783  
 Post-Test Leak Rate: 0.002 cfm @ 10 in.Hg.  
 Post-Test Leak Check: Pitot: ✓ Orsat: —

[illegible]

$$\Delta V_m = 147.718 \sqrt{\Delta p} = 1.7342 \sqrt{\Delta H} = 1.74 \sqrt{T_S} = 103$$

72 = 72

$$\Delta R = 3.01$$

## SAMPLE RECOVERY DATA

Plant AK Middletown Run No. P-CARB-3  
 Date 9/15/14 Sample Box No. NB-6 Job No. 56074.0172  
 Sample Location Picking Bayhouse Filter No. Quartz  
 Train Preparer NB/BS Sample Head No. .8  
 Sample Recovery Person DA/CS Barometer No. 1  
 Comments CARB Balance No. 1

Front Half

Acetone P-CARB-3 Liquid —  
 Container No. — Level Marked — Sealed —

Filter

Container No. Quartz P-CARB-3 Sealed ✓

Description of Filter Clear

Samples Stored and Locked ✓

Back Half/Moisture

Container No. P-CARB-3

Liquid Level Marked — Sealed —

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	MT	-0	490.3	511.4	21.1
2	H <sub>2</sub> O	100	771.1	764.8	6.3
3	MT	-0	694.0	697.7	3.7
4	Silica Gel	250	973.2	1012.8	39.6
5					
6					
Total					70.7

Description of Impinger Catch: clear

TRAP  
6

Plant: AK Middle town  
 Sampling Location: Combustion Stack  
 Run Number: 6-CARB-1 Date: 4-13-16  
 Pretest Leak Rate: .4 cfm @ 10 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: -

Sample Type: CARB Operator: NP  
 Pbar: 30.20 Ps: 1.94  
 CO<sub>2</sub>: 3 O<sub>2</sub>: 15  
 Probe Length/Type: 6'64 Pitot#: T6-15P  
 Stack Diameter: 16.8" K: 53.113

Nozzle ID: 500 Thermocouple #: T6-15P  
 Assumed Bws: 10 Filter #: unfired Q2  
 Meter Box #: 2 Y: 1.085 AH@: 1.637  
 Post-Test Leak Rate: 102.1 cfm @ 10 in.Hg.  
 Post-Test Leak Check: Pitot: ✓ Orsat: -

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	1005	284.387											
1	5	1010	287.2	.03	1.0	1.0	353	260	260	85	NA	65	65	3
2	10	1015	290.5	.04	1.4	1.4	355	261	264	65	66	63	63	3
3	15	1020	293.8	.04	1.4	1.4	358	265	263	64	65	63	63	3
4	20	1025	297.2	.04	1.4	1.4	359	264	263	59	65	64	64	3
5	25	1030	300.5	.04	1.4	1.4	363	257	264	56	63	65	64	5
6	30	1035	303.9	.04	1.4	1.4	366	264	264	54	63	67	64	5
7	35	1040	307.3	.04	1.4	1.4	369	269	265	55	64	69	65	5
8	40	1045	310.7	.04	1.4	1.4	373	267	264	56	48	72	66	5
9	45	1050	314.1	.04	1.4	1.4	367	266	264	57	50	75	67	5
10	50	1055	317.4	.04	1.4	1.4	344	268	265	57	50	76	68	5
11	55	1100	320.7	.04	1.4	1.4	345	264	264	59	57	77	69	5
12	60	1105	324.1	.04	1.4	1.4	351	262	264	58	49	79	70	5
1	65	1110	327.4	.04	1.4	1.4	353	266	264	57	48	80	70	5
2	70	1115	330.7	.04	1.4	1.4	354	267	250	57	47	80	71	5
3	75	1120	334.1	.04	1.4	1.4	359	266	264	56	52	81	73	5
4	80	1125	337.4	.04	1.4	1.4	361	263	264	56	52	81	73	5
5	85	1130	340.7	.04	1.4	1.4	364	265	264	56	53	82	74	5
6	90	1135	344.1	.04	1.4	1.4	370	257	264	56	55	83	74	5
7	95	1140	347.4	.04	1.4	1.4	372	265	264	56	54	83	75	5
8	100	1145	350.8	.04	1.4	1.4	376	266	264	57	53	84	75	5
9	105	1150	354.1	.04	1.4	1.4	372	257	264	57	55	84	76	5
10	110	1155	357.6	.04	1.4	1.4	375	258	263	57	55	84	76	5
11	115	1200	360.9	.04	1.4	1.4	346	270	264	60	56	85	77	5
12	120	1205	364.2	.04	1.4	1.4	352	262	263	60	56	86	77	5

$$\Delta V_m = \sqrt{\Delta p} = \frac{\Delta H}{T_s} = \frac{T_m}{T_s}$$

Plant: AK Middletown  
 Sampling Location: Combustion Stack  
 Run Number: C-CARB-1 Date: 9-12-16  
 Pretest Leak Rate: 0.01 cfm @ 10 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: -

Sample Type: D/F CARB Operator: UP  
 Pbar: 30.30 Ps: -94  
 CO<sub>2</sub>: 3 O<sub>2</sub>: 15  
 Probe Length/Type: 6' GL Pitot# 76-15P  
 Stack Diameter: 168" K: 53.1/3

Nozzle ID: 1500 Thermocouple #: 76-15P  
 Assumed Bws: 10 Filter #: Untared QZ  
 Meter Box #: 2 Y: 1005 AH@: 1.687  
 Post-Test Leak Rate: 0.01 cfm @ 10 in.Hg.  
 Post-Test Leak Check: Pitot: ✓ Orsat: -

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	AH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
1	125	1210	367.6	.04	1.4	1.4	355	253	264	57	59	86	79	5
2	130	1215	371.0	.04	1.4	1.4	355	254	264	58	57	87	79	5
3	135	1220	374.4	.04	1.4	1.4	357	260	265	58	57	87	79	5
4	140	1225	378.3	.04	1.4	1.4	362	256	264	57	55	88	80	5
5	145	1230	381.6	.04	1.4	1.4	366	263	264	57	55	88	80	5
6	150	1235	385.0	.04	1.4	1.4	370	264	264	57	56	90	80	5
7	155	1240	389.4	.04	1.4	1.4	375	267	264	61	53	89	81	5
8	200 160	1245	391.8	.04	1.4	1.4	376	267	265	61	60	89	81	5
9	205 165	1250	395.1	.04	1.4	1.4	352	260	264	61	51	90	82	5
10	210 170	1255	398.5	.04	1.4	1.4	344	261	263	58	53	90	82	5
11	215 175	1300	401.9	.04	1.4	1.4	346	251	264	58	53	90	83	5
12	220 180	1305	405.3	.04	1.4	1.4	349	261	264	58	55	90	83	5
1	225 185	1310	408.8	.04	1.4	1.4	350	263	265	58	55	91	83	5
2	230 190	1315	412.0	.04	1.4	1.4	353	263	265	58	53	90	83	5
3	235 195	1320	415.0	.04	1.4	1.4	355	264	264	61	53	91	84	5
4	240 200	1325	418.8	.04	1.4	1.4	356	265	263	61	53	91	84	5
5	245 205	1330	422.1	.04	1.4	1.4	366	263	263	56	48	91	84	5
6	250 210	1335	425.3	.04	1.4	1.4	377	267	265	56	49	92	85	5
7	255 215	1340	428.9	.04	1.4	1.4	377	259	266	56	49	92	85	5
8	260 220	1345	432.3	.04	1.4	1.4	378	253	265	56	48	92	85	5
9	265 225	1350	434.8	.04	1.4	1.4	345	253	264	56	50	92	85	5
10	270 230	1355	439.2	.04	1.4	1.4	344	260	263	57	50	93	86	5
11	275 235	1400	442.7	.04	1.4	1.4	352	261	263	57	51	93	86	5
12	280 240	1405	445.855	.04	1.4	1.4	353	262	265	57	51	93	86	5

$$\Delta Vm = 161.469 \quad \sqrt{\Delta P} = 1.444 \quad \Delta H = 1.3917 \quad Ts = 360$$

$$Tm = 80$$

$$\sqrt{\Delta P} = 0.19944 \quad Ave \quad 0.19944$$



## SAMPLE RECOVERY DATA

Plant AK Middletown Run No. C-CARB-1  
Date 9/12/16 Sample Box No. 2 Job No. 0520740172  
Sample Location COMBUSTION STACK Filter No. NA  
Train Preparer MP Sample Head No. 10  
Sample Recovery Person BF/RIC Barometer No. rwl.com  
Comments CARB Method Balance No. FB-2

Front Half

Acetone Liquid  
Container No. C-CARB-1 Level Marked ✓ Sealed ✓

Filter

Container No. C-CARB-1 Sealed ✓

Description of Filter Black

Samples Stored and Locked ✓

Back Half/Moisture

Container No. NA

Liquid Level Marked NA Sealed NA

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	—	—	484.0	816.5	332.5
2	H <sub>2</sub> O	100	708.3	729.4	- 38.9
3	—	—	665.7	669.6	3.9
4	Silica	250	907.3	942.3	35.0
5					
6					
Total					332.5

Description of Impinger Catch: clear

✓BF

Plant: **AK Middleton**Sampling Location: **Combustion Space**Run Number: **C-CARB-2** Date: **9-12-16**Pretest Leak Rate: **.001** cfm @ **10** in.Hg.Pretest Leak Check: Pitot: **✓** Orsat: **—**Sample Type: **CARB**Operator: **NP**Pbar: **30.15** Ps: **—**CO<sub>2</sub>: **3** O<sub>2</sub>: **15**Probe Length/Type: **6' 6"** Pitot#: **76-15P**Stack Diameter: **16 1/2"** K: **53.113**Nozzle ID: **500** Thermocouple #: **T6-15P**Assumed Bws: **10** Filter #: **untared QZ**Meter Box #: **2** Y: **1005** ΔH@: **1687**Post-Test Leak Rate: **—** cfm @ **—** in.Hg.Post-Test Leak Check: Pitot: **—** Orsat: **—**

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	955	446.130	.04	1.3	1.3	379	260	260	65	60	63	63	4
1	5	1000	449.4	.04	1.3	1.3	353	252	270	65	60	63	64	4
2	10	1005	452.7	.04	1.4	1.4	356	262	265	63	36	67	66	4
3	15	1010	456.9	.04	1.4	1.4	355	264	265	61	37	68	66	4
4	20	1015	459.3	.04	1.4	1.4	357	264	265	58	37	70	67	4
5	25	1020	462.5	.04	1.4	1.4	362	266	262	59	37	73	67	4
6	30	1025	465.8	.04	1.4	1.4	364	265	264	59	37	74	67	5
7	35	1030	469.3	.04	1.4	1.4	371	264	264	60	37	76	69	5
8	40	1035	472.5	.04	1.4	1.4	374	264	265	60	38	77	69	5
9	45	1040	475.8	.04	1.4	1.4	374	264	264	60	38	78	69	5
10	50	1045	479.1	.04	1.4	1.4	374	264	264	60	38	78	70	5
11	55	1050	482.4	.04	1.4	1.4	380	264	265	60	37	78	70	5
12	60	1055	485.7	.04	1.4	1.4	345	263	264	59	38	80	71	5
1	65	1100	489.1	.04	1.4	1.4	346	264	263	59	38	81	72	5
2	70	1105	492.4	.04	1.4	1.4	349	265	265	60	38	82	73	5
3	75	1110	495.8	.04	1.4	1.4	351	263	264	60	39	82	73	5
4	80	1115	499.2	.04	1.4	1.4	350	264	264	60	39	82	73	5
5	85	1120	502.6	.04	1.4	1.4	351	264	264	62	40	85	76	5
6	90	1125	505.9	.04	1.4	1.4	361	266	265	61	41	86	77	5
7	95	1130	509.2	.04	1.4	1.4	367	264	264	62	42	87	78	5
8	100	1135	513.1	.04	1.4	1.4	368	263	263	62	42	88	78	5
9	105	1140	516.0	.04	1.4	1.4	372	264	264	62	43	88	78	5
10	110	1145	519.5	.04	1.4	1.4	375	267	263	63	44	88	79	5
11	115	1150	522.9	.04	1.4	1.4	340	265	263	64	44	88	80	5
12	120	1155	526.4	.04	1.4	1.4	360	264	263	64	44	89	81	5

$$\Delta V_m = \frac{\sqrt{\Delta p}}{\sqrt{\Delta H}} \quad \Delta H = \frac{\Delta T_m}{T_s} = \frac{T_m}{T_s}$$



Plant: AK Middleton  
 Sampling Location: Cambushen Stack  
 Run Number: C-CARB-2 Date: 9-12-16  
 Pretest Leak Rate: 2.1 cfm @ 10 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: -

Sample Type: CARB Operator: NP  
 Pbar: 30.5 Ps: ~.9  
 CO<sub>2</sub>: 3 O<sub>2</sub>: 15  
 Probe Length/Type: 6' G-2 Pitot#: T6-07P  
 Stack Diameter: 168" K: 53.113

Nozzle ID: 500 Thermocouple #: T6-15P  
 Assumed Bws: 10 Filter #: Untared Q2  
 Meter Box #: 2 Y: 1003 ΔH@: 1687  
 Post-Test Leak Rate: 2002 cfm @ 9 in.Hg.  
 Post-Test Leak Check: Pitot: ✓ Orsat: -

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature BF		Impinger Temp. of	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
1	125	1200	530.0	.04	1.4	1.4	355	264	263	55	36	89	82	5
2	130	1205	533.1	.04	1.4	1.4	355	265	265	56	37	89	82	5
3	135	1210	536.5	.04	1.4	1.4	355	264	262	56	37	90	82	5
4	140	1215	539.9	.04	1.4	1.4	356	264	263	56	38	90	82	5
5	145	1220	543.3	.04	1.4	1.4	357	266	264	58	37	90	82	5
6	150	1225	546.7	.04	1.4	1.4	358	269	264	58	38	90	82	5
7	155	1230	550.1	.04	1.4	1.4	360	264	264	58	39	91	83	5
8	160	1235	553.5	.04	1.4	1.4	361	265	263	54	39	90	83	5
9	165	1240	556.9	.04	1.4	1.4	373	264	264	53	37	90	83	5
10	170	1245	560.5	.04	1.4	1.4	375	264	263	53	37	90	83	5
11	175	1250	563.9	.04	1.4	1.4	358	264	263	54	37	90	83	5
12	180	1255	567.3	.04	1.4	1.4	359	264	262	54	37	90	83	5
1	185	1300	570.6	.04	1.4	1.4	348	263	265	57	38	90	83	5
2	190	1305	574.0	.04	1.4	1.4	349	258	265	56	37	89	83	5
3	195	1310	577.4	.04	1.4	1.4	352	265	264	55	38	89	83	5
4	200	1315	580.8	.04	1.4	1.4	353	263	264	56	38	89	83	5
5	205	1320	584.2	.04	1.4	1.4	355	263	264	56	38	89	83	5
6	210	1325	587.6	.04	1.4	1.4	357	265	265	57	40	90	83	5
7	215	1330	591.2	.04	1.4	1.4	368	264	264	62	43	90	83	5
8	220	1335	594.3	.04	1.4	1.4	364	261	264	61	43	90	83	5
9	225	1340	598.0	.04	1.4	1.4	372	266	264	60	41	90	83	5
10	230	1345	601.3	.04	1.4	1.4	373	262	264	60	40	90	83	5
11	235	1350	604.6	.04	1.4	1.4	373	263	264	59	40	91	84	5
12	240	1355	608.096	.04	1.4	1.4	370	264	264	58	40	91	84	5

$$\Delta Vm = 161.966 \sqrt{\Delta P} = .2000 \Delta H = 1.3950 Ts = 362$$

$$Ave DP = .04$$

$$Tm = 81$$

JAC

## SAMPLE RECOVERY DATA

Plant AK Middletown Run No. Comb Carb - 2  
 Date 9/10/16 Sample Box No. #28-2 Job No. 052074.0172  
 Sample Location COMBUSTION Filter No. NA  
 Train Preparer BF/RK Sample Head No. 34-10  
 Sample Recovery Person BF/RK Barometer No. TWC.com  
 Comments CARB Balance No. F8-2

Front Half

Acetone Liquid  
 Container No. C-CARB-2 Level Marked ✓ Sealed ✓

## Filter

Container No. C-CARB-2 Sealed ✓

Description of Filter black

Samples Stored and Locked ✓

Back Half/Moisture

Container No. NA

Liquid Level Marked NA Sealed NA

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	—	—	486.0	815.3	329.3
2	H <sub>2</sub> O	100	773.5	765.7	-7.8
3	—	—	669.3	674.1	4.8
4	Silica Gel	250	982.2	1016.9	34.7
5					
6					
Total					361.0

Description of Impinger Catch: clear

JBF

Plant: AK Middleton  
 Sampling Location: Cambuslangh Stack  
 Run Number: C-4463 Date: 9-14-16  
 Pretest Leak Rate: 100 cfm @ 10 in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: —

Sample Type: CRB Operator: NP  
 Pbar: 30.21 Ps: -9  
 CO<sub>2</sub>: 3 O<sub>2</sub>: 15  
 Probe Length/Type: 6' GL Pitot# 76-15P  
 Stack Diameter: 16.4" K: 53.113

Nozzle ID: 500 Thermocouple #: 76-15P  
 Assumed Bws: 10 Filter #: UNfiltered  
 Meter Box #: 2 Y: 1005 ΔH@: 1.667  
 Post-Test Leak Rate: — cfm @ — in.Hg.  
 Post-Test Leak Check: Pitot: — Orsat: —

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature BF		Impinger Temp. of	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0	955	603.340											
1	5	1000	611.6	.04	1.4	1.4	350	260	260	65	33	62	62	4
2	10	1005	614.9	.04	1.4	1.4	345	265	267	65	33	64	64	4
3	15	1010	613.2	.04	1.4	1.4	350	263	264	65	42	65	64	4
4	20	1015	621.5	.04	1.4	1.4	352	265	264	56	34	66	65	5
5	25	1020	624.3	.04	1.4	1.4	351	266	264	49	34	68	65	5
6	30	1025	628.2	.04	1.4	1.4	352	266	265	49	34	68	65	5
7	35	1030	631.6	.04	1.4	1.4	357	263	264	48	35	70	66	5
8	40	1035	634.9	.04	1.4	1.4	362	265	264	49	35	71	67	5
9	45	1040	638.4	.04	1.4	1.4	364	262	264	49	34	74	67	5
10	50	1045	641.7	.04	1.4	1.4	367	264	263	51	33	75	68	5
11	55	1050	645.1	.04	1.4	1.4	373	265	264	53	33	77	69	5
12	60	1055	648.4	.04	1.4	1.4	347	264	264	53	33	80	71	5
1	65	1100	651.8	.04	1.4	1.4	345	264	264	53	34	80	71	5
2	70	1105	655.1	.04	1.4	1.4	351	261	265	57	35	84	74	5
3	75	1110	658.4	.04	1.4	1.4	352	268	265	56	35	86	74	5
4	80	1115	661.8	.04	1.4	1.4	350	265	264	56	35	84	75	5
5	85	1120	665.1	.04	1.4	1.4	348	267	263	57	35	84	75	5
6	90	1125	668.8	.04	1.4	1.4	358	263	265	56	36	84	76	5
7	95	1130	671.9	.04	1.4	1.4	367	261	264	58	37	86	77	5
8	100	1135	675.2	.04	1.4	1.4	368	266	264	58	37	86	77	5
9	105	1140	678.5	.04	1.4	1.4	370	265	263	58	37	86	78	5
10	110	1145	681.9	.04	1.4	1.4	371	264	264	59	37	86	78	5
11	115	1150	685.4	.04	1.4	1.4	370	265	261	59	38	87	78	5
12	120	1155	688.7	.04	1.4	1.4	364	266	263	59	38	87	78	5

$$\Delta V_{tm} = \sqrt{\Delta p} = \frac{\Delta H}{\Delta H} = \frac{T_s}{T_m} =$$

Plant: AK Middletown Sample Type: CARB Operator: NP  
 Sampling Location: Combustion Stack Pbar: 30.21 Ps: -4  
 Run Number: C-CARB-3 Date: 9-14-16 CO<sub>2</sub>: 3 O<sub>2</sub>: 15  
 Pretest Leak Rate: .001 cfm @ 10 in.Hg. Probe Length/Type: 6' 04" Pitot#: 16-15P  
 Pretest Leak Check: Pitot: ✓ Orsat: - Stack Diameter: 16.2" K: 53.113

Nozzle ID: 506 Thermocouple #: 76-15P  
 Assumed Bws: 10 Filter #: untreated Q2  
 Meter Box #: 2 Y: 1-005 ΔH@: 1.687  
 Post-Test Leak Rate: .001 cfm @ 8 in.Hg.  
 Post-Test Leak Check: Pitot: ✓ Orsat: NA

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp, °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
1	129	1200	692.1	.04	1.4	1.4	352	261	263	65	48	88	81	5
2	130	1205	695.6	.04	1.4	1.4	352	264	263	65	41	89	81	5
3	135	1210	699.1	.04	1.4	1.4	353	264	264	61	39	89	81	5
4	140	1215	702.5	.04	1.4	1.4	355	265	265	55	37	89	82	5
5	145	1220	706.0	.04	1.4	1.4	355	266	264	54	37	89	82	5
6	150	1225	709.4	.04	1.4	1.4	351	265	264	54	34	89	82	5
7	155	1230	712.7	.04	1.4	1.4	360	266	265	53	34	90	83	5
8	160	1235	716.3	.04	1.4	1.4	365	263	263	53	35	90	83	5
9	165	1240	719.8	.04	1.4	1.4	365	264	264	53	35	90	83	5
10	170	1245	723.2	.04	1.4	1.4	365	265	265	53	35	90	83	5
11	175	1250	726.6	.04	1.4	1.4	378	261	263	54	35	91	84	5
12	180	1255	730.0	.04	1.4	1.4	363	267	263	55	35	91	84	5
1	185	1300	733.4	.04	1.4	1.4	346	264	264	56	34	91	84	5
2	190	1305	737.1	.04	1.4	1.4	348	260	265	57	35	91	84	5
3	195	1310	740.8	.04	1.4	1.4	349	267	264	57	35	91	84	5
4	200	1315	744.2	.04	1.4	1.4	354	266	264	58	36	91	85	5
5	205	1320	747.2	.04	1.4	1.4	356	266	263	58	36	91	85	5
6	210	1325	750.7	.04	1.4	1.4	356	265	265	54	32	92	85	5
7	215	1330	753.8	.04	1.4	1.4	353	260	264	58	36	92	85	5
8	220	1335	757.2	.04	1.4	1.4	358	263	263	58	36	92	85	5
9	225	1340	760.6	.04	1.4	1.4	359	262	264	57	35	92	86	5
10	230	1345	764.0	.04	1.4	1.4	360	261	263	57	35	93	86	5
11	235	1350	767.5	.04	1.4	1.4	361	260	265	57	35	93	86	5
12	240	1355	770.961	.04	1.4	1.4	362	265	263	54	35	93	86	5

$$\Delta V_m = 162.671 \sqrt{\Delta p} = .2 \quad \Delta H = 1.4 \quad T_s = 357$$

$$T_m = 81$$

ACON - .04

✓

## SAMPLE RECOVERY DATA

Plant AK Steel - Middletown Run No. C-CARB-3  
 Date 9/24/16 Sample Box No. HSB-2 Job No. 5024.0172  
 Sample Location Combustion Filter No. Pent 2  
 Train Preparer BF/RK Sample Head No. SW 10  
 Sample Recovery Person BF/RK Barometer No. TWC com  
 Comments CARB Train Balance No. 15B-2

Front Half

Acetone Liquid  
 Container No. C-CARB-3 Level Marked ☒ Sealed ☒

Filter

Container No. C-CARB-3 Sealed ☒

Description of Filter black

Samples Stored and Locked ☒

Back Half/Moisture

Container No. NA

Liquid Level Marked NA Sealed NA

Imp. No.	Contents	Initial Vol (ml)	Weight (grams)		
			Initial	Final	Net
1	-O-	-O-	487.2	867.8	380.6
2	H <sub>2</sub> O	100	771.9	767.1	-4.8
3	-O-	-O-	670.9	676.0	5.1
4	Silicobal	250	965.8	1001.8	36.0
5					
6					
Total					416.9

Description of Impinger Catch: clear

✓BF

**FLOW**

## TRAVERSE POINT LOCATION FOR CIRCULAR DUCTS

Plant: Hot Steel Mill between

Date: 8/22/16

Date: \_\_\_\_\_  
Sampling Location: Pushing, Bughouse, Stacks 1-5

Inside of Far Wall to Outside of Nipple: 4 1/2

Inside of Near Wall to Outside of Nipple (Nipple Length): 6

Stack I.D.: 35 1/2

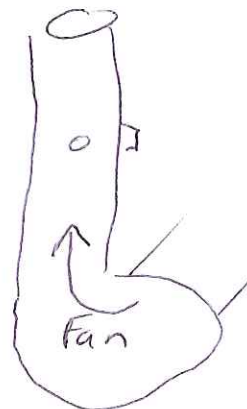
Distance Downstream from Flow Disturbance (Distance B):

300 Inches/Stack I.D. = 8.5 dd

Distance Upstream from Flow Disturbance (Distance A):

72 Inches/Stack I.D. = 20 dd

Calculated By: Doug Allen



### Schematic of Sampling Location

[illegible]

# CEM CALIBRATION DATA SHEET

Company:  
Location:  
Project No.:

AK steel Middletown  
Pushing Bayhorse  
50074.0172

Operator: \_\_\_\_\_  
Date: \_\_\_\_\_

Don't Wen / Ben Fern  
8/30/16

[illegible]



## CEM CALIBRATION DATA SHEET

Ak Middleton  
Pushing Bayhouse  
050674-072

Company:  
Location:  
Project No:

Operator:  
Date:

Ben Fern  
8/30/16

Final cal

[illegible]

## CEM CALIBRATION DATA SHEET

Allen

813416

813416

[illegible]



Environmental Quality Management, Inc.

# CEM CALIBRATION DATA SHEET

Company: Ak Steel Middletown

Location:

Operator: C. Janzen

Project No.: 50074.0172

Date: 7/6/16

COMBUSTION

POST-HYDRO

Pollutant/ Range/ Inst. ID	Cal Gas	Cal Gas Conc.	Calibration Response		Post Test Run 1			Post Test Run 2			Post Test Run 3			Cylinder No.
			Direct	System	ppm/%	%Drift	%Bias	ppm/%	%Drift	%Bias	ppm/%	%Drift	%Bias	
			Time:	Time:	Time: 1002 -	1434		Time: 1507 - 1525	1717		Time:			
02	Zero	0	0.181	0.075	0.119	0.047		0.024	-0.018					
	Low	-												
	Mid	11.02	11.199	10.937										
	High	21.89	22.059	21.769	21.829	21.952		21.927	22.045					
CO2	Zero	0	0.252	0.158	0.258	0.134		0.079	0.052					
	Low	-												
	Mid	11.33	11.224	11.083	10.946	11.242		11.163	11.264					
	High	21.94	22.175	21.720										
CO	Zero	0	0.71	0.71	-0.72	0.04		-0.43	-0.51					
	Low	-												
	Mid	190.9	189.75	189.87	184.22	185.75		184.57	184.81					
	High	454.0	452.68	449.74										
	Zero													
	Low													
	Mid													
	High													
Averages														

PAID 1300 COMBUSTION OFF  
RESTORE 1307 CAL



## CEM CALIBRATION DATA SHEET

Company:

AK steel mddletown

Location:

Combustion

Project No.:

52074-0172

Operator:

Date:

CombustionDisbury[illegible]

## CEM CALIBRATION DATA SHEET

Company: Ak steel Middletown  
Location: Combustion stack  
Project No.: 50074-0172

[illegible]





## CEM CALIBRATION DATA SHEET

Company:

Av steel mddletan

Location:

Combustion & Cooling Bal

Project No.:

52074.0172  
Combustion  
System

Operator:

Date: 9/12/16

Pushing SYSTEM

Pollutant/ Range/ Inst. ID	Cal Gas	Cal Gas Conc.	Calibration Response		Post Test Run 1			Post Test Run 2			Post Test Run 3			Cylinder No.
			Direct Time:	System Time:	ppm/% Time:	%Drift	%Bias	ppm/% Time:	%Drift	%Bias	ppm/% Time:	%Drift	%Bias	
O <sub>2</sub>	Zero	0	-0.009	0.085	1005-1305	0.098	1336-1741	-0.062	-0.046					
	Low													
	Mid	11.02	16.95	16.95	14.778			10.945						
	High	21.89	22.03	22.179	21.879	21.910	21.932	21.910						
CO <sub>2</sub>	Zero	0	0.064	0.146	0.018	0.018	0.072	0.054	0.072					
	Low	-												
	Mid	11.33	11.06	11.218	10.946	11.085	10.968							
	High	21.94	22.12	22.208		22.063	21.910							
CO	Zero	0		5.26	7.20	7.20	7.92	0.26	7.92					
	Low	-												
	Mid	190.9	192.07	192.03	193.01	193.18	192.91							
	High	454.8	454.16	455.14		455.91								
	Zero													
	Low													
	Mid													
	High													
Averages	O <sub>2</sub>				14.718		20.728							
	CO <sub>2</sub>				3.452		0.254							
	CO				91.10		37.57							

## CEM CALIBRATION DATA SHEET

Company:

Location:

Project No.:

AK STEEL MIDDLETOWN

PUSHING BACKHOUSE

052074.0172

Operator:

Date:

Canzer

9/12/16 - 9/13/16

[illegible]



## CEM CALIBRATION DATA SHEET

Company: AK STEEL MIDLETOWN  
 Location: CONCRETE STACK / PUSHING BAYHOUSE  
 Project No.: 050074.0172

Operator: BF  
 Date: 9/13/16

[illegible]



## CEM CALIBRATION DATA SHEET

Company:

AK Middle town

AK Middleton  
Combustion Stack, Pushing Bayhouse

Project No.:

050074.0172

Operator:

Date:

Ben Fern

9/14/16

COMBUSTION COMBUSTION RUN 3

## PUSHING SYSTEM CAL

pushing run

[illegible]



## CEM CALIBRATION DATA SHEET

Company:  
Location:  
Project No.:

Operator:  
Date:

9/14-15/16

[illegible]



Flows

Plant: AK Middletown Sample Type: EZ Operator: EZ Nozzle ID: \_\_\_\_\_ Thermocouple #: \_\_\_\_\_  
 Sampling Location: Baghouse Stack 1 Pbar: 30.44 Ps: -1.0 Assumed Bws: \_\_\_\_\_ Filter #: \_\_\_\_\_  
 Run Number: 8 Date: 6/29/06 CO<sub>2</sub>: \_\_\_\_\_ O<sub>2</sub>: \_\_\_\_\_ Meter Box #: 1010 Y: 1010 ΔH@: 179  
 Pretest Leak Rate: \_\_\_\_\_ cfm @ \_\_\_\_\_ in.Hg. Post-Test Leak Rate: \_\_\_\_\_ cfm @ \_\_\_\_\_ in.Hg.  
 Pretest Leak Check: Pitot: ✓ Orsat: \_\_\_\_\_ Post-Test Leak Check: Pitot: \_\_\_\_\_ Orsat: \_\_\_\_\_

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0													
1				2.8			118							
2				2.9			122							
3				2.9			125							
4				2.9			124							
5				3.0			122							
6				3.0			127							
1				2.9			123							
2				3.2			123							
3				3.2			123							
4				3.2			125							
5				3.2			123							
6				3.1			120							
#1														
2														
3														
4														
5														
6														
1														
2														
3														
4														
5														
6														
1														

ΔV<sub>m</sub> = \_\_\_\_\_  $\sqrt{\Delta p} = 1.7388$  ΔH = \_\_\_\_\_ T<sub>s</sub> = 123

T<sub>m</sub> = \_\_\_\_\_

## FIELD DATA SHEET

Plant: AK Middleton Sample Type: Flare Operator: EZ Nozzle ID: \_\_\_\_\_ Thermocouple #: \_\_\_\_\_  
 Sampling Location: Baghouse Stack Pbar: 30.20 Ps: -1.1 Assumed Bws: \_\_\_\_\_ Filter #: \_\_\_\_\_  
 Run Number: Flare Date: 9/12/16 CO<sub>2</sub>: \_\_\_\_\_ Meter Box #: 11 Y: 1.210 ΔH@: 1.791  
 Pretest Leak Rate: \_\_\_\_\_ cfm @ \_\_\_\_\_ in.Hg. Post-Test Leak Rate: \_\_\_\_\_ cfm @ \_\_\_\_\_ in.Hg.  
 Pretest Leak Check: Pitot: √E Orsat: \_\_\_\_\_ Stack Diameter: 35.5" K: \_\_\_\_\_ Post-Test Leak Check: Pitot: \_\_\_\_\_ Orsat: \_\_\_\_\_

Traverse Point Number	Sampling Time	Clock Time	Gas Meter Reading	Velocity Head	ΔH		Stack Temp (Ts)	Temperature EF		Impinger Temp. °F	Aux. Temp.	Dry Gas Meter Temp.		Pump Vacuum (in. Hg)
					Desired	Actual		Probe	Filter			Inlet	Outlet	
0	0													
1				2.7			92							
2				2.7			102							
3				3.5			110							
4				3.7			115							
5				3.4			121							
6				3.5			118							
7				3.2			129							
8				3.0			125							
9				3.4			121							
10				3.5			115							
11				3.3			126							
12				3.4			130							
13				3.1			135							
14				3.2			130							
15				3.2			120							
16				3.1			132							
17				3.0			138							
18				3.0			127							
19				3.0			126							
20				2.9			120							
21				2.9			125							
22				3.0			135							
23				3.0			130							
24				3.0			127							

ΔV<sub>m</sub> =  $\sqrt{\Delta p}$  = 1.774 ΔH = 123 T<sub>m</sub> = \_\_\_\_\_

## FIELD DATA SHEET

Plant: AK Middlebury Sample Type: CS Operator: CS  
 Sampling Location: Baghouse stack Pbar: 1 Ps: 1  
 Run Number: Flow Date: 9/12-13/16 O<sub>2</sub>: CO<sub>2</sub>:  
 Pretest Leak Rate: cfm @ in.Hg. Probe Length/Type: Pitot#:  
 Pretest Leak Check: Pitot: Orsat: Stack Diameter: K:

[illegible]

$\Delta V_m =$	$\sqrt{\Delta p} =$	$\Delta H =$	$T_S =$	$T_m =$
----------------	---------------------	--------------	---------	---------



Operator: \_\_\_\_\_  
 Ps: \_\_\_\_\_  
 O2: \_\_\_\_\_  
 Length/Type: \_\_\_\_\_ Pitot#: \_\_\_\_\_  
 Diameter: \_\_\_\_\_ K: \_\_\_\_\_

Nozzle ID: \_\_\_\_\_ Thermocouple #: \_\_\_\_\_

[illegible]

$$\Delta V_m = \sqrt{\Delta p} = \overline{\Delta H} = T_s =$$

---

 $Tm =$

## GAS VELOCITY AND VOLUMETRIC FLOW RATE

Plant: AK Middletown Date: 9/13/16  
 Sampling Location: Bughouse Stack 1 Clock Time: \_\_\_\_\_  
 Run #: Flow Operators: EZ  
 Barometric Pressure, in. Hg: 30.15 Static Pressure, in. H<sub>2</sub>O: -1.3  
 Moisture, %: \_\_\_\_\_ Molecular wt., Dry: \_\_\_\_\_ Pitot Tube, Cp: \_\_\_\_\_  
 Stack Dimension, in. Diameter or Side 1: \_\_\_\_\_ Side 2: \_\_\_\_\_  
 Wet Bulb, °F: \_\_\_\_\_ Dry Bulb, °F: \_\_\_\_\_ CO<sub>2</sub> % \_\_\_\_\_  
 Pitot # \_\_\_\_\_ Thermocouple # \_\_\_\_\_ O<sub>2</sub> % \_\_\_\_\_

[Push #]

Pitot Leak Check: Positive \_\_\_\_\_ Negative \_\_\_\_\_

Time

Traverse Point Number	Velocity Head in. H <sub>2</sub> O	Stack Temp, °F
1	<del>3.5</del> 4.0	98
2	4.1	115
3	3.8	130
4	3.8	136
5	3.7	137
6	3.8	135
7	3.7	133
8	3.6	130
9	3.5	137
10	3.5	136
11	3.6	125
12	3.6	130
13	3.6	133
14	3.6	128
15	3.6	132
16	3.7	133
17	3.5	135
18	3.5	132
19	3.5	140
20	3.5	138
21	3.5	139
22	3.6	138
23	3.5	132
24	3.5	135
25	3.5	128
$\sqrt{\Delta P} = 1.9053$		$\overline{T_s} = 131$

$$Md = (0.44 \times \%CO_2) + (0.32 \times \%O_2) + (0.28 \times \%N_2)$$

$$Md = (0.44 \times \quad) + (0.32 \times \quad) + (0.28 \times \quad)$$

$$Md =$$

$$Ms = Md \times \left(1 - \frac{\%H_2O}{100}\right) + 18 \times \left(\frac{\%H_2O}{100}\right)$$

$$Ms = \left(\quad\right) \times \left(1 - \frac{\quad}{100}\right) + 18 \times \left(\frac{\quad}{100}\right)$$

$$Ms =$$

$$\overline{T_s} = \quad ^\circ F = \quad ^\circ R (^\circ F + 460)$$

$$Ps = Pb + \frac{SP}{13.6} = \left(\quad\right) + \frac{\quad}{13.6}$$

$$Ps = \quad \text{in. Hg}$$

$$\sqrt{\Delta P} =$$

$$Vs = 85.49 \times Cp \times \sqrt{\Delta P} \times \sqrt{\frac{T_s(^{\circ}R)}{Ps \times Ms}}$$

$$Vs = 85.49 \times \left(\quad\right) \times \left(\quad\right) \times \sqrt{\quad}$$

$$Vs = \quad \text{ft/s}$$

$$As = \quad \text{ft}^2$$

$$Qs = Vs \times As \times 60$$

$$Qs = \quad \times \quad \times 60$$

$$Qs = \quad \text{acfm}$$

$$Q_{sstd} = Qs \times 17.647 \times \frac{Ps}{T_s} \times \left(1 - \frac{\%H_2O}{100}\right)$$

$$Q_{sstd} = \quad \times 17.647 \times \quad \times \left(1 - \frac{\quad}{100}\right)$$

$$Q_{sstd} = \quad \text{dscfm}$$

## GAS VELOCITY AND VOLUMETRIC FLOW RATE

Plant: AK Middletown

Date: 9/13/16

Sampling Location: Bridgeway Stack 2

Clock Time: \_\_\_\_\_

Run #: Flow

Operators: EL

Barometric Pressure, in. Hg: 30.15

Static Pressure, in. H<sub>2</sub>O: 4.0

Moisture, %:                      Molecular wt., Dry:

Pitot Tube,  $C_p$ : \_\_\_\_\_

Stack Dimension, in. Diameter or Side 1:

Side 2: \_\_\_\_\_

Wet Bulb, °F: \_\_\_\_\_ Dry Bulb, °F: \_\_\_\_\_

Dry Bulb, °F: \_\_\_\_\_ CO<sub>2</sub> % \_\_\_\_\_

CO<sub>2</sub> % \_\_\_\_\_

Pitot #	Thermocouple #
1	1
2	2
3	3
4	4
5	5
6	6
7	7
8	8
9	9
10	10
11	11
12	12
13	13
14	14
15	15
16	16
17	17
18	18
19	19
20	20
21	21
22	22
23	23
24	24
25	25
26	26
27	27
28	28
29	29
30	30
31	31
32	32
33	33
34	34
35	35
36	36
37	37
38	38
39	39
40	40
41	41
42	42
43	43
44	44
45	45
46	46
47	47
48	48
49	49
50	50
51	51
52	52
53	53
54	54
55	55
56	56
57	57
58	58
59	59
60	60
61	61
62	62
63	63
64	64
65	65
66	66
67	67
68	68
69	69
70	70
71	71
72	72
73	73
74	74
75	75
76	76
77	77
78	78
79	79
80	80
81	81
82	82
83	83
84	84
85	85
86	86
87	87
88	88
89	89
90	90
91	91
92	92
93	93
94	94
95	95
96	96
97	97
98	98
99	99
100	100

Thermocouple # \_\_\_\_\_ O<sub>2</sub> % \_\_\_\_\_O<sub>2</sub> % \_\_\_\_\_

[Push #]

Pitot Leak Check: Positive	Negative
----------------------------	----------

[illegible]

$$Md = (0.44 \times \%CO_2) + (0.32 \times \%O_2) + (0.28 \times \%N_2)$$

$$Md = (0.44 \times \quad) + (0.32 \times \quad) + (0.28 \times \quad)$$

Md=

$$M_s = M_d \times \left(1 - \frac{\%H_2O}{100}\right) + 18 \times \left(\frac{\%H_2O}{100}\right)$$

$$MS = \left( \quad \right) \times \left( 1 - \frac{\quad}{100} \right) + 18 \times \left( \frac{\quad}{100} \right)$$

$$M_S =$$

$$\overline{\text{TS}} = \quad ^\circ\text{F} = \quad ^\circ\text{R} (^\circ\text{F} + 460)$$

$$P_s = P_b + \frac{SP}{13.6} = ( \quad ) + \frac{\quad}{13.6}$$

Ps =                      in. Hg

$$\sqrt{\Delta P} =$$

$$V_s = 85.49 \times C_p \times \sqrt{\Delta P} \times \sqrt{\frac{T_s(^{\circ}R)}{P_s \times M_s}}$$

$$V_s = 85.49 \times (\quad) \times (\quad) \times \sqrt{\quad}$$

$$V_S = \quad \text{ft/s}$$

$$A_s = \quad \text{ft}^2$$

$$O_s = V_s \times A_s \times 60$$

$$Q_s = \quad \times \quad \times 60$$

0s = acfm

$$Q_{S_{std}} = Q_S \times 17.647 \times \frac{P_S}{T_S} \times \left(1 - \frac{\%H_2O}{100}\right)$$

$$Q_{Std} = \quad \times 17.647 \times \frac{\quad}{\quad} \times \left(1 - \frac{\quad}{100}\right)$$

$$Q_{std} = \text{dscfm}$$

### GAS VELOCITY AND VOLUMETRIC FLOW RATE

Plant:

Date:

Sampling Location: Bayhorse Stack 1

Clock Time:

Run #: Flaw Operators: MP

Operators:

Barometric Pressure, in. Hg: ~~30.75~~ 30.21 Static Pressure, in. H<sub>2</sub>O: -1.3Static Pressure, in.H<sub>2</sub>O:

Moisture, %:                      Molecular wt., Dry:                      Pitot Tube, Cp:

Pitot Tube,  $C_p$ :

Stack Dimension, in. Diameter or Side 1: \_\_\_\_\_ Side 2: \_\_\_\_\_

Side 2:

Wet Bulb, °F:                      Dry Bulb, °F:                      CO<sub>2</sub> %

Dry Bulb, °F:

CO<sub>2</sub> %

Pitot #	Thermocouple #	O <sub>2</sub> %
---------	----------------	------------------

Thermocouple #

O<sub>2</sub> %

Push #

Pitot Leak Check: Positive

Negative

Traverse Point Number	Velocity Head in. H <sub>2</sub> O	Stack Temp., °F
1	4.0	84
2	3.9	91
3	3.8	95
4	3.9	96
5	3.9	102
6	4.0	104
7	3.7	107
8	3.7	120
9	3.5	117
10	3.6	119
11	3.5	122
12	3.8	95
13	3.9	78
14	3.9	110
15	3.4	109
16	3.8	106
17	3.7	111
18	3.8	113
19	3.7	117
20	3.8	120
21	3.8	124
22	3.7	121
23	3.7	122
24	3.7	124
25	3.7	123
$\sqrt{\Delta P} =$	1.9429	Ts=109

$$Md = (0.44 \times \%CO_2) + (0.32 \times \%O_2) + (0.28 \times \%N_2)$$
$$Md = (0.44 \times \quad) + (0.32 \times \quad) + (0.28 \times \quad)$$

Md=

$$M_s = M_d \times \left(1 - \frac{\%H_2O}{100}\right) + 18 \times \left(\frac{\%H_2O}{100}\right)$$
$$MS = \left( \frac{1}{100} \right) \times \left( 1 - \frac{1}{100} \right) + 18 \times \left( \frac{1}{100} \right)$$

Ms=

$$\overline{T_S} = \quad {}^\circ\text{F} = \quad {}^\circ\text{R}({}^\circ\text{F} + 460)$$
$$P_s = P_b + \frac{SP}{13.6} = ( \quad ) + \frac{\quad}{13.6}$$

$$P_s = \quad \text{in. Hg}$$
$$\sqrt{\Delta P} =$$
$$V_s = 85.49 \times C_p \times \sqrt{\Delta P} \times \sqrt{\frac{T_s(^{\circ}R)}{P_s \times M_s}}$$
$$V_s = 85.49 \times ( ) \times ( ) \times \sqrt{ }$$
$$V_s = \quad \text{ft/s}$$
$$A_S = \quad \text{ft}^2$$
$$Q_s = V_s \times A_s \times 60$$
$$Q_s = \quad \times \quad \times 60$$
$$Q_s = \quad \text{acfm}$$
$$Q_{S_{std}} = Q_S \times 17.647 \times \frac{P_S}{T_S} \times \left(1 - \frac{\%H_2O}{100}\right)$$
$$Q_{Std} = \quad \times 17.647 \times \frac{\quad}{\quad} \times \left(1 - \frac{\quad}{100}\right)$$
$$Q_{s_{std}} = \text{dscfm}$$

### GAS VELOCITY AND VOLUMETRIC FLOW RATE

Plant: AK Middletown Date: 9/14/16  
 Sampling Location: P. Baghouse #2 Clock Time: \_\_\_\_\_  
 Run #: P-315-2 Operators: GD  
 Barometric Pressure, in. Hg: 30.21 Static Pressure, in. H<sub>2</sub>O: \_\_\_\_\_  
 Moisture, %: \_\_\_\_\_ Molecular wt., Dry: \_\_\_\_\_ Pitot Tube, Cp: 0.84  
 Stack Dimension, in. Diameter or Side 1: 35.5" Side 2: \_\_\_\_\_  
 Wet Bulb, °F: \_\_\_\_\_ Dry Bulb, °F: \_\_\_\_\_ CO<sub>2</sub> % \_\_\_\_\_  
 Pitot # T4-16 Thermocouple # T4-16 O<sub>2</sub> % \_\_\_\_\_

Pitot Leak Check: Positive ☒ Negative ☒

CLOCK TIME	Traverse Point Number	Velocity Head in. H <sub>2</sub> O	Stack Temp, °F
1018	1	3.2	95
1030	2	3.2	98
1044	3	3.3	104
1106	4	3.1	113
1122	5	3.3	116
1139	6	3.1	120
1159	1	3.0	125
1218	2	3.1	141
1237	3	3.0	139
1256	4	3.0	137
1315	5	3.2	139
1327	6	3.5	120
1426	1	3.3	108
1436	2	3.2	114
1451	3	3.1	120
1504	4	3.2	125
1521	5	2.8	130
1547	6	3.0	128
1558	1	2.8	126
1613	2	2.7	124
	3		
	4		
	5		
	6		
	1		
	2		
	3		
	4		
$\sqrt{\Delta P} =$		1.7613	Ts = 121

$$Md = (0.44 \times \%CO_2) + (0.32 \times \%O_2) + (0.28 \times \%N_2)$$

$$Md = (0.44 \times \quad) + (0.32 \times \quad) + (0.28 \times \quad)$$

$$Md =$$

$$Ms = Md \times \left(1 - \frac{\%H_2O}{100}\right) + 18 \times \left(\frac{\%H_2O}{100}\right)$$

$$Ms = \left( \quad \right) \times \left(1 - \frac{\quad}{100}\right) + 18 \times \left(\frac{\quad}{100}\right)$$

$$Ms =$$

$$TS = \quad ^\circ F = \quad ^\circ R (^\circ F + 460)$$

$$Ps = Pb + \frac{SP}{13.6} = \left( \quad \right) + \frac{\quad}{13.6}$$

$$Ps = \quad \text{in. Hg}$$

$$\sqrt{\Delta P} =$$

$$Vs = 85.49 \times Cp \times \sqrt{\Delta P} \times \sqrt{\frac{Ts(^{\circ}R)}{Ps \times Ms}}$$

$$Vs = 85.49 \times \left( \quad \right) \times \left( \quad \right) \times \sqrt{\quad}$$

$$Vs = \quad \text{ft/s}$$

$$As = \quad \text{ft}^2$$

$$Qs = Vs \times As \times 60$$

$$Qs = \quad \times \quad \times 60$$

$$Qs = \quad \text{acfm}$$

$$Qs_{std} = Qs \times 17.647 \times \frac{Ps}{Ts} \times \left(1 - \frac{\%H_2O}{100}\right)$$

$$Qs_{std} = \quad \times 17.647 \times \quad \times \left(1 - \frac{\quad}{100}\right)$$

$$Qs_{std} = \quad \text{dscfm}$$

## GAS VELOCITY AND VOLUMETRIC FLOW RATE

Plant: AK MIDDLETOWN Date: 9/14-15/16  
Sampling Location: PUSHING BAGHOUSE (STACK 1) Clock Time: \_\_\_\_\_  
Run #: \_\_\_\_\_ Operators: LT  
Barometric Pressure, in. Hg: 30.71 Static Pressure, in. H<sub>2</sub>O: -1.3  
Moisture, %: \_\_\_\_\_ Molecular wt., Dry: \_\_\_\_\_ Pitot Tube, Cp: \_\_\_\_\_  
Stack Dimension, in. Diameter or Side 1: \_\_\_\_\_ Side 2: \_\_\_\_\_  
Wet Bulb, °F: \_\_\_\_\_ Dry Bulb, °F: \_\_\_\_\_ CO<sub>2</sub> % \_\_\_\_\_  
Pitot # \_\_\_\_\_ Thermocouple # \_\_\_\_\_ O<sub>2</sub> % \_\_\_\_\_

Pitot Leak Check: Positive	Negative
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TIME	Traverse Point Number	Velocity Head in. H <sub>2</sub> O	Stack Temp. °F
2222	1	4.0	84
2231	2	4.0	97
1246	3	3.9	101
2305	4	3.8	104
2323	5	3.8	102
2343	6	3.8	103
0001	7	3.9	103
0020	8	3.8	108
0040	9	3.8	106
0058	10	3.9	102
0118	11	3.9	98
0136	12	3.8	100
0145	13	4.0	86
0320	14	3.9	94
0336	15	3.8	99
0345	16	3.8	102
0355	17	3.9	99
0402	18	4.0	94
0400	19	3.8	94
0420	20	3.9	95
0435	21	4.0	92
0452	22	3.9	94
	23	4.0	89
	24	3.9	96
	25	4.0	92
$\overline{\Delta P} =$	1.9727	$\overline{T}_s = 97$	

$$Md = (0.44 \times \%CO_2) + (0.32 \times \%O_2) + (0.28 \times \%N_2)$$

$$Md = (0.44 \times \quad) + (0.32 \times \quad) + (0.28 \times \quad)$$

Md=

$$M_s = M_d \times \left(1 - \frac{\%H_2O}{100}\right) + 18 \times \left(\frac{\%H_2O}{100}\right)$$

$$MS = \left( \quad \right) \times \left( 1 - \frac{\quad}{100} \right) + 18 \times \left( \frac{\quad}{100} \right)$$

Ms=

$$\overline{\text{TS}} = \quad {}^{\circ}\text{F} = \quad {}^{\circ}\text{R}({}^{\circ}\text{F} + 460)$$

$$P_s = P_b + \frac{SP}{13.6} = ( \quad ) + \frac{\quad}{13.6}$$

Ps = \_\_\_\_\_ in. Hg

$$\sqrt{\Delta P} =$$

$$V_s = 85.49 \times C_p \times \sqrt{\Delta P} \times \sqrt{\frac{T_s(^{\circ}R)}{P_s \times M_s}}$$

$$V_s = 85.49 \times (\quad) \times (\quad) \times \sqrt{\quad}$$

$$V_S = \quad \text{ft/s}$$

$$A_s = \quad \text{ft}^2$$

$$Q_s = V_s \times A_s \times 60$$

$$Q_s = \quad \times \quad \times 60$$

Qs =            acfm

$$Q_{S_{std}} = Q_S \times 17.647 \times \frac{P_S}{T_S} \times \left(1 - \frac{\%H_2O}{100}\right)$$

$$Q_{Std} = \frac{15}{100} \times 17.647 \times \frac{100}{100} \times \left(1 - \frac{100}{100}\right)$$

$$Q_{S_{std}} = \text{dscfm}$$

## GAS VELOCITY AND VOLUMETRIC FLOW RATE

Plant: FA Middle Farm

Date: 9-15-16

Sampling Location: Combustion Stack 1

Clock Time: \_\_\_\_\_

Run #: 10-10-10

Operators: NP

Barometric Pressure, in. Hg: 30.24

Static Pressure, in.H<sub>2</sub>O: 71.5

Moisture, %: \_\_\_\_\_ Molecular wt., Dry: \_\_\_\_\_ Pitot Tube, Cp: \_\_\_\_\_

Molecular wt., Dry: \_\_\_\_\_ Pitot Tube, Cp: \_\_\_\_\_

Pitot Tube,  $C_p$ : \_\_\_\_\_

Stack Dimension, in. Diameter or Side 1:

Side 2:

Wet Bulb, °F: \_\_\_\_\_ Dry Bulb, °F: \_\_\_\_\_ CO<sub>2</sub> % \_\_\_\_\_

Dry Bulb, °F: \_\_\_\_\_ CO<sub>2</sub> % \_\_\_\_\_CO<sub>2</sub> % \_\_\_\_\_Pitot # \_\_\_\_\_ Thermocouple # \_\_\_\_\_ O<sub>2</sub> % \_\_\_\_\_Thermocouple # \_\_\_\_\_ O<sub>2</sub> % \_\_\_\_\_O<sub>2</sub> % \_\_\_\_\_

Pitot Leak Check: Positive	Negative
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[illegible]

$$Md = (0.44 \times \%CO_2) + (0.32 \times \%O_2) + (0.28 \times \%N_2)$$

$$Md = (0.44 \times \quad) + (0.32 \times \quad) + (0.28 \times \quad)$$

Md=

$$M_s = M_d \times \left(1 - \frac{\%H_2O}{100}\right) + 18 \times \left(\frac{\%H_2O}{100}\right)$$

$$M_S = \left( \quad \right) \times \left( 1 - \frac{\quad}{100} \right) + 18 \times \left( \frac{\quad}{100} \right)$$

$$M_S =$$

$$\overline{\text{TS}} = \quad \quad \quad ^\circ\text{F} = \quad \quad \quad ^\circ\text{R} (^{\circ}\text{F} + 460)$$

$$P_S = P_b + \frac{SP}{13.6} = ( \quad ) + \frac{\quad}{13.6}$$

Ps = \_\_\_\_\_ in. Hg

$$\sqrt{\Delta P} =$$

$$V_s = 85.49 \times C_p \times \sqrt{\Delta P} \times \sqrt{\frac{T_s(^{\circ}R)}{P_s \times M_s}}$$

$$V_s = 85.49 \times \left( \frac{1}{100} \right) \times \left( \frac{1}{100} \right) \times \sqrt{\frac{1}{100}}$$

$$V_s = \quad \text{ft/s}$$

$$As = \frac{1}{2} \pi r^2 \quad \text{ft}^2$$

$$Q_s = V_s \times A_s \times 60$$

$$Q_s = \quad \times \quad \times 60$$

0s = acfm

$$Q_{Sstd} = Q_S \times 17.647 \times \frac{P_S}{T_S} \times \left(1 - \frac{\%H_2O}{100}\right)$$

$$Q_{std} = \quad \times 17.647 \times \frac{100}{100} \times \left(1 - \frac{100}{100}\right)$$

$$0s_{std} = \text{dscfm}$$

## GAS VELOCITY AND VOLUMETRIC FLOW RATE

Plant: AK Middletown Date: 9/15/16  
 Sampling Location: P. Baghouse # 2 Clock Time: \_\_\_\_\_  
 Run #: P-315-3 Operators: GP  
 Barometric Pressure, in. Hg: 30.24 Static Pressure, in. H<sub>2</sub>O: \_\_\_\_\_  
 Moisture, %: \_\_\_\_\_ Molecular wt., Dry: \_\_\_\_\_ Pitot Tube, Cp: 0.84  
 Stack Dimension, in. Diameter or Side 1: 35.5" Side 2: \_\_\_\_\_  
 Wet Bulb, °F: \_\_\_\_\_ Dry Bulb, °F: \_\_\_\_\_ CO<sub>2</sub> % \_\_\_\_\_  
 Pitot # T4-16 Thermocouple # T4-16 O<sub>2</sub> % \_\_\_\_\_

Pitot Leak Check: Positive ☒ Negative ☒

Clock Time	Traverse Point Number	Velocity Head in. H <sub>2</sub> O	Stack Temp, °F
1059	3	3.5	105
1130	4	3.3	114
1140	5	3.2	123
1235	6	3.1	118
1243	1	3.2	121
1251	2	3.2	120
1259	3	3.3	126
1309	4	3.2	127
1320	5	3.4	129
1334	6	3.2	132
1343	1	3.3	132
1438	2	3.2	124
1450	3	3.1	129
1506	4	3.3	136
1523	5	3.5	130
1540	6	3.2	127
1558	1	3.1	131
1615	2	3.3	126
1632	3	3.2	121
1650	4	3.1	117
1707	5	3.4	123
1724	6	3.2	121
1737	1	3.4	120
	2		
	3		
	4		
	5		
	6		
$\sqrt{\Delta P} = 1.8043$		$\overline{T_s} = 124$	

$$Md = (0.44 \times \%CO_2) + (0.32 \times \%O_2) + (0.28 \times \%N_2)$$

$$Md = (0.44 \times \quad) + (0.32 \times \quad) + (0.28 \times \quad)$$

$$Md =$$

$$Ms = Md \times \left(1 - \frac{\%H_2O}{100}\right) + 18 \times \left(\frac{\%H_2O}{100}\right)$$

$$Ms = \left(\quad\right) \times \left(1 - \frac{\quad}{100}\right) + 18 \times \left(\frac{\quad}{100}\right)$$

$$Ms =$$

$$\overline{T_s} = \quad ^\circ F = \quad ^\circ R (^\circ F + 460)$$

$$Ps = Pb + \frac{SP}{13.6} = \left(\quad\right) + \frac{\quad}{13.6}$$

$$Ps = \quad \text{in. Hg}$$

$$\sqrt{\Delta P} =$$

$$Vs = 85.49 \times Cp \times \sqrt{\Delta P} \times \sqrt{\frac{T_s(^{\circ}R)}{Ps \times Ms}}$$

$$Vs = 85.49 \times \left(\quad\right) \times \left(\quad\right) \times \sqrt{\quad}$$

$$Vs = \quad \text{ft/s}$$

$$As = \quad \text{ft}^2$$

$$Q_s = Vs \times As \times 60$$

$$Q_s = \quad \times \quad \times 60$$

$$Q_s = \quad \text{acfm}$$

$$Q_{sstd} = Q_s \times 17.647 \times \frac{Ps}{T_s} \times \left(1 - \frac{\%H_2O}{100}\right)$$

$$Q_{sstd} = \quad \times 17.647 \times \quad \times \left(1 - \frac{\quad}{100}\right)$$

$$Q_{sstd} = \quad \text{dscfm}$$



## TRAVERSE POINT LOCATION FOR CIRCULAR DUCTS

Plant: Hesperis matronalis Middleton

Date: 8/22/16

Sampling Location: Combustion Stack

Inside of Far Wall to Outside of Nipple: \_\_\_\_\_

Inside of Near Wall to Outside of Nipple (Nipple Length): \_\_\_\_\_

Stack I.D.: 168

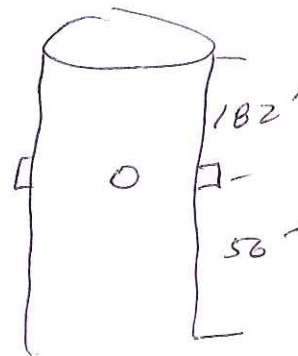
Distance Downstream from Flow Disturbance (Distance B):

2184 Inches/Stack I.D. = 13 dd

Distance Upstream from Flow Disturbance (Distance A):

672 Inches/Stack I.D. = 26 dd

Calculated By: Doug Allen



### Schematic of Sampling Location

[illegible]